



NMDQi Thermal-Hydraulic Optimization, Analysis, and Scoping Tool (TOAST)

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ABSTRACT

The Thermal-hydraulic Optimization, Analysis, and Scoping Tool (TOAST) is developed to support the thermal-hydraulic aspects for the design of optimal irradiation vehicles for the Nuclear Materials Discovery and Qualification initiative (NMDQi). TOAST is currently a MATLAB-based tool that utilizes a simplified steady-state analytical model where a radial thermal resistance circuit is utilized to account for conduction through up to 2 capsules, a gas gap, a thermal bond, a sample cladding, and a sample, as well as the convection from a water coolant outside the capsules. The geometry is discretized axially along the user-defined height of a basket with a user-defined number of points/nodes, essentially turning TOAST into a semi-2D heat transfer analysis utility for cylindrical irradiation vehicles with practically any configuration, solving for temperatures radially at multiple axial locations. TOAST utilizes a Graphical User Interface (GUI) in-which a user can define the geometrical layout, the materials utilized for each component, the coolant characteristics, and the required solution. The user can define the geometry by inputting the diameters, thicknesses, and heights for each component, whereas the materials are defined via the user-provided constant or variable thermal conductivities. The user can select the coolant's inlet temperature, pressure, and the pressure drop across the height of the problem (which is used to calculate the velocity of the flow). Finally, the user can choose to solve for a sample heat generation rate limit by inputting temperature limits for the sample and capsules or can choose to purely solve for the axial temperature distributions of each component by inputting a pre-selected heat generation rate. Either way, TOAST provides the user with axial temperature distributions of all the components including the coolant, and the heat generation rate limit as well as the maximum outlet coolant temperature. The user can also choose to do one of 6 sensitivity analyses in TOAST. The sensitivity analyses yield plots of the sensitivity of the heat generation rate limit, the maximum coolant temperature, and the pressure limit for the annular components due to perturbations in 1-2 unknown variables based on the selected sensitivity analysis. Benchmarks between computations in TOAST and equivalent 2D axis symmetric ABAQUS models are presented, showing that TOAST results are within less than 3% of ABAQUS results in most cases, and a maximum of 8% difference in some cases. The benchmarks also revealed that this uncertainty is tied to the selection of an appropriate Nusselt number correlation and appropriate thermal conductivities, which the user can do from the GUI. Regardless, TOAST is demonstrated as a computationally efficient, highly accessible, and accurate utility for optimization and scoping of studies different irradiation vehicles.

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ACRONYMS

AFC	Advanced Fuel Campaign
AFC-FAST	Advanced Fuels Campaign Fission Accelerated Steady-State Testing
ANS	American Nuclear Society
ASME	American Society of Mechanical Engineers
ATF	accident tolerant fuel
ATR	Advanced Test Reactor
DNBR	departure from nucleate boiling ratio
FIR	flow instability ratio
GUI	graphical user interface
INL	Idaho National Laboratory
MOOSE	Multiphysics Object-Oriented Simulation Environment
NMDQi	Nuclear Materials Discovery and Qualification initiative
NRC	Nuclear Regulatory Commission
ODs	outer diameters
IDs	inner diameters
THAT	Thermal-Hydraulic Analysis Team
TOAST	Thermal-hydraulic Optimization, Analysis, and Scoping Tool
V&V	verification and validation

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NMDQi Thermal-Hydraulic Optimization, Analysis, and Scoping Tool (TOAST)

1. PREFACE

In winter 2016, Dr. Andrew Klein, then president of the American Nuclear Society (ANS), launched a nuclear grand challenge effort, wherein more than 125 nuclear professionals and students conducted roundtable brainstorming sessions to come up with ideas for such challenges that must be resolved by 2030 [1]. By June 2017, all the ideas were consolidated into the following nine grand challenges via recommendations made by more than 300 professionals in multiple ANS divisions.

1. “Transform the way the nuclear technologies sector thinks about public engagement.”
2. “Establish the scientific basis for modern low-dose radiation regulation.”
3. “Close the nuclear fuel cycle.”
4. “Ensure continuous availability of radioisotopes.”
5. “Rejuvenate nuclear technology infrastructure and facilities.”
6. “Accelerate development and qualification of advanced materials.”
7. “Accelerate utilization of simulation and experimentation.”
8. “Expedite licensing and deployment of advanced reactor designs.”
9. “Expedite nuclear education updates and knowledge transfer.”

It is important to note that the general reoccurring theme across most of the challenges is the need for establishing tools and capabilities to accelerate and expedite the development of new technologies and rejuvenate the existing nuclear technology infrastructure. The nuclear industry is potentially the slowest industry at adapting to changes and technological advancements, as is evidenced by the lengthy and costly licensing and qualification processes for anything related to the design and construction of a nuclear reactor. Other industries and markets react to technological advancements much differently, which is clearly demonstrated in the vast differences between an iPhone 4 (2010) and an iPhone 11 (2019) (per information found on www.gadgetsnow.com).

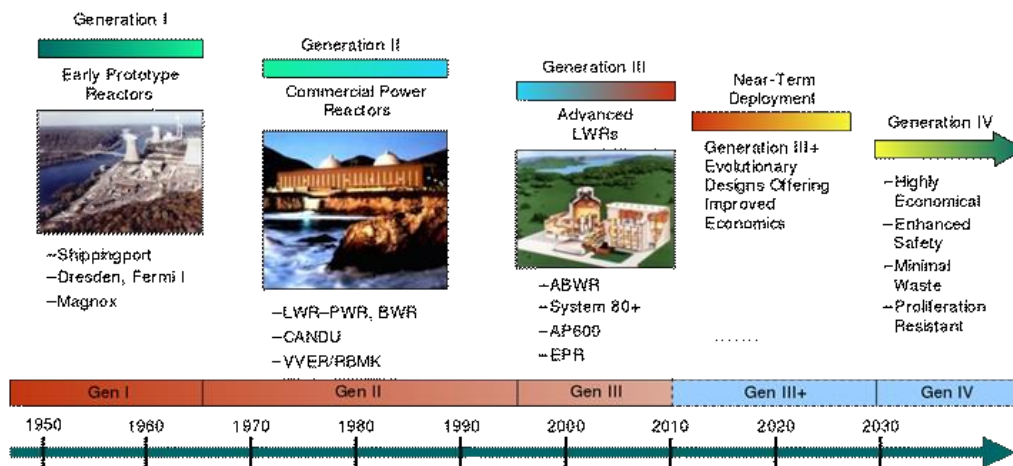


Figure 1. Nuclear reactor generations and a proposed timeline [2].

In this decade, the iPhone processor speed more than doubled and the RAM storage more than quadrupled all-while the launch price (accounting for inflation) remained approximately the same. In that same decade, advances in new nuclear infrastructure (reactors, powerplants) exponentially grew without many changes to the existing technology. The nuclear industry sported commercial nuclear reactors from Gen II (PWRs, BWRs, CANDUs) for decades without showing much intergenerational progress. It wasn't until the recent opening of the Barakah reactor unit in Abu Dhabi, UAE that a reactor from a "new generation" has surfaced in the market. The sluggishness and costliness in nuclear technological advancements is shown in the generic reactor generations chart (see Figure 1), where Gen III reactors seem like necessary safety upgrades to Gen II reactors and an intermediary generation was necessary to separate Gen III and the elusive Gen IV with, once again, the evolutions of Gen II reactors.

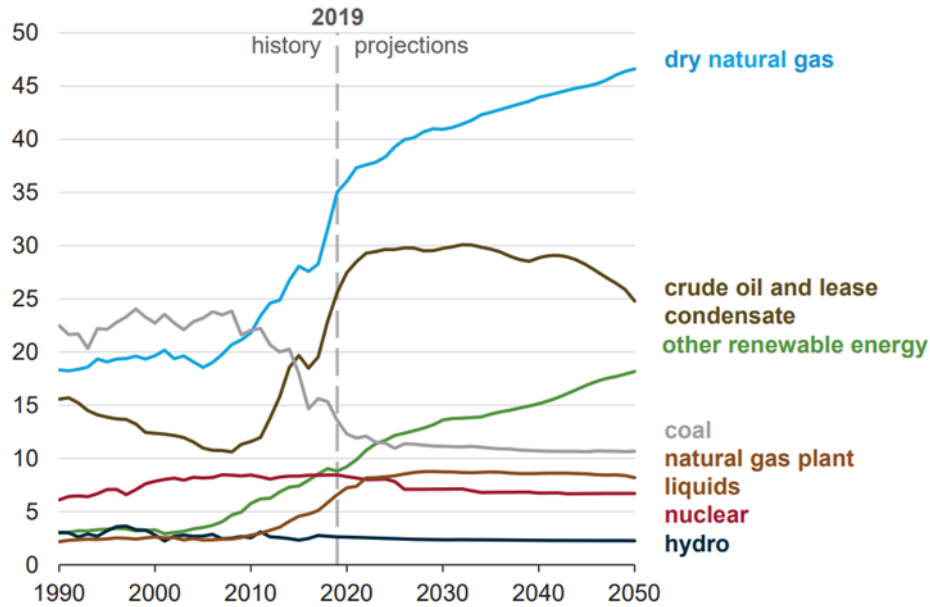


Figure 2. Percent share of every energy source in the U.S. throughout the years [3].

While natural gas, crude oil, and renewable energy production shares increased within this decade, nuclear almost flat-lined, with projections of its energy share decreasing as renewable energy subsidies increase. The gap left by decreases in the massive nuclear power capacity cannot be solely replaced by renewables, forcing an increased reliance on volatile natural gas, which in turn would contribute to a larger natural gas energy share. This increased natural gas reliance may be economical in the short-term, but long-term disadvantages would far outweigh those short-term economic advantages. For starters, an increase in natural gas energy production would lead to increased fracking and the production of more greenhouse gases, further contributing to global warming. Additionally, as the reliance on natural gas grows so will its demand, meaning that sooner-or-later the supply will suffer and the prices will increase, potentially offsetting any short-term economic advantages. For those reasons, it is important to keep nuclear power competitive in the energy market with advanced nuclear reactors that are more efficient and less costly than existing technologies. This is the primary goal of most of the listed nuclear challenges.

Multiple initiatives have since been developed to address those challenges, with efforts primarily directed to the verification and validation (V&V) of thermal-hydraulic computational fluid dynamics and system-level codes (Nuclear Regulatory Commission initiatives [4], American Society of Mechanical Engineers (ASME) V&V Problems), and, of most interest to this report, an accelerated nuclear materials discovery and qualification process. To support all those initiatives, it is vital to develop more accessible tools, correlations, methodologies, and databases to accelerate and refine the current processes.

2. INTRODUCTION

Due to the nature of the nuclear materials discovery and qualification process, multiple irradiation experiments are necessary to assist in qualification efforts. This leads to large arrays of iterative tests with various irradiation conditions. Naturally, this implies that each experiment conducted would consist of a unique and specific combination of dimensions, materials, incident neutron flux, and heat loads. Each experiment's characteristics are typically chosen using a set of computational studies prior to irradiation to ensure appropriate experiments are carried out safely [5,6]. This procedure implies multidecade development cycles to iterate through the variations of a material (fuel, clad, structural support, etc.) in order to qualify it [7,8]. Not only does this suggest extremely high financial and labor costs towards the qualification of advanced nuclear materials, it also makes it less likely for innovative materials to be considered as the discovery process of such materials will further extend the development procedure. This suppresses innovation in the field of nuclear materials, as lengthy development processes come with an increased financial burden and decreased likelihood for implementation during our lifetimes, driving away potential investors and aspiring scientists and engineers. As such, it is no surprise that future nuclear technologies will require a shortened and more streamlined development and deployment timeline, which implies a shortened discovery and qualification process for nuclear materials [9].

To support this sentiment, the Nuclear Materials Discovery and Qualification Initiative (NMDQi) was recently established as an effort to develop the tools and capabilities for supporting the accelerated discovery and engineering qualification of new materials for use in advanced nuclear reactors [10,11]. The acceleration of thermal-hydraulic optimization studies for irradiation experiments, particularly at the Advanced Test Reactor (ATR) at Idaho National Laboratory (INL) [12], is of particular interest to the work outlined in this report, where a versatile thermal analysis tool is developed with sensitivity and parametric analysis capabilities for different experiment dimensions (fuel, clad, capsules, etc.). This tool serves as a dimensional and thermal-hydraulic optimization utility that can drive decisions about the sizing of any material in an irradiation environment with any set of thermal-hydraulic characteristics (temperature limits, coolant flow rates, linear heat generation rates, etc.) while maintaining computational efficiency (i.e., little computational power is required).

This report outlines the methodology by which the thermal-hydraulic analysis model is driven, how the sensitivity analysis system works, and the frameworks that allows the user to interface with the models and its results. Benchmark problems are also presented to provide an understanding of the tool's uncertainties and their sources as compared to results from similar models in the commercial software ABAQUS [13], which is typically used in thermal-hydraulic safety and programmatic analyses at INL.

3. METHODOLOGY

3.1 Thermal-Hydraulic Analysis Model

The Thermal-Hydraulic Optimization, Analysis, and Scoping Tool (TOAST) adopts a generalized geometry layout that closely reflects the Advanced Fuel Campaign (AFC) irradiation vehicle layout [5,14] in an effort to remain computationally inexpensive and highly accessible. This general layout allows for a wide range of cylindrical irradiation vehicles, accommodating single-capsule and multicapsule setups. This geometrical layout is illustrated in Figure 3, where a basket contains the coolant channel (water for the purposes of this report). Within the coolant channel lies an outer capsule (Capsule 1) casing an inner capsule (Capsule 2) with a gas gap in between the two capsules. Capsule 2 holds a thermal bond of some thickness separating the capsule from the rodlet clad, which houses the sample.

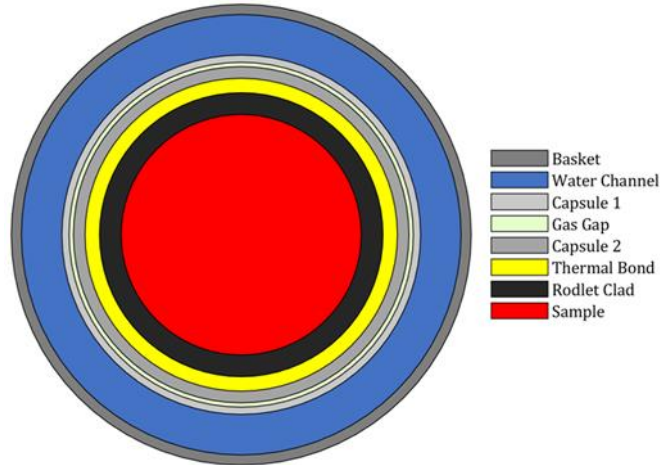


Figure 3. A top view of the generalized layout setup for TOAST.

The layout above is simplified by assuming symmetry in the axial and radial thermal profiles, yielding the simplified geometrical setup shown in Figure 4, where only a quarter of the geometry is found necessary with the aforementioned assumptions. It is implied that the user has control over the dimensions and thermal conductivities of the components in the irradiation vehicle (capsules, clad, and sample) as well as the flow rate (proxy of the pressure drop) and inlet temperature and pressure of the coolant. Note that end-caps are not accounted for in this model, but the actual coolant path is maintained. As such, unlike what Figure 4 suggests, no flow occurs directly above the sample and clad but instead occurs directly above the capsules.

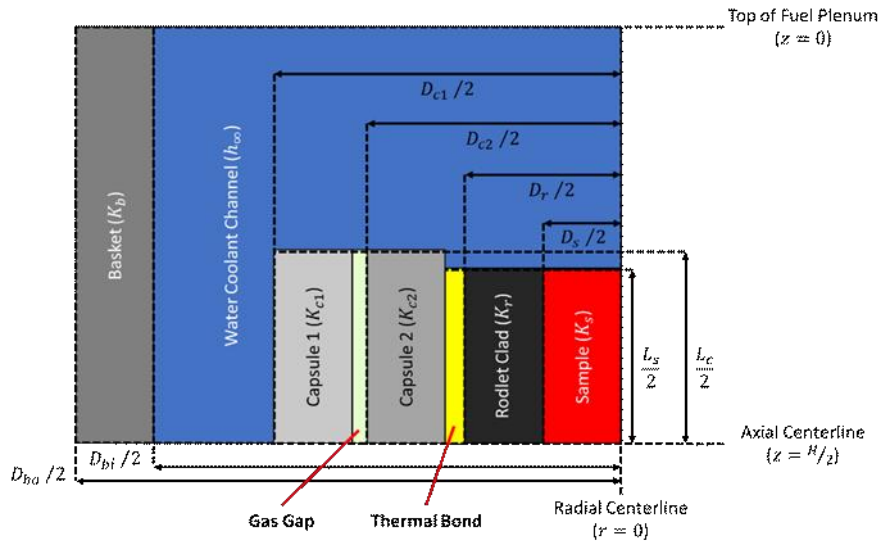


Figure 4. A side view of the simplified geometrical setup for TOAST.

With the geometrical layout defined, an appropriate thermal analysis model can be developed. The model developed for TOAST is a semi-2D model that provides axial temperature distributions at specific radial positions by solving a radial heat transfer network at multiple axial locations. The selected radial positions are at the inner surface of each of the components and at the sample centerline, due to the assumption that the highest temperature for each component would be at its innermost radial position. As such, the radial positions are listed below, and they consist of the inner diameters (IDs) and outer diameters (ODs) of different components.

- Coolant temperature at the innermost location (OD of Capsule 1 when the capsule is reached or at the radial centerline otherwise)
- ID of Capsule 1
- ID of Capsule 2
- ID of the rodlet clad
- Radial centerline of the sample

The axial (height-wise) direction is uniformly discretized via a set of equally spaced points (e.g., nodes) spanning the entire height of the geometry (typically the height of the basket). The number of axial points is selected by the user in TOAST. In a sense, this setup corresponds to a 2D mesh that is discretized uniformly in the axial direction with a user-set number of points and exactly five points in the radial direction. In that sense, the mesh is very coarse compared to meshes that are generated in other finite element or volume codes, with thousands of nodes in all directions. It somewhat corresponds to modeling approaches implemented in system-level thermal-hydraulic codes, such as RELAP [15] and TRACE [16], or severe accident codes, such as MELCOR [17]. This radial coarseness in the spatial discretization is beneficial, as it allows for the inexpensive computation of the components' maximum temperatures, which is usually of high importance for scoping and optimization studies. This is possible by only considering the innermost points of each of the components, where the data predicts the maximum temperatures. A finer radial discretization is possible in a future version of TOAST; however, for the time-being, this simplified approach is more advantageous.

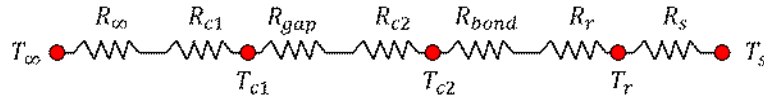


Figure 5. The radial thermal resistance circuit used for each axial position modeled in TOAST.

Corresponding to the simplified geometrical setup shown in Figure 4 and the aforementioned discretization system, a thermal resistance circuit can be setup for different axial positions to model the steady-state temperature profile at each radial position throughout the geometry. This leads to the circuit shown in Figure 5, where the coolant temperature (T_{∞}) is used to calculate the inner temperature of Capsule 1 (T_{c1}) using the thermal resistance due to convection through the coolant (R_{∞}) and conduction through Capsule 1 (R_{c1}). T_{c1} can then be used to calculate the inner temperature of Capsule 2 (T_{c2}) by accounting for the thermal resistance due to conduction through the gas gap (R_{gap}) and Capsule 2 (R_{c2}). Similarly, T_{c2} is used to calculate the rodlet clad inner temperature (T_r) by accounting for thermal resistances due to conduction through the thermal bond (R_{bond}) and through the rodlet clad (R_r). Finally, the sample centerline temperature (T_s) can be calculated using T_r and the thermal resistance due to conduction through the sample (R_s). Although the in-depth description of the circuit is seemingly unnecessary due to its intuitiveness, we will define the working variables of the problem when discussing the thermal resistance circuit and will further elaborate in later sections of this document.

T_{∞} is calculated by considering the heat rate of the sample and assuming the coolant inhibits a cosine heating distribution of a similar format to that of the chopped cosine axial gamma heat distribution at different irradiation experiment positions in ATR [18]. The cosine heating distribution for the water is shown in Equation 1, where the sample heat rate (q'_{limit}), spacing between axial discretization points (Δz), the sample length (L_s) are accounted for alongside a cosine fitting constant (c , assumed to be 1 for this report), the axial position relative to the top of the basket (z), the axial centerline relative to the top of the basket (z_{cent}), and the maximum heat rate offset from the axial centerline (x_0).

$$q'(z) = q'_{limit} \Delta z \cos(c [|z - z_{cent}| - x_0]) \quad (1)$$

The axial distribution of the coolant temperature can then be derived assuming a constant mass flow rate (\dot{m}) and specific heat (c_p), yielding the discretization-friendly relation shown in Equation 2. In Equation 2, the coolant temperature at each axial position (z) is calculated by adding the sample heating contributions to the coolant temperature at the previous axial location ($z - 1$), such that $z = 0$ represents the inlet boundary of the flow with a user-specified inlet temperature.

$$T_{\infty}(z) = T_{\infty}(z - 1) + \left(\frac{q'_{limit} \Delta z}{\dot{m} c_p} \sin(c [|z - z_{cent}| - x_0]) + \sin(c [z_{cent} - x_0]) \right) \quad (2)$$

As for the q'_{limit} , which drives the whole thermal analysis procedure, it is important to reiterate that the user has the choice to provide the sample linear heat generation rate (q'_s) or provide the temperature limits for the capsules and the sample. If the user provides q'_s , q'_{limit} is calculated using Equation 3a based on the user's preference for a constant or a cosine-shaped heat-rate profile in the axial direction. If the user provides temperature limits, three different heat rates are calculated, corresponding to each temperature limit, and the minimum of the three is the q'_{limit} , as shown in Equation 3b. $T_{\infty,max}$ corresponds to the maximum coolant temperature (typically at the outlet), and it is used as a conservative measure to ensure a safe q'_{limit} is chosen when doing the calculations for each of the heat rates. This maximum coolant temperature is found by iterating the thermal analysis procedure until a constant value for $T_{\infty,max}$ is reached (to within 0.1 Kelvin).

$$q'_{limit} = \begin{cases} q'_s, & \text{constant heat rate} \\ q'_s \cos(c [|z - z_{cent}| - x_0]), & \text{cosine heat rate profile} \end{cases} \quad (3a)$$

$$Q_{limit} = \min(q'_{c1}, q'_{c2}, q'_s), \quad \begin{cases} q'_{c1} = \frac{T_{c1,limit} - T_{\infty,max}}{R_{\infty} + R_{c1}} \\ q'_{c2} = \frac{T_{c2,limit} - T_{\infty,max}}{R_{\infty} + R_{c1} + R_{gap} + R_{c2}} \\ q'_{c2} = \frac{T_{s,limit} - T_{\infty,max}}{R_{\infty} + R_{c1} + R_{gap} + R_{c2} + R_{bond} + R_r + R_s} \end{cases} \quad (3b)$$

The thermal resistances for each of the components in the system and the coolant are found based on Equation 4a through Equation 4g, where the basket length (L_b), capsules length (L_{cap}), and L_s (sample and rodlet clad length) are used alongside the ID of the basket (D_{bi}), the ODs of Capsules 1 and 2 (D_{c1} and D_{c2} respectively), the ODs of the rodlet clad and sample (D_r and D_s , respectively), and the gas gap

and thermal bond thicknesses (t_{gap} and t_{bond} , respectively). Additionally, the thermal conductivities of Capsule 1, the gas gap, Capsule 2, the thermal bond, the rodlet clad, and the sample are accounted for as well (k_{c1} , k_{gap} , k_{c2} , k_{bond} , k_r , and k_s , respectively).

$$R_{c1} = \frac{\ln(D_{c1}/[D_{c2}+2t_{gap}])}{2\pi k_{c1}} \quad (4a)$$

$$R_{gap} = \frac{\ln([D_{c2}+2t_{gap}]/D_{c2})}{2\pi k_{gap}} \quad (4b)$$

$$R_{c2} = \frac{\ln(D_{c2}/[D_r+2t_{bond}])}{2\pi k_{c2}} \quad (4c)$$

$$R_{bond} = \frac{\ln([D_r+2t_{bond}]/D_r)}{2\pi k_{bond}} \quad (4d)$$

$$R_r = \frac{\ln(D_r/D_s)}{2\pi k_r} \quad (4e)$$

$$R_s = \frac{1}{4\pi k_s} \quad (4f)$$

$$R_{\infty} = \frac{1}{h_{\infty}\pi D_{eq}} \quad (4g)$$

Each thermal conductivity is provided by the user as either a constant or as a variable function of temperature for the respective component (sample, Capsule 1, etc.). The user can provide the variable conductivities by providing the function constants for either a power function (Equation 5a) or as a polynomial function up to a 5th order (Equation 5b). We assume that the conductivity (whether constant or variable) is in units of $\frac{W}{m-K}$. If variable conductivities are selected for the sample, the capsules, or the rodlet clad, those conductivities are calculated at each axial location using the maximum temperature of their respective component in the previous axial location. If variable conductivities are selected for the gas gap or the thermal bond, those are calculated at the average temperature of the two surrounding components, where the gas gap is surrounded by Capsule 1 and 2 and the thermal bond is surrounded by Capsule 2 and the rodlet clad.

$$k_{power}(T) = A \cdot B^{C \cdot T} \quad (5a)$$

$$k_{poly}(T) = p_0 + p_1T + p_2T^2 + p_3T^3 + p_4T^4 + p_5T^5 \quad (5b)$$

R_{∞} is the only thermal resistance in this model that is due to convection, which is why it requires a special treatment, particularly regarding its convective heat transfer coefficient (h_{∞}) and the noted equivalent diameter (D_{eq}). D_{eq} changes depending on the axial location of the coolant, as shown in Equation 6, while h_{∞} can be calculated by correlating it to a Nusselt number (Nu), the hydraulic diameter (D_{hyd}), and the coolant conductivity (k_{∞}), as shown in Equation 7. k_{∞} , for this report, is found for water at 2.5 MPa, and it changes as a function of the coolant temperature per data from the National Institute of Standards and Technology [19].

$$D_{eq} = \begin{cases} D_{bi}, & \text{above capsule 1's top surface} \\ D_{bi} - \frac{D_{c1} L_c}{L_b}, & \text{below capsule 1's top surface} \end{cases} \quad (6)$$

$$h_{\infty} = \frac{Nu k_{\infty}}{D_{hyd}}, \begin{cases} D_{bi}, & \text{above capsule 1's top surface} \\ D_{bi} - D_{c1}, & \text{below capsule 1's top surface} \end{cases} \quad (7)$$

Nu is typically expressed as a function of the Reynolds number (Re) and Prandtl number (Pr) of the coolant, where the Re is a characteristic of the flow, being a multiple of the coolant's density (ρ_{∞}), velocity (U_{∞}), and D_{hyd} divided by the coolant's dynamic viscosity (μ_{∞}). In this report, five Nu correlations are considered, including the Dittus-Boelter correlation in Equation 8 [20], the modified Dittus-Boelter correlation in Equation 9 [21], the Seider-Tate correlation in Equation 10 [22], the Gnielinski correlation in Equation 11 [23], and a custom correlation in Equation 12 developed by combining features in all the aforementioned correlations. Each Nu correlation is benchmarked against results from ABAQUS. The reoccurring f in Equation 11 and Equation 12 is the friction factor of the flow in the coolant channel. It should be noted that the user can choose any of the Nusselt number correlations shown in Equation 8–12.

$$Nu = 0.023 Re^{0.8} Pr^{0.4} \quad (8)$$

$$Nu = (1 + 0.912 Re^{-0.1} Pr^{0.4} [1 - 2.0043 e^{-D_{hyd}/D_{c1}}]) \cdot 0.023 Re^{0.8} Pr^{0.4} \quad (9)$$

$$Nu = 0.027 Re^{0.8} Pr^{1/3} \left(\frac{\mu_{\infty}}{\mu_{wall}} \right)^{0.14}, \text{ assume } \mu_{wall} = \mu(T_{\infty} + 200 K) \quad (10)$$

$$Nu = \frac{(f/8)(Re-1000)Pr}{1+12.7(f/8)^{0.5}(Pr^{2/3}-1)} \quad (11)$$

$$Nu = 0.027 \frac{(Re^{0.9})(Pr^{0.7}-1)\left(\frac{\mu_{\infty}}{\mu_{wall}}\right)^{0.14}}{|1+(20(f/8)^{0.3}Pr^{0.25})|} \quad (12)$$

The convective nature of the heat transfer between the coolant and Capsule 1 requires the computation of the flow's velocity, as evidenced by the Re presence in every Nu correlation needed to calculate h_{∞} . To accommodate this, TOAST asks the user to provide the pressure drop across the basket height (ΔP), which can then be used to calculate the flow's velocity using a procedure outlined in the INL thermal hydraulics analysis guidebook [24]. The approach utilizes a user-provided ΔP alongside a calculated friction loss coefficient (K_f , Equation 13) and conservatively assumed contraction and expansion losses ($K_c = 0.5$ and $K_e = 1$, respectively) to calculate the velocity of the flow by applying the conservation of energy neglecting potential energy (Equation 14).

$$K_f = \frac{4fL}{D}, \quad f = \left[-4 \ln \left(\frac{0.27 \epsilon}{D} + \left(\frac{7}{Re} \right)^{0.9} \right) \right]^{-2} \quad (13)$$

$$U = \sqrt{\frac{2 \Delta P}{\rho_{\infty} (K_c + K_e + K_f)}} \quad (14)$$

Due to the approach adopted here, a Reynolds number is necessary in order to calculate the friction loss coefficient K_f , which presents a conundrum as the Reynolds number is an unknown being solved for. In order to assess that, an analysis was conducted to see how much K_f changes with different Reynolds numbers, where the friction factor (f) is calculated using Churchill's equation for a smooth cast-iron pipe ($\epsilon = 0.26 \text{ mm}$) [25]. The results showed that K_f reaches a steady state at $Re \geq 10^4$ (the expected flow conditions in the core); therefore, K_f is always calculated at the conservative Re of 4×10^6 in this study (Figure 6).

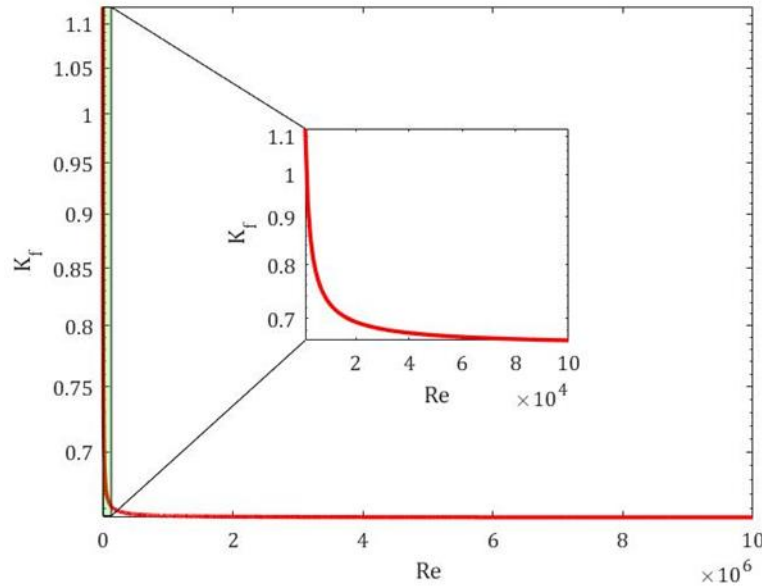


Figure 6. K_f evolution as a function of Re using Churchill's equation for the friction factor f .

The calculated U would act as the velocity at the axial centerline, from which a mass flow rate is calculated by multiplying it with the density of the coolant and the area of fluid at the centerline. Per the conservation of mass principle, the mass flow rate would remain constant across all axial discretization points, but the changing temperature of the coolant would cause the velocity to change as well to maintain a conserved mass. This allows for the computation of the flow velocity at any axial location using this constant mass flow rate. As such, the Reynolds number at each axial location can be calculated, yielding different Nu and h_∞ values at each axial location to use for the thermal resistance through the coolant. This completes the thermal resistance circuits that allow for the computation of the axial temperature profiles of each component.

3.2 Sensitivity Analysis System

TOAST has a sensitivity and parametric analysis capability, where a user can have one unknown parameter in the thermal analysis model and obtain figures that show the sensitivity of q'_{limit} and $T_{\infty,max}$ as a function of the changes to that unknown parameter. In some instances, it is also capable of producing plots for the pressure limits of each cylindrical shell (the capsules and the rodlet clad) per the ASME thin-wall pressure limits due to circumferential stress on longitudinal joints, as described in the ASME pressure vessel codes [26]. This pressure limit (P_{limit}) is calculated as shown in Equation 15, where S_y is the yield strength of each component's material, E is the joint efficiency (assume $E = 1$), t is the thickness of each component, and D_i is the inner diameter of the corresponding component.

$$P_{limit} = \frac{S_y E t}{\frac{D_i}{2} + 0.6t} \quad (15)$$

The ability to track the effects that changes in one unknown parameter has on multiple sensitive values of interest, such as q'_{limit} , $T_{\infty,max}$, and P_{limit} , simultaneously allows the user to perform thorough optimization studies that account for multiple aspects that are relevant to the design process. As such, it is natural to also consider safety margins for the coolant, such as the departure from nucleate boiling ratio (DNBR) and the flow instability ratio (FIR). DNBR provides a measure of how close the critical heat flux is to the local heat flux of the coolant. To compute it, Equation 16 is used, where q''_c is the critical heat flux calculated using the correlation laid out by L. Bernath [27], which was used by the Atomic Energy Commission (now superseded by the NRC) [28] and the Arnold Engineering Development Center of the U.S. Air Force [29], and is recommended by the Thermal-Hydraulic Analysis Team (THAT) guidebook [24] for this type of experiment geometry (annular flow channel). The q''_{max} is supposed to be the maximum heat flux that the surface contacting the coolant is emitting, and, as such, it is the maximum heat flux of Capsule 1 (outer capsule). However, as a conservative measure, q''_{max} is set to the maximum heat flux of the sample instead.

$$DNBR = \frac{q''_c}{q''_{max}} = \frac{5.68 \left(12915 \frac{D_{hyd}}{D_{hyd} + D_{heat}} + 127 \frac{V}{D_{hyd}^{0.35}} \right) \left(60 \ln(P) - 80.8 \frac{P}{P+135} - 0.25 V - T_{\infty} \right)}{q''_{max}} \quad (16)$$

where D_{hyd} [ft] is the hydraulic diameter ($D_{bi} - D_{c1}$), D_{heat} [ft] is the heated diameter (D_{c1}), P [psi] is the coolant pressure, V [ft/s] is the coolant velocity (calculated using a total pressure drop), T_{∞} [°C] is the coolant temperature (conservatively assumed to be $T_{\infty,max}$), q''_c [W/m^2] is the critical heat flux, and q''_{max} [W/m^2] is the maximum heat flux of the sample (conservatively assumed as $\frac{q'_{limit}}{\pi D_{c1}}$).

It is important to note that, theoretically, if $DNBR > 1$ is achieved, $q''_{max} < q''_c$ and no departure from nucleate boiling is expected. However, it is desirable to use a lower limit that is higher than 1 during the design in order to accommodate any uncertainties or accidents. Those DNBR limits vary from one reactor to another [30], but, for INL's ATR irradiation experiments, that lower limit is 2. As such, it is recommended to maintain $DNBR > 2$.

$$FIR = \frac{T_{\infty,sat} - T_{\infty,in}}{T_{\infty,out} - T_{\infty,in}} \quad (17)$$

FIR on the other hand provides a measure of how close the coolant's temperature is to its saturation temperature. In other words, how close is the coolant to evaporating at any given pressure. The FIR calculation is performed as shown in Equation 17, where $T_{\infty,sat}$ is the saturation temperature of the water at the set operating pressure. Per the thermodynamic tables [31], researchers can find the saturation temperature at any desired pressure. $T_{\infty,in}$ and $T_{\infty,out}$ are the inlet and outlet temperatures of the coolant, where $T_{\infty,out} = T_{\infty,max}$, per the thermal analysis model implemented in TOAST. Much like DNBR, it is desirable to maintain an $FIR > 2$ to ensure safe operation with little 2-phase flow instability.

The sensitivity studies that the user is capable of performing in TOAST are in the following list, where each provides the variations in q'_{limit} (Q_{limit}/L_s), $T_{\infty,max}$, and P_{limit} as a function of the changes in the unknown parameter.

1. Sensitivity analysis with respect to D_{bi}

2. Sensitivity analysis with respect to D_{c1}
3. Sensitivity analysis with respect to D_{c2}
4. Sensitivity analysis with respect to D_s
5. Sensitivity analysis with respect to t_{bond}
 - a. Set $T_{s,limit}$
 - b. Varied $T_{s,limit}$

Each sensitivity analysis is expanded upon in the following subsections. Note that some sensitivity analyses have unique features that are not shared with the others. This differentiation is due to the current work's objectives and are not a limitation of TOAST or its potential. Any feature implemented in any of the sensitivity analyses can be implemented in all the other sensitivity analyses as well as any others that may be of interest. More sensitivity analyses can be constructed in the vein of the ones presented here (e.g., consider the analyses listed here as examples for any future sensitivity analysis framework).

3.2.1 Sensitivity analysis with respect to the basket ID (D_{bi})

The user can track changes to q'_{max} , $T_{\infty,max}$, and P_{limit} with respect to changes in D_{bi} using the automated procedure presented in Figure 7. The procedure begins by grabbing the D_{bo} and D_{c1} user-selected values, which serve as the constraints on how large and how small D_{bi} can get. Minimum thicknesses for the annulus and the basket are assumed constant in order to facilitate realistic results. These minimum thicknesses (0.8 mm for the basket and 0.1 mm for the annulus) are currently hardcoded into TOAST, but a future version may provide the user with the ability to change them manually. Another assumption is made regarding the basket material, where the S_y of the basket is assumed to be equal to that of stainless-steel 316L (170 MPa). As with the minimum thicknesses, the S_y is hardcoded into TOAST but can easily be altered in the source code. A future version of TOAST would provide the user with more control over the sensitivity studies in general. Once the assumptions are made, a minimum D_{bi} is calculated to obtain a minimum fraction with respect to the maximum allowable D_{bi} ($D_{bo} - 2t$). This fraction is used to initiate the study at the smallest possible value for D_{bi} , continuing until 99% of the maximum allowable D_{bi} is reached. Once that 99% mark is reached, two plots are generated containing the linear heat generation rate limit for the sample, the pressure limit of the basket, and the maximum coolant temperature, all as a function of D_{bi} . This provides an insight into the effects of a changing D_{bi} on the thermal-hydraulic behavior as well as its effects on the allowable pressure limits on the basket.

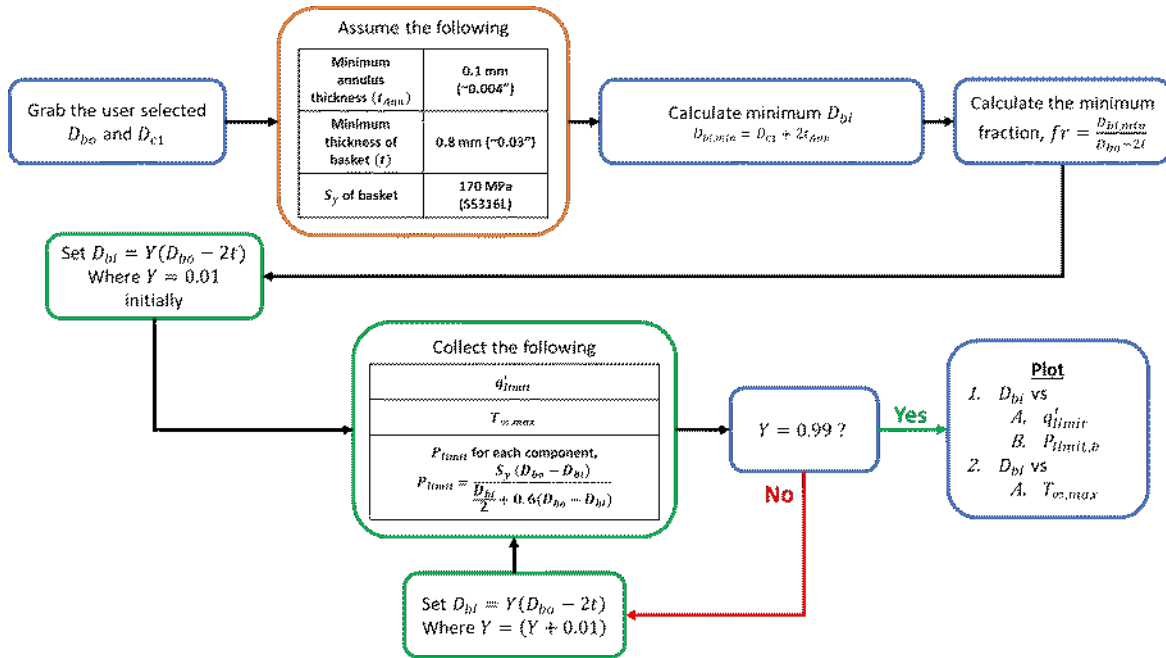


Figure 7. The automated procedure for the sensitivity analysis with respect to D_{bi} .

3.2.2 Sensitivity analysis with respect to the OD of capsule 1 (D_{c1})

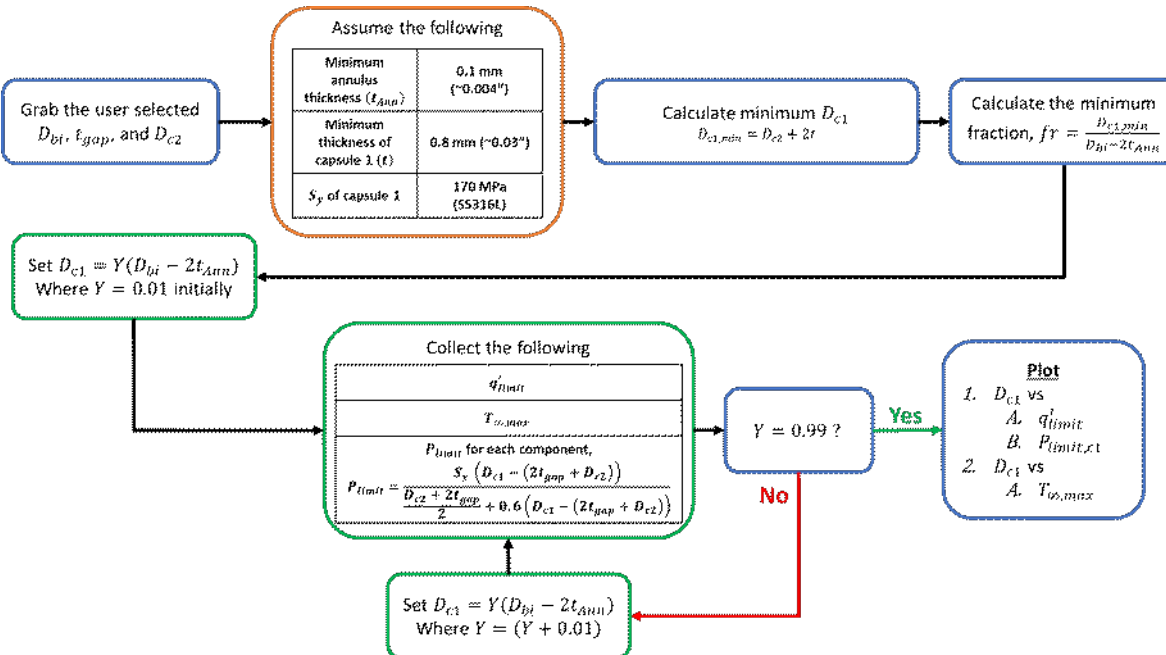


Figure 8. The automated procedure for the sensitivity analysis with respect to D_{c1} .

The procedure laid out for D_{c1} perturbations, shown in Figure 8, is very similar to that of the D_{bi} procedure with trivial differences in how the minimum D_{c1} and fraction are calculated and how the results are reported. This provides an insight into the effects of a changing D_{c1} on the thermal-hydraulic behavior as well as its effects on the allowable pressure limits on the basket.

3.2.3 Sensitivity analysis with respect to the OD of capsule 2 (D_{c2})

Like D_{bi} and D_{c1} , the procedure for D_{c2} includes the same steps with the same trivial differences between them. Figure 9 shows this procedure, which conveniently allows the user to investigate the sensitivity of the sensitive parameters (q'_{limit} , $T_{\infty,max}$, and P_{limit}) with respect to changes in D_{c2} .

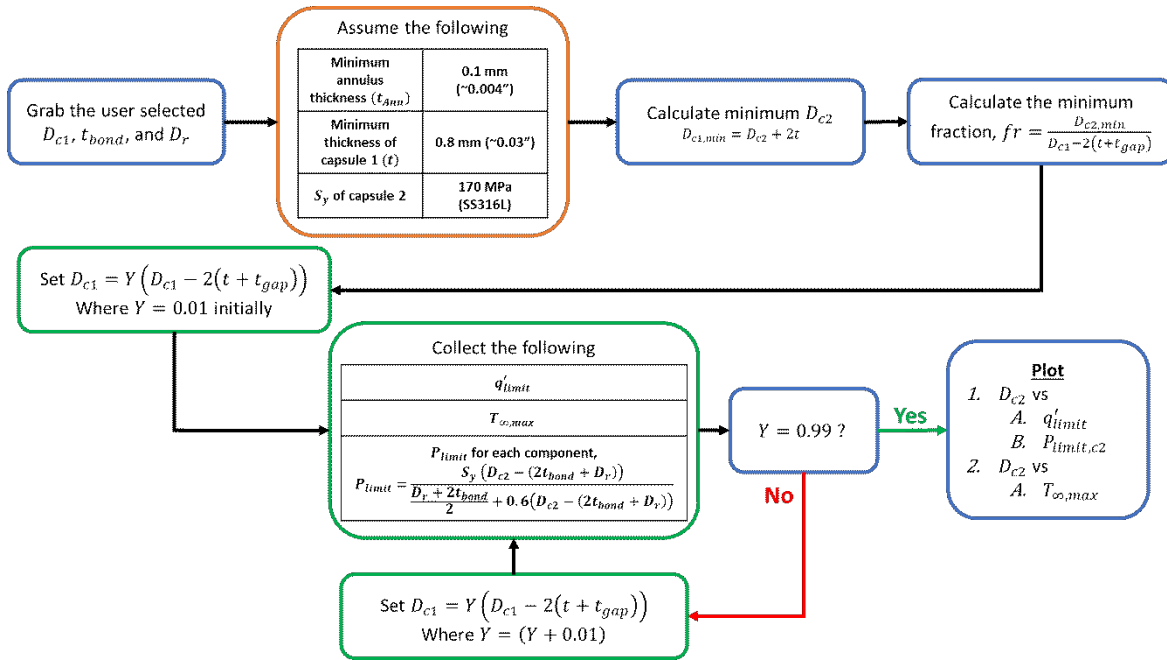


Figure 9. The automated procedure for the sensitivity analysis with respect to D_{c2} .

3.2.4 Sensitivity analysis with respect to the sample diameter (D_s)

The sample diameter sensitivity analysis procedure, shown in Figure 10, is slightly different than the past three that were introduced. For starters, the system assumes a constant thickness for all the components (capsules and rodlet clad) and calculates a maximum D_s and fraction instead of a minimum. In that sense, it starts with the smallest possible D_s (assumed to be 1% of D_{bi}) and it works its way up to 99% of the maximum D_s . Instead of calculating the P_{limit} for one component, the D_s sensitivity analysis calculates it for all the components and puts them on one plot, with the other plot containing the q'_{limit} and $T_{\infty,max}$ as functions of D_s . It should be noted that any results reported in this sensitivity analysis reflect their priority to the current work and, if needed, can be easily implemented in each of the sensitivity analyses in the future.

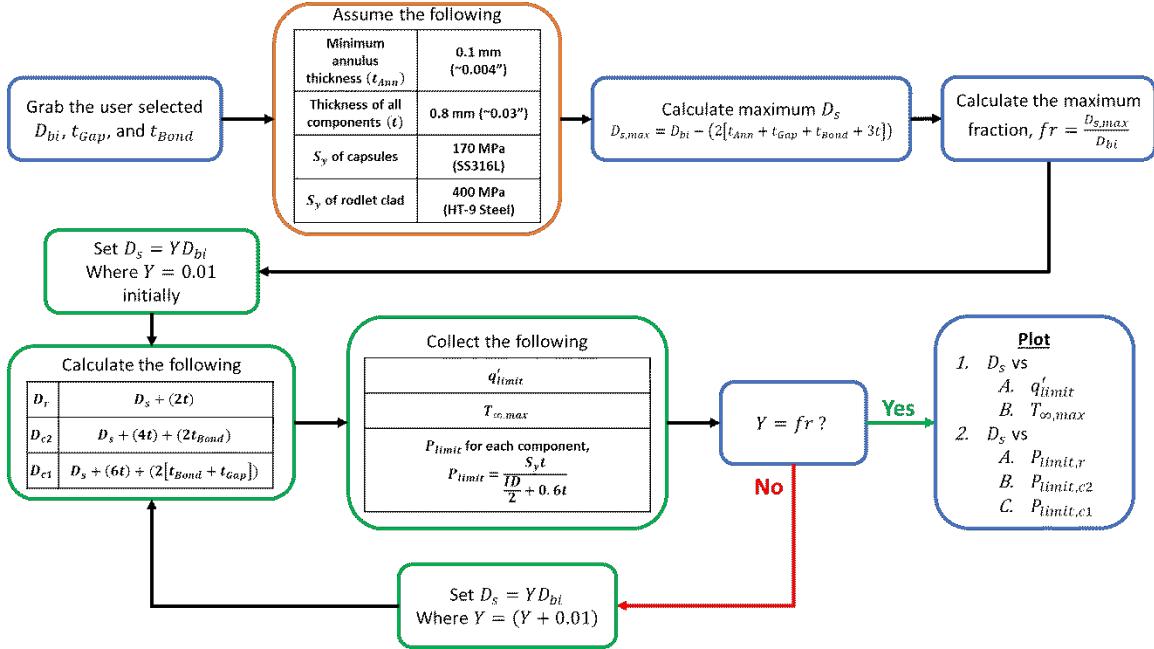


Figure 10. The automated procedure for the sensitivity analysis with respect to D_s .

3.2.5 Sensitivity analysis with respect to the bond thickness (t_{bond}) with a set sample temperature ($T_{s,limit}$)

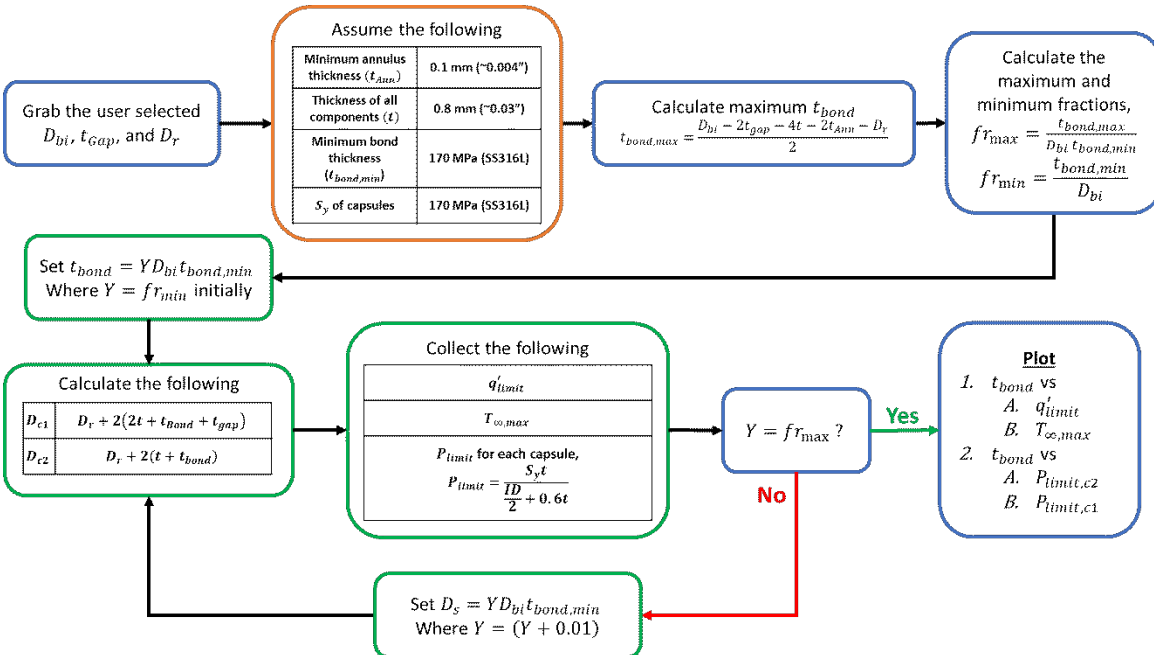


Figure 11. The automated procedure for the sensitivity analysis with respect to t_{bond} .

The t_{bond} sensitivity analysis when a set sample temperature limit ($T_{s,limit}$) is selected has a very similar procedure to that of D_s . This is shown in Figure 11, where almost the exact same steps implemented in D_s are also implemented here. An exception is how the fraction is used to step through the different t_{bond} sizes, where both a maximum and an assumed minimum for t_{bond} are used to find respective maximum and minimum fractions to bound the t_{bond} perturbations to. In essence, the t_{bond} expansion and depression is controlled by the user-provided D_{bi} , t_{gap} , D_r , and the thickness of each component (which is assumed to be constant in this work). The P_{limit} for the affected components (the capsules) are also calculated to show the user how sensitive P_{limit} is to changes in t_{bond} (which would affect the IDs of each of the capsules).

3.2.6 Sensitivity analysis with respect to the bond thickness (t_{bond}) with a varied sample temperature limit ($T_{s,limit}$)

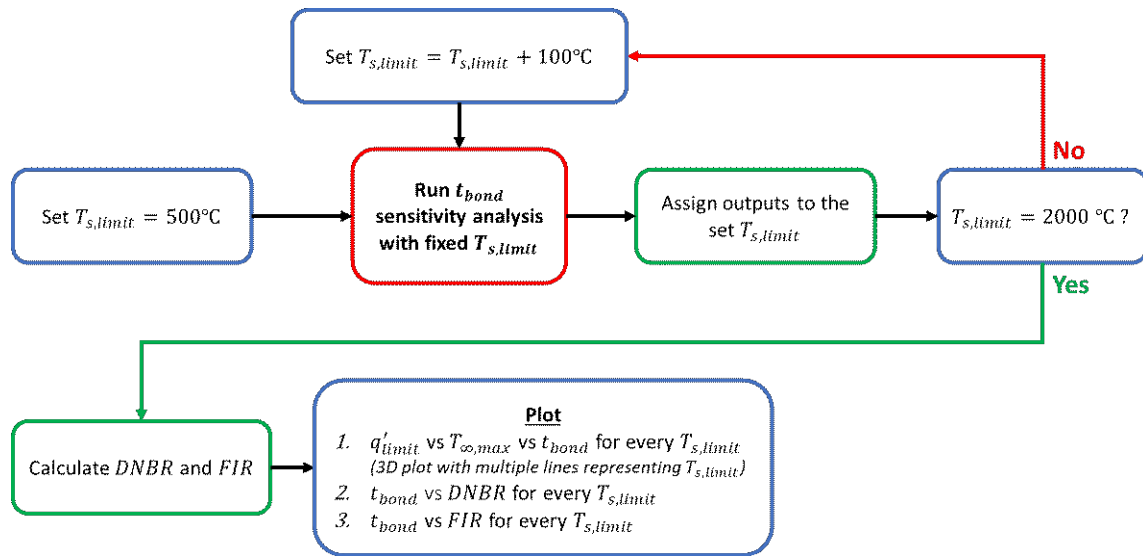


Figure 12. The automated procedure for the sensitivity analysis with respect to t_{bond} and a varied $T_{s,limit}$.

Due to the demands of this work, an additional feature was enabled for the t_{bond} sensitivity analysis, enabling the analysis to account for the effects of changing $T_{s,limit}$ by stepping through an array of values for it as well. In this procedure, shown in Figure 12, TOAST begins by setting a $T_{s,limit}$ value of 500°C and running the t_{bond} sensitivity analysis with a constant $T_{s,limit}$, as shown in Figure 11. The results are then stored in a directory specific to that selected $T_{s,limit}$ in order to assist with the postprocessing that occurs later. Once the outputs are stored appropriately, the code increases the $T_{s,limit}$ by an increment of 100°C and repeats the process until a $T_{s,limit}$ of 2000°C is reached. The postprocessing begins after this by calculating the $DNBR$ and FIR using the stored information for each temperature at all potential t_{bond} sizes. After the successful calculation of $DNBR$ and FIR , three plots are generated, the first of which is a 3D plot with $T_{\infty,max}$ on the x-axis, q'_{limit} on the y-axis, and t_{bond} on the z-axis with multiple curves plotted (each of which corresponds to a different $T_{s,limit}$). The other two plots are for the $DNBR$ and FIR respectively as a function of t_{bond} for multiple $T_{s,limit}$ values (multiple curves).

3.3 Graphical User Interface

TOAST is presented to the user via a simple and highly accessible graphical user interface (GUI) that provides flexibility when determining the specifics of the studies. The GUI consists of two tabs that are shown in Figure 13 and Figure 14, respectively, and it is created in MATLAB along with the rest of the TOAST framework. Starting with the Main Settings tab in Figure 13, the GUI consists of 11 user inputs for the geometry definition (any or none of which can be set to zero); three temperature limit inputs (for both capsules and the sample); five thermal conductivity inputs for all the components including the basket (although the basket conductivity is currently unused in this version); three flow behavior inputs (pressure, pressure drop, and inlet temperature); and one drop down menu to select the number of axial discretization points. It also includes four labels, one to provide the status of the thermal model (top left), one to provide the status of the sensitivity study that is being run (bottom left), and two labels to express the $T_{\infty,max}$ and q'_{limit} (bottom right). There are two plots in the GUI (both in the Main Settings tab): the first visualizes the user-defined geometry (top right), and the second plot shows the half-axial temperature distributions (top of coolant channel to the axial centerline) for each of the components (except for the basket, which is assumed to be negligible) and the coolant temperature. Additionally, a coolant temperature full-axial distribution (spanning the entire height of the coolant channel) is plotted on an external figure.

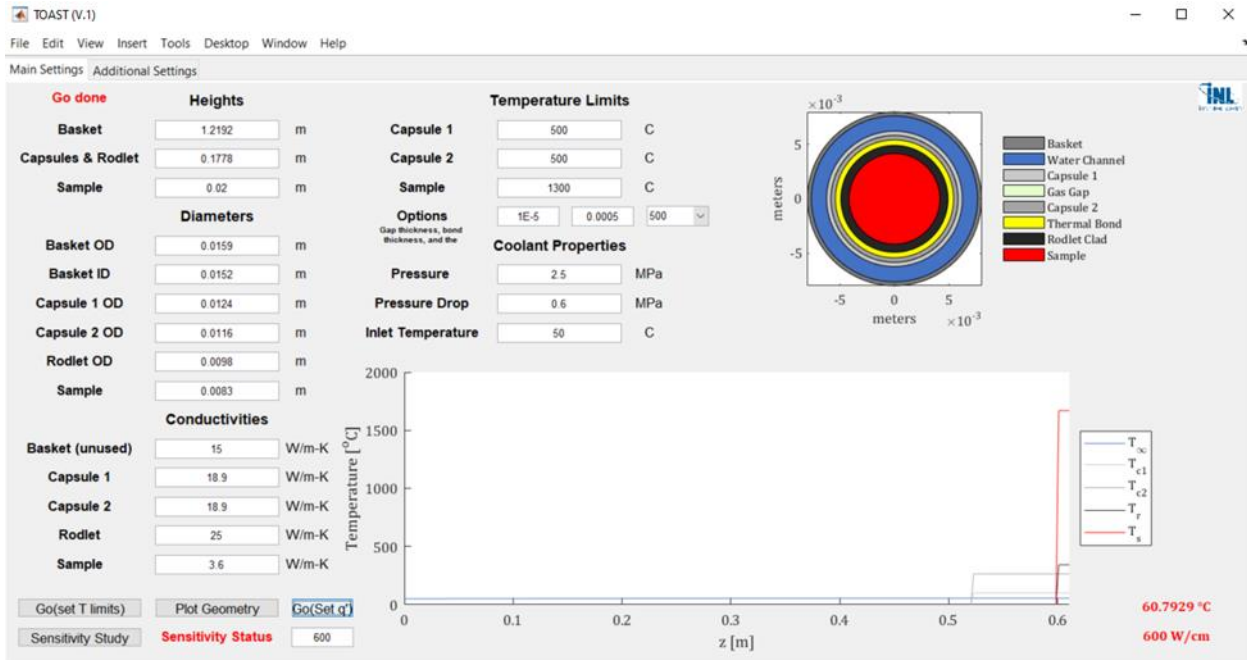


Figure 13. The Main Settings tab of the GUI for TOAST.

The user is provided with four buttons on the bottom-left portion of the Main Settings tab, each initiating a different function when pressed. The *Go (set T limits)* button allows the user to run the thermal analysis model with their selected geometry, conductivities, flow conditions, and discretization points with the set temperature limits for the capsules and the sample such that Equation 3b is used to determine the q'_{limit} . The *Go (set q')* button on the other hand allows the user to run the thermal analysis model with a predefined q'_{limit} (W/cm) in the white blank underneath the button. The *Plot Geometry* button does exactly what the name suggests in that it only plots the geometry in the top right of the Main Settings tab for visualization purposes only.

Finally, the *Sensitivity Study* button allows the user to run the sensitivity analyses described in section 3.2 of this report. This is done by having the user place a question mark symbol (?) in the white text

boxes corresponding to the sensitivity analysis of interest, which are currently limited to the *basket ID*, *capsule 1* and *capsule 2 OD* values, *Sample* diameter, *Bond thickness*, or the combination of *Bond thickness* and *Sample* temperature limits. When the user presses the *Sensitivity Study* button after placing the question mark symbol in the appropriate place(s), TOAST automatically proceeds with the sensitivity analysis of choice per the procedures laid out in section 3.2.

As mentioned earlier in Section Thermal-Hydraulic Analysis Model, the user has ability to prescribe the conductivity of any of the components as functions of their temperatures, and this is accommodated in the Additional Settings tab of the GUI, which is shown in Figure 14. The user can prescribe the constants for either a power function or a polynomial function of up to the 5th order (per Equation 5a and 5b, respectively). On this Additional Settings tab, the user can also choose the heat generation behavior by picking whether they desire a constant q'_s or a cosine-shaped q'_s . Finally, at the very bottom of the screen, the user can choose from any of the five available *Nu* correlations, where each correlation is listed in the order corresponding to Equation 8–12 such that the *Dittus-Boelter (1930)* correlation corresponds to Equation 8 and the *AWeiss (2020)* correlation corresponds to the custom correlation that is Equation 12.

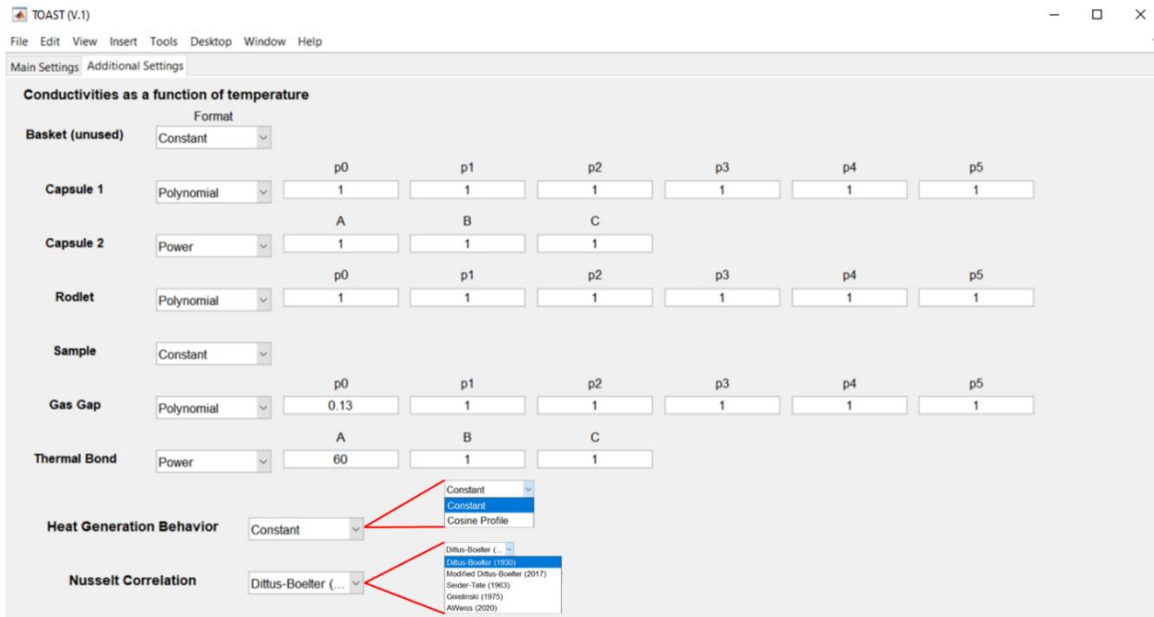


Figure 14. The Additional Settings tab of the GUI for TOAST.

It should be noted that TOAST automatically outputs the coolant axial temperature distribution and a .csv file with all the q'_{limit} and temperature distributions shown in the bottom plot of the GUI. The interests of this current work allowed the development of TOAST to be carried out in MATLAB, which allows for a variety of built-in accessibility functions, allowing any user to manually save the plots or even customize the GUI with ease. A future version of TOAST can be easily (relatively) redeveloped in more opensource or readily accessible environments, such as Python, by porting the existing MATLAB functions into Python scripts.

This concludes the description of TOAST and its capabilities, which are used in the following sections describing the benchmark (providing an uncertainty of the code) and the optimization results for the NMDQi experiments.

4. BENCHMARK

4.1 Benchmark Setup

In an effort to verify the results from TOAST for the NMDQi experiments, with which most of the future parametric and sensitivity studies shall be conducted, a set of benchmark problems were solved using TOAST and the commercial software ABAQUS. The results from TOAST are compared directly to ABAQUS to provide a better understanding of TOAST's accuracy with respect to the other two software packages. The benchmarks are inspired by previous thermal-hydraulic analyses of accident tolerant fuels (ATFs) irradiation [6] and the Advanced Fuels Campaign Fission Accelerated Steady-State Testing (AFC-FAST) thermal-hydraulic analyses [32].

The benchmarks are set up as follows, where a user-supplied constant q'_{limit} of 200, 225, 250, 275, and $300 \frac{W}{cm}$ are provided for each of the setups.

1. U-10Zr Fuel – Constant conductivities $\left(\frac{W}{m-K}\right)$
 - a. $k_{sample} = 22$
 - b. $k_r = k_{c1} = k_{c2} = 13$
 - c. $k_{gap} = 0.13$
 - d. $k_{bond} = 60$

2. U-10Zr Fuel – Variable conductivities $\left(\frac{W}{m-K}\right)$
 - a. $k_{sample} = 11.71188 + (0.01334 T) + (9.38 \times 10^{-6} T^2)$
 - b. $k_r = 29.65 - (0.06668 T) + (2.184 \times 10^{-4} T^2) - (2.527 \times 10^{-7} T^3) + (9.621 \times 10^{-11} T^5)$
 - c. $k_{c1} = k_{c2} = 8.38266 + (0.01750316 T) - (3.146906 \times 10^{-6} T^2)$
 - d. $k_{gap} = 0.06187 + (2.89714 \times 10^{-4} T)$
 - e. $k_{bond} = 111.5731 - (0.07026424 T) + (2.373302 \times 10^{-5} T^2) - (8.567 \times 10^{-9} T^3) + (2.025858 \times 10^{-12} T^4) - (2.163437 \times 10^{-16} T^5)$

The thermal conductivity function for the sample is based on a U-10Zr sample with 0% porosity, based on models suggested by Billone et al. [33]. The rodlet clad assumes an HT-9 steel material whose thermal conductivity function is suggested by Argonne National Laboratory [34]. Both capsules are assumed to be made of stainless-steel 316L with the conductivity function based on data from the works of Umezawa et al. [35] and Lucks et al. [36]. For the gas gap, we assume 100% He gas, with a thermal conductivity function from the works of Siefken et al. [37]. The thermal bond was liquid sodium, with a thermal conductivity function based on the works of Ho et al. [38]. It should be noted that all those thermal conductivity models are the ones used by the BISON [39] code package within the Multiphysics Object-Oriented Simulation Environment (MOOSE) Multiphysics framework [40].

For all the benchmarks, the following characteristics apply.

Characteristic	Value
Basket ID (D_{bi})	14.0208 mm (0.552 in)
Capsule 1 OD (D_{c1})	10.9728 mm (0.432 in)
Capsule 2 OD (D_{c2})	9.4488 mm (0.372 in)
Rodlet clad OD (D_r)	2.921 mm (0.115 in)
Sample OD (D_s)	2.4638 mm (0.097 in)
Basket length (L_{Basket})	2.1336 m (84 in)
$L_{capsules} = L_{clad} = L_{sample}$	15.6464 cm (6.16 in)
Gap thickness (t_{gap})	0.0508 mm (0.002 in)
Thermal bond thickness (t_{bond})	2.8829 mm (0.113 in)
$\Delta P_{across\ basket}$ $[U_{coolant}]$	0.08193 MPa [8.53 m/s]
Coolant pressure ($P_{coolant}$)	2.5 MPa
$T_{coolant,inlet} = T_{\infty,in}$	50 °C

The ABAQUS simulations consisted of a 2D axisymmetric model with approximately 155,000 quadrilateral heat transfer elements in the mesh, with grading in and out of the gas gap. The coolant in the simulation is modeled as a constant sink temperature with a heat transfer coefficient that is a function of the film temperature. The ABAQUS simulations are run on a local windows machine with a quad-core i7-8665U processor and 16 GB of RAM. Each ABAQUS simulation took hours to set up and <5 minutes to run on the local machine.

Results from the TOAST simulation will consider 250 axially discretized points from the top of the irradiation basket to the axial centerline. Axial and radial symmetry about the centerline is assumed. A constant heat generation profile is assumed for all benchmark cases, wherein q'_{limit} does not vary with the height of the sample. Different Nu correlations are benchmarked here as well, all of which were listed earlier with Equations 8–12 in Section Thermal-Hydraulic Analysis Model. The purpose of using different Nu correlations is to highlight the overall sensitivity of the thermal behavior to Nu variance and, therefore, the h_{∞} uncertainty. It should be noted that each computation in TOAST took anywhere between a few seconds to nearly a couple minutes to set up (versus the hours it takes for ABAQUS), and it ran within seconds (5–30 seconds depending on the user-selected number of axial discretization points) on a local machine with a 2-core i5-7200U processor and 12 GB of RAM.

4.2 Benchmark Results

The ABQUS results are compared to results from TOAST with the five different Nu correlations shown in Equations 8–12, respectively (i.e., TOAST 1 = Equation 8, TOAST 2 = Equation 9, etc.). The benchmarked temperatures are for Capsule 1's inner temperature (T_{c1}), Capsule 2's outer temperature ($T_{c2,out}$), the rodlet clad inner temperature (T_r), and the sample centerline temperature (T_s). Table 1 shows the results for the benchmarks with constant thermal conductivities, and Table 2 shows the corresponding percent difference ($\epsilon_{c1}, \epsilon_{c2,out}, \epsilon_r, \epsilon_s$) between the ABAQUS temperature results and the results from each TOAST computation. Similarly, Table 3 and Table 4 correspond to the benchmark cases with the prescribed variable thermal conductivities.

Table 1. Constant conductivity benchmarks.

Case	q'_{limit} (W/cm)	Computation	T_{c1} (°C)	$T_{c2,out}$ (°C)	T_r (°C)	T_s (°C)
1	200	ABAQUS	111.34	373.13	493.20	565.54
		TOAST 1	110.29	372.17	492.25	564.60
		TOAST 2	113.65	375.52	495.61	567.95
		TOAST 3	105.83	367.71	487.80	560.14
		TOAST 4	109.33	371.21	491.29	563.64
		TOAST 5	108.88	370.76	490.85	563.19
2	225	ABAQUS	117.03	411.54	546.62	628.01
		TOAST 1	117.72	412.33	547.43	628.82
		TOAST 2	121.40	416.01	551.11	632.49
		TOAST 3	112.77	407.39	542.49	623.87
		TOAST 4	116.66	411.28	546.37	627.76
		TOAST 5	116.40	411.01	546.11	627.49
3	250	ABAQUS	122.71	449.94	600.03	690.46
		TOAST 1	125.13	452.48	602.59	693.02
		TOAST 2	129.11	456.46	606.57	697.00
		TOAST 3	119.71	447.05	597.16	687.59
		TOAST 4	123.98	451.33	601.44	691.87
		TOAST 5	123.95	451.30	601.40	691.83
4	275	ABAQUS	128.37	488.32	653.42	752.89
		TOAST 1	132.55	492.64	657.76	757.23
		TOAST 2	136.83	496.91	662.03	761.50
		TOAST 3	126.66	486.74	651.86	751.33
		TOAST 4	131.32	491.41	656.53	756.00
		TOAST 5	131.57	491.66	656.78	756.25
5	300	ABAQUS	134.01	526.69	706.79	815.31
		TOAST 1	139.78	532.60	712.73	821.24
		TOAST 2	144.22	537.03	717.17	825.68
		TOAST 3	133.50	526.32	706.45	814.97
		TOAST 4	138.50	531.32	711.45	819.97
		TOAST 5	139.41	532.23	712.36	820.87

The constant thermal conductivity cases show that Dittus-Boelter (Equation 8) works particularly well at lower q'_{limit} values and tend to lose accuracy as the q'_{limit} increases. Modified Dittus-Boelter (Equation 9) works similarly to Dittus-Boelter with respect to increasing the q'_{limit} ; however, it leads to less accurate results, particularly at T_{c1} , which is where the coolant effect should be most noticeable and, hence, where the Nu (and h_{∞} by extension) matters the most. This indicates that the modified Dittus-Boelter correlation may not be desirable for this kind of thermal problem on account of its inaccurate h_{∞} prediction and its inaccurate depiction of the convection heat transfer between the coolant and Capsule 1 (the outer capsule).

Seider-Tate (Equation 10) tends to work inversely to the Dittus-Boelter correlations with respect to an increasing q'_{limit} . As the sample gets hotter, lower ϵ values are observed across all temperatures. It is noteworthy however that, at a lower q'_{limit} , Seider-Tate tends to be noticeably more inaccurate than all other Nu correlations. This indicates that Seider-Tate is likely a desirable Nu correlation if high q'_{limit} values are expected, as it performs best compared to its alternatives, but it is highly undesirable at lower q'_{limit} values.

Table 2. Percent difference between ABAQUS and TOAST for the constant conductivity benchmarks.

Case	q'_{limit} (W/cm)	Computation	ϵ_{c1}	$\epsilon_{c2,out}$	ϵ_r	ϵ_s
1	200	TOAST 1	-0.94%	-0.26%	-0.19%	-0.17%
		TOAST 2	2.07%	0.64%	0.49%	0.43%
		TOAST 3	-4.95%	-1.45%	-1.10%	-0.95%
		TOAST 4	-1.81%	-0.52%	-0.39%	-0.34%
		TOAST 5	-2.21%	-0.63%	-0.48%	-0.42%
2	225	TOAST 1	0.59%	0.19%	0.15%	0.13%
		TOAST 2	3.73%	1.09%	0.82%	0.71%
		TOAST 3	-3.64%	-1.01%	-0.76%	-0.66%
		TOAST 4	-0.31%	-0.06%	-0.05%	-0.04%
		TOAST 5	-0.54%	-0.13%	-0.09%	-0.08%
3	250	TOAST 1	1.97%	0.56%	0.43%	0.37%
		TOAST 2	5.22%	1.45%	1.09%	0.95%
		TOAST 3	-2.45%	-0.64%	-0.48%	-0.42%
		TOAST 4	1.04%	0.31%	0.24%	0.20%
		TOAST 5	1.01%	0.30%	0.23%	0.20%
4	275	TOAST 1	3.26%	0.88%	0.66%	0.58%
		TOAST 2	6.59%	1.76%	1.32%	1.14%
		TOAST 3	-1.33%	-0.32%	-0.24%	-0.21%
		TOAST 4	2.30%	0.63%	0.48%	0.41%
		TOAST 5	2.50%	0.68%	0.51%	0.45%
5	300	TOAST 1	4.30%	1.12%	0.84%	0.73%
		TOAST 2	7.62%	1.96%	1.47%	1.27%
		TOAST 3	-0.38%	-0.07%	-0.05%	-0.04%
		TOAST 4	3.35%	0.88%	0.66%	0.57%
		TOAST 5	4.03%	1.05%	0.79%	0.68%

Gnielinski (Equation 11), alongside the custom correlation (Equation 12) seem to be the most balanced options across all q'_{limit} values, with Gnielinski's correlation being slightly more accurate than the custom correlation. It is notable however that, just like the Dittus-Boelter and modified Dittus-Boelter correlations, the ϵ for the Gnielinski and custom correlation seems to increase with an increasing q'_{limit} but with a lower rate. This indicates that the Gnielinski and custom correlations are likely most desirable in intermediate q'_{limit} values, where higher ϵ values may be found with any other correlation.

It should be noted however that, across most of the current benchmarks, ϵ tends to not exceed 8%, which is very good considering the purpose of TOAST is to provide a quick, computationally inexpensive, and fairly accurate framework for conducting thermal analyses, particularly for optimization and programmatic studies. Moreover, the sample centerline temperature, which will almost always be the maximum temperature in the geometry, is predicted with an $\epsilon < 1\%$ across all Nu correlations, which is astonishing considering the simplified nature of TOAST. This proves TOAST's ability to perform pre- and mid-irradiation thermal safety, programmatic, and optimization analyses, particularly for typical irradiation experiments in the ATR.

Table 3. Variable conductivity benchmarks.

Case	q'_{limit} (W/cm)	Computation	T_{c1} (°C)	$T_{c2,out}$ (°C)	T_r (°C)	T_s (°C)
1	200	ABAQUS	108.13	280.64	362.04	426.20
		TOAST 1	106.61	277.75	359.26	421.65
		TOAST 2	109.87	280.29	361.83	424.07
		TOAST 3	102.30	274.39	355.85	418.45
		TOAST 4	105.68	277.03	358.52	420.96
		TOAST 5	105.25	276.69	358.18	420.64
2	225	ABAQUS	113.30	303.13	395.55	465.08
		TOAST 1	113.35	301.49	393.75	461.15
		TOAST 2	116.90	304.21	396.53	463.75
		TOAST 3	108.57	297.84	390.03	457.68
		TOAST 4	112.33	300.71	392.96	460.41
		TOAST 5	112.07	300.51	392.76	460.22
3	250	ABAQUS	118.43	325.65	428.57	503.05
		TOAST 1	120.02	324.52	427.77	499.79
		TOAST 2	123.86	327.41	430.74	502.55
		TOAST 3	114.80	320.60	423.75	496.04
		TOAST 4	118.92	323.69	426.92	498.99
		TOAST 5	118.88	323.66	426.90	498.97
4	275	ABAQUS	123.52	347.25	461.30	540.37
		TOAST 1	126.66	346.92	461.43	537.69
		TOAST 2	130.77	349.97	464.57	540.62
		TOAST 3	121.00	342.74	457.11	533.68
		TOAST 4	125.48	346.05	460.53	536.85
		TOAST 5	125.72	346.23	460.71	537.03
5	300	ABAQUS	128.57	368.31	493.73	577.06
		TOAST 1	133.06	368.61	494.63	574.83
		TOAST 2	137.31	371.71	497.86	577.82
		TOAST 3	127.05	364.23	490.09	570.62
		TOAST 4	131.84	367.71	493.71	573.97
		TOAST 5	132.71	368.35	494.37	574.58

The same trends that are observable for the constant conductivity benchmarks can be seen in the variable conductivity benchmarks with the notable exception of the strong variation in the temperature values when compared to the temperature values of the constant conductivity benchmarks. This indicates that this sort-of thermal analysis problem is highly sensitive to changes in the thermal conductivity and thus allowing the user to input a variable conductivity equation in multiple formats (power or polynomial) is an added benefit of TOAST. This also demonstrates that in this problem (i.e., any irradiation thermal analysis), the temperatures are equally if not more sensitive to variations in the thermal conductivity relative to variations in the convection heat transfer coefficient.

Once again, the sensitivity of the temperatures to convection heat transfer accuracy is shown through the different Nu correlations. While similar trends are observable in Table 4 and Table 2, it should be noted that conduction (i.e., thermal conductivities) plays an even bigger role in the accuracy of the thermal analysis, per the comparison between the temperatures in Table 1 and Table 3.

Table 4. Percent difference between ABAQUS and TOAST for the variable conductivity benchmarks.

Case	q'_{limit} (W/cm)	Computation	ϵ_{c1}	$\epsilon_{c2,out}$	ϵ_r	ϵ_s
1	200	TOAST 1	-1.40%	-1.03%	-0.77%	-1.07%
		TOAST 2	1.61%	-0.12%	-0.06%	-0.50%
		TOAST 3	-5.40%	-2.23%	-1.71%	-1.82%
		TOAST 4	-2.26%	-1.29%	-0.97%	-1.23%
		TOAST 5	-2.66%	-1.41%	-1.07%	-1.31%
2	225	TOAST 1	0.04%	-0.54%	-0.45%	-0.84%
		TOAST 2	3.18%	0.36%	0.25%	-0.29%
		TOAST 3	-4.17%	-1.75%	-1.39%	-1.59%
		TOAST 4	-0.86%	-0.80%	-0.66%	-1.00%
		TOAST 5	-1.08%	-0.86%	-0.71%	-1.04%
3	250	TOAST 1	1.34%	-0.35%	-0.19%	-0.65%
		TOAST 2	4.58%	0.54%	0.51%	-0.10%
		TOAST 3	-3.07%	-1.55%	-1.12%	-1.39%
		TOAST 4	0.41%	-0.60%	-0.38%	-0.81%
		TOAST 5	0.38%	-0.61%	-0.39%	-0.81%
4	275	TOAST 1	2.54%	-0.09%	0.03%	-0.50%
		TOAST 2	5.87%	0.78%	0.71%	0.05%
		TOAST 3	-2.04%	-1.30%	-0.91%	-1.24%
		TOAST 4	1.58%	-0.35%	-0.17%	-0.65%
		TOAST 5	1.78%	-0.29%	-0.13%	-0.62%
5	300	TOAST 1	3.49%	0.08%	0.18%	-0.39%
		TOAST 2	6.80%	0.92%	0.84%	0.13%
		TOAST 3	-1.18%	-1.11%	-0.74%	-1.12%
		TOAST 4	2.54%	-0.16%	0.00%	-0.53%
		TOAST 5	3.22%	0.01%	0.13%	-0.43%

Nonetheless, it is once again astonishing how accurate the centerline sample temperatures are predicted by TOAST (relative to ABAQUS), where $\epsilon < 2\%$ at the most.

5. CONCLUSIONS

A Thermal-Hydraulic Optimization, Analysis, and Scoping Tool (referred to as TOAST) was successfully created for easier programmatic, optimization, and sensitivity analyses, particularly towards helping fulfil the mission of the NMDQi program. TOAST was built on a semi-2D thermal analysis framework where thermal resistance networks are solved radially at multiple axial locations until the axial and radial centerline is reached, at which symmetry conditions are assumed, enabling a significant reduction in the computational expense. It resembles a steady-state 3D-axisymmetric simulation with a mesh that consists of only five radial nodes and a user-supplied number axial node (100–1000 nodes per the user's preferences). The discretization scheme adopted in TOAST allows for a more accurate calculation of the coolant temperature at different axial heights, resembling a backward difference discretization scheme. It was found that 500 axial nodes were sufficient to obtain reasonably accurate results with less than a 2% difference to results from a 3D-axisymmetric simulation in ABAQUS software.

TOAST is driven by user-supplied inputs in a highly accessible GUI that requires little-to-no thermal-hydraulic experience from the user. The GUI allows the user to perform thermal-hydraulic computations for the axial temperature profiles of each component in a cylindrical irradiation vehicle by calculating the coolant temperature alongside the temperatures of any number of capsules used, the rodlet cladding surrounding the sample, and the cylindrical sample itself. The user can supply temperature limits for the capsules and sample, or can provide a sample heat rate (constant or cosine-shaped) in order to obtain the thermal behavior. If the user does not supply a heat rate for the sample, the allowable sample heat rate will be displayed on the GUI upon its computation. The user is also able to leave certain dimensions or temperature limits as unknowns, and TOAST will be able to produce plots for the sensitivity of the sample heat rate, the maximum coolant temperature, and the ASME pressure limits of the capsules with respect to changes in the unknown parameter. This allows the user to perform sensitivity studies that would require multiple meshes and lengthy simulations in other codes anywhere between seconds and minutes (depending on the local machine's performance).

A benchmark was carried out to compare the performance of TOAST against the ABAQUS commercial software, which is highly utilized in INL for thermal-hydraulic safety and programmatic analyses. The results show that TOAST is within less than 3% of ABAQUS in most cases and a maximum of 8% difference in some computations. The benchmarks showed that this uncertainty is tied back to the appropriate selection of a Nusselt number correlation or the appropriate selection of thermal conductivity values (whether constant or variable). Nonetheless, for the purposes of programmatic and sensitivity analyses, it is a great tool due to its computational cost efficiency, its high accessibility, and its sensitivity analysis features.

6. Appendix: TOAST MATLAB Program

Each appendix subsection contains a MATLAB function or txt file that is necessary to run TOAST. Each of the 10 files (nine *.m* files and at least one *.txt* file) must be stored in the same directory. Once all the files are stored in the same directory, the TOAST GUI can be called by either running the *TOAST_GUI.m* file in MATLAB or typing *TOAST_GUI* in the MATLAB command window. Once the GUI is displayed, the user can use TOAST to its full capability. It should be noted that a lot of GUI elements (including all the buttons) can show a callout message when the user hovers their cursor over them, providing insight into the functions and limitations of each button (or some other GUI elements).

It should also be noted that, for all the sensitivity study features to work, within the same directory, the following subdirectories must be created manually and named exactly as they are named below. The *SampleStats* and *tBondStats* subdirectories are only necessary for studying the sensitivity with respect to an unknown sample diameter and an unknown bond thickness (respectively).

- Coolant_Max_Temps
- Heat_and_Pressure_Limits
- SampleStats
- tBondStats

6.1 TOAST_GUI.m

```

function TOAST_GUI
%Tab1 Elements
global Tc1_max_Label Tc2_max_Label Tinf_max_Label q_Label Stat_Go2_Label...
    Stat_Label Q_PRIME text_Tinf_in text_DP text_Pinf DISCs BondCheck...
    GapCheck text_Ts_limit text_Tc2_limit text_Tc1_limit text_kS text_kR...
    text_kC2 text_kC1 text_kB text_DS text_DR text_DC2 text_DC1 text_DBi...
    text_DBo text_LS text_LC text_LB axG axT FSize NuCor_Check
%Tab2 Elements
global QCos_Check F_kBond E_kBond D_kBond C_kBond B_kBond A_kBond...
    kBond_check F_kGap E_kGap D_kGap C_kGap B_kGap A_kGap kGap_check...
    F_kS E_kS D_kS C_kS B_kS A_kS kS_check F_kR E_kR D_kR C_kR B_kR A_kR...
    kR_check F_kC2 E_kC2 D_kC2 C_kC2 B_kC2 A_kC2 kC2_check F_kC1 E_kC1...
    D_kC1 C_kC1 B_kC1 A_kC1 kC1_check F_kB E_kB D_kB C_kB B_kB A_kB kB_check

close all
clc
MAINFIG=figure('Name','TOAST (V.1)','NumberTitle',...
    'off','units','pixels','Position',[88 67 1224 597]);
TAGR=uitabgroup(MAINFIG);
TABS(1)=uitab(TAGR,'Title','Main Settings');
TABS(2)=uitab(TAGR,'Title','Additional Settings');

% set(gcf,'Color','w')
X0=0.01; Y0=0.95; X1=0.1; Y1=0.035;
DY=0.05; DX=0.275;
FSize=10;

% %% Heights
numy=0; numx=0;
uicontrol(TABS(1),'Style','text','String','Heights','units','normalized',...
    'Position',[X0+(DX*numx)+0.11 Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize+1);

numy=numy+1;
uicontrol(TABS(1),'Style','text','String','Basket','units','normalized',...
    'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);
text_LB =
uicontrol(TABS(1),'Style','edit','String','1.2192','units','normalized','Position',[X0+(DX*numx)+
0.11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1),'Style','text','String','m','units','normalized',...
    'Position',[X0+(DX*numx)+0.21 Y0-(DY*numy) Y1 Y1],'FontSize',FSize);

numy=numy+1;
uicontrol(TABS(1),'Style','text','String','Capsules & Rodlet','units','normalized',...
    'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);
text_LC =
uicontrol(TABS(1),'Style','edit','String','0.1778','units','normalized','Position',[X0+(DX*numx)+
0.11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1),'Style','text','String','m','units','normalized',...
    'Position',[X0+(DX*numx)+0.21 Y0-(DY*numy) Y1 Y1],'FontSize',FSize);

numy=numy+1;
uicontrol(TABS(1),'Style','text','String','Sample','units','normalized',...
    'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);
text_LS =
uicontrol(TABS(1),'Style','edit','String','0.02','units','normalized','Position',[X0+(DX*numx)+0.
11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1),'Style','text','String','m','units','normalized',...
    'Position',[X0+(DX*numx)+0.21 Y0-(DY*numy) Y1 Y1],'FontSize',FSize);

% %% Diameters
numy=numy+1; numx=0;
uicontrol(TABS(1),'Style','text','String','Diameters','units','normalized',...
    'Position',[X0+(DX*numx)+0.11 Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize+1);

numy=numy+1;
uicontrol(TABS(1),'Style','text','String','Basket OD','units','normalized',...
    'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);

```

```

text_DBo =
uicontrol(TABS(1), 'Style', 'edit', 'String', '0.0159', 'units', 'normalized', 'Position', [X0+(DX*numx)+
0.11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'm', 'units', 'normalized', ...
'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Basket ID', 'units', 'normalized', ...
'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_DBi =
uicontrol(TABS(1), 'Style', 'edit', 'String', '0.0152', 'units', 'normalized', 'Position', [X0+(DX*numx)+
0.11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'm', 'units', 'normalized', ...
'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Capsule 1 OD', 'units', 'normalized', ...
'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_DC1 =
uicontrol(TABS(1), 'Style', 'edit', 'String', '0.0124', 'units', 'normalized', 'Position', [X0+(DX*numx)+
0.11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'm', 'units', 'normalized', ...
'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Capsule 2 OD', 'units', 'normalized', ...
'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_DC2 =
uicontrol(TABS(1), 'Style', 'edit', 'String', '0.0116', 'units', 'normalized', 'Position', [X0+(DX*numx)+
0.11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'm', 'units', 'normalized', ...
'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Rodlet OD', 'units', 'normalized', ...
'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_DR =
uicontrol(TABS(1), 'Style', 'edit', 'String', '0.0098', 'units', 'normalized', 'Position', [X0+(DX*numx)+
0.11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'm', 'units', 'normalized', ...
'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Sample', 'units', 'normalized', ...
'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_DS =
uicontrol(TABS(1), 'Style', 'edit', 'String', '0.0083', 'units', 'normalized', 'Position', [X0+(DX*numx)+
0.11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'm', 'units', 'normalized', ...
'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1 Y1], 'FontSize', FSize);

%% Conductivities
numy=numy+1; numx=0;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Conductivities', 'units', 'normalized', ...
'Position', [X0+(DX*numx)+0.11 Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize+1);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Basket (unused)', 'units', 'normalized', ...
'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_kB =
uicontrol(TABS(1), 'Style', 'edit', 'String', '15', 'units', 'normalized', 'Position', [X0+(DX*numx)+0.11
Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'W/m-K', 'units', 'normalized', ...
'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Capsule 1', 'units', 'normalized', ...
'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_kC1 =
uicontrol(TABS(1), 'Style', 'edit', 'String', '18.9', 'units', 'normalized', 'Position', [X0+(DX*numx)+0.
11 Y0-(DY*numy) X1 Y1]);

```

```

uicontrol(TABS(1), 'Style', 'text', 'String', 'W/m-K', 'units', 'normalized', ...
    'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Capsule 2', 'units', 'normalized', ...
    'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_kC2 =
uicontrol(TABS(1), 'Style', 'edit', 'String', '18.9', 'units', 'normalized', 'Position', [X0+(DX*numx)+0.
11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'W/m-K', 'units', 'normalized', ...
    'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Rodlet', 'units', 'normalized', ...
    'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_kR =
uicontrol(TABS(1), 'Style', 'edit', 'String', '25', 'units', 'normalized', 'Position', [X0+(DX*numx)+0.11
Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'W/m-K', 'units', 'normalized', ...
    'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Sample', 'units', 'normalized', ...
    'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_kS =
uicontrol(TABS(1), 'Style', 'edit', 'String', '3.6', 'units', 'normalized', 'Position', [X0+(DX*numx)+0.1
1 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'W/m-K', 'units', 'normalized', ...
    'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1], 'FontSize', FSize);

%% Temperature Limits
numy=0; numx=1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Temperature Limits', 'units', 'normalized', ...
    'Position', [X0+(DX*numx)+0.1 Y0-(DY*numy) X1+0.02
Y1], 'FontWeight', 'bold', 'FontSize', FSize+1);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Capsule 1', 'units', 'normalized', ...
    'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_Tc1_limit =
uicontrol(TABS(1), 'Style', 'edit', 'String', '500', 'units', 'normalized', 'Position', [X0+(DX*numx)+0.1
1 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'C', 'units', 'normalized', ...
    'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Capsule 2', 'units', 'normalized', ...
    'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_Tc2_limit =
uicontrol(TABS(1), 'Style', 'edit', 'String', '500', 'units', 'normalized', 'Position', [X0+(DX*numx)+0.1
1 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'C', 'units', 'normalized', ...
    'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1], 'FontSize', FSize);

numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Sample', 'units', 'normalized', ...
    'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
text_Ts_limit =
uicontrol(TABS(1), 'Style', 'edit', 'String', '1300', 'units', 'normalized', 'Position', [X0+(DX*numx)+0.
11 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1), 'Style', 'text', 'String', 'C', 'units', 'normalized', ...
    'Position', [X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1], 'FontSize', FSize);

%Options row
numy=numy+1;
uicontrol(TABS(1), 'Style', 'text', 'String', 'Options', 'units', 'normalized', ...
    'Position', [X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight', 'bold', 'FontSize', FSize);
uicontrol(TABS(1), 'Style', 'text', 'String', 'Gap thickness, bond thickness, and the
discretization', 'units', 'normalized', ...
    'Position', [X0+(DX*numx) Y0-(DY*numy)-0.03 X1 Y1], 'FontWeight', 'bold', 'FontSize', 6);
%% Gap Check

```

```

hint1=['Assumes gas gap filled with Helium and 20% argon fraction, with the set thickness [m]
(can be zero)',newline,'Located between the capsules 1 and 2',newline,...
'k(T)=0.00020347396*T + 0.0423552'];
GapCheck = uicontrol(TABS(1),'Style','edit','String','1E-5','units','normalized',...
'Position',[X0+(DX*numx)+0.11 Y0-(DY*numy) X1/2 Y1],'TooltipString',hint1);

% %% Thermal bond thickness
hint1=['Assumes liquid sodium bond with the set thickness [m] (can be zero)',newline,'Located
between capsule 2 and the rodlet',newline,...
'k(T)=111.5731-(0.07026424*T)+(T^2 * 2.373302E-5)-(T^3 * 8.567E-9)+(T^4 * 2.025858E-12)-(T^5
* 2.163437E-16)'];
BondCheck = uicontrol(TABS(1),'Style','edit','String','0.0005','units','normalized',...
'Position',[X0+(DX*numx)+0.17 Y0-(DY*numy) X1/2 Y1],'TooltipString',hint1);

% %% # of discretizations text field
hint1=['Number of Discretized points along the entire height of the basket'...
,newline,'(Mesh size)'];
DISCs =
uicontrol(TABS(1),'Style','popupmenu','String',{'100','200','300','400','500','600','700','800','
900','1000'},'units','normalized',...
'Position',[X0+(DX*numx)+0.23 Y0-(DY*numy)+0.002 X1/2 Y1],'Value',1,'TooltipString',hint1);

% %% Coolant Properties
numy=numy+1; numx=1;
uicontrol(TABS(1),'Style','text','String','Coolant Properties','units','normalized',...
'Position',[X0+(DX*numx)+0.1 Y0-(DY*numy) X1+0.02
Y1],'FontWeight','bold','FontSize',FSize+1);

numy=numy+1;
uicontrol(TABS(1),'Style','text','String','Pressure (constant)','units','normalized',...
'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);
text_Pinf =
uicontrol(TABS(1),'Style','edit','String','2.5','units','normalized','Position',[X0+(DX*numx)+0.1
1 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1),'Style','text','String','MPa','units','normalized',...
'Position',[X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1],'FontSize',FSize);

numy=numy+1;
uicontrol(TABS(1),'Style','text','String','Pressure Drop','units','normalized',...
'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);
text_DP =
uicontrol(TABS(1),'Style','edit','String','0.6','units','normalized','Position',[X0+(DX*numx)+0.1
1 Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1),'Style','text','String','MPa','units','normalized',...
'Position',[X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1],'FontSize',FSize);

numy=numy+1;
uicontrol(TABS(1),'Style','text','String','Inlet Temperature','units','normalized',...
'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);
text_Tinf_in =
uicontrol(TABS(1),'Style','edit','String','50','units','normalized','Position',[X0+(DX*numx)+0.11
Y0-(DY*numy) X1 Y1]);
uicontrol(TABS(1),'Style','text','String','C','units','normalized',...
'Position',[X0+(DX*numx)+0.21 Y0-(DY*numy) Y1+0.01 Y1],'FontSize',FSize);

% %% Plots
axG=axes(TABS(1),'Position',[0.62 0.65 0.3 0.3],'Visible','off'); %Geometry Plot
axT=axes(TABS(1),'Position',[0.32 0.1 0.6 0.4],'Visible','off'); %Axial Temps Plot
axes(TABS(1),'Position',[0.95 0.95 0.05 0.05]); imshow('INL_Logo.jpg'); %Logo

% %% Buttons
%Go Button
numx=0; numy=17.5;
hint1=['This generates axial temperature distributions from the top of basket to the sample
centerline',...
newline,'The results are displayed on the big axis (bottom-right axis)'];
GoButton = uicontrol(TABS(1),'Style','pushbutton','string','Go(set T limits)',...
'units','normalized','position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontSize',FSize,...
'TooltipString',hint1);
set(GoButton,'callback',{@Go});

```



```

%Go2 Button
numx=0; numy=18.5;
hint1=['This performs the functions of Go(set T limits), but also alters any ONE of the following
diameters to generate q'' plots as a function of changing diameter',...
newline,' - Basket ID',newline,' - Capsule 1 OD',newline,' - Capsule 2 OD',newline,' - Sample
OD',...
newline,'The sensitivity analysis results are plotted in separate pop-up figures'];
Go2Button = uicontrol(TABS(1),'Style','pushbutton','string','Sensitivity Study',...
'units','normalized','position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontSize',FSize,...
'TooltipString',hint1);
set(Go2Button,'callback',{@Go2});

%Plot Geometry Button
numx=0.4; numy=17.5;
hint1=['This plots the geometry radially',...
newline,'The results are displayed on the small axis (top-right axis)'];
PlotGeoButton = uicontrol(TABS(1),'Style','pushbutton','string','Plot Geometry',...
'units','normalized','position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontSize',FSize,...
'TooltipString',hint1);
set(PlotGeoButton,'callback',{@PlotGeo});

%Go3
numx=0.8; numy=17.5;
hint1=['This calculates the temperatures everywhere based on a set heat limit (below)',...
newline,'(disregards capsules and sample temperature limits)'];
Go3Button = uicontrol(TABS(1),'Style','pushbutton','string','Go(Set q'')',...
'units','normalized','position',[X0+(DX*numx) Y0-(DY*numy) X1/2 Y1],'FontSize',FSize,...
'TooltipString',hint1);
set(Go3Button,'callback',{@Go3});
numy=18.5;
hint1='q'' of the sample [W/cm]';
Q_PRIME = uicontrol(TABS(1),'Style','edit','String','600','units','normalized',...
'Position',[X0+(DX*numx) Y0-(DY*numy) X1/2 Y1],'TooltipString',hint1);

% %% Labels
%General Status Label
numx=0; numy=-0.1;
MES='Status';
Stat_Label=uicontrol(TABS(1),'Style','text','String',MES,'units','normalized','ForegroundColor','r',...
'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);

%Go2 Status Label
numx=0.4; numy=18.5;
Stat_Go2_Label=uicontrol(TABS(1),'Style','text','String','Sensitivity
Status','units','normalized','ForegroundColor','r',...
'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);

%q'min Label
numx=3.2; numy=18.5;
MES='q'' limit';
q_Label=uicontrol(TABS(1),'Style','text','String',MES,'units','normalized','ForegroundColor','r',...
'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);

%max Tinf Label
numx=3.2; numy=17.5;
Tinf_max_Label = uicontrol(TABS(1),'Style','text','String','max
Tinf','units','normalized','ForegroundColor','r',...
'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);

%Tc1 and Tc2 labels (invisible)
numx=3.2; numy=8;
Tc1_max_Label = uicontrol(TABS(1),'Style','text','String','max Tc1','units',...
'normalized','Position',[X0+(DX*numx) Y0-(DY*numy) 0.001 0.001]);
Tc2_max_Label = uicontrol(TABS(1),'Style','text','String','max Tc2','units',...
'normalized','Position',[X0+(DX*numx) Y0-(DY*numy) 0.001 0.001]);

% %%Additional Settings Tab%% %

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X0=0.01; Y0=0.95; X1=0.1; Y1=0.035;
DY=0.05; DX=0.275;
FSize=10;

%%% Conductivities Additional Settings
numy=0; numx=0;
uicontrol(TABS(2), 'Style','text','String','Conductivities as a function of
temperature','units','normalized',...
    'Position',[X0+(DX*numx)+0.005 Y0-(DY*numy*0.5) X1*3
Y1], 'FontWeight','bold','FontSize',FSize+1,'HorizontalAlignment','left');
uicontrol(TABS(2), 'Style','text','String','Format','units','normalized',...
    'Position',[X0+(DX*numx)+0.12 Y0-(DY*(numy+0.8)) X1 Y1], 'FontSize',FSize);

numy=numy+1.5;
uicontrol(TABS(2), 'Style','text','String','Basket (unused)','units','normalized',...
    'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight','bold','FontSize',FSize);
kB_check =
uicontrol(TABS(2), 'Style','popupmenu','String',{'Constant','Polynomial','Power'}, 'units','normali
zed',...
    'Position',[X0+(DX*numx)+0.12 Y0-(DY*numy) X1
Y1], 'FontSize',FSize,'Callback',@kBCHECKER);
A_kB_lab=uicontrol(TABS(2), 'Style','text','String','p0','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
A_kB_lab2=uicontrol(TABS(2), 'Style','text','String','A','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
A_kB=uicontrol(TABS(2), 'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*numy) X1 Y1], 'FontSize',FSize,'Visible','off');
B_kB_lab=uicontrol(TABS(2), 'Style','text','String','p1','units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
B_kB_lab2=uicontrol(TABS(2), 'Style','text','String','B','units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
B_kB=uicontrol(TABS(2), 'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*numy) X1 Y1], 'FontSize',FSize,'Visible','off');
C_kB_lab=uicontrol(TABS(2), 'Style','text','String','p2','units','normalized',...
    'Position',[X0+(DX*0)+0.45 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
C_kB_lab2=uicontrol(TABS(2), 'Style','text','String','C','units','normalized',...
    'Position',[X0+(DX*0)+0.45 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
C_kB=uicontrol(TABS(2), 'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.45 Y0-(DY*numy) X1 Y1], 'FontSize',FSize,'Visible','off');
D_kB_lab=uicontrol(TABS(2), 'Style','text','String','p3','units','normalized',...
    'Position',[X0+(DX*0)+0.56 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
D_kB=uicontrol(TABS(2), 'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.56 Y0-(DY*numy) X1 Y1], 'FontSize',FSize,'Visible','off');
E_kB_lab=uicontrol(TABS(2), 'Style','text','String','p4','units','normalized',...
    'Position',[X0+(DX*0)+0.67 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
E_kB=uicontrol(TABS(2), 'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.67 Y0-(DY*numy) X1 Y1], 'FontSize',FSize,'Visible','off');
F_kB_lab=uicontrol(TABS(2), 'Style','text','String','p5','units','normalized',...
    'Position',[X0+(DX*0)+0.78 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
F_kB=uicontrol(TABS(2), 'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.78 Y0-(DY*numy) X1 Y1], 'FontSize',FSize,'Visible','off');

numy=numy+2;
uicontrol(TABS(2), 'Style','text','String','Capsule 1','units','normalized',...
    'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1], 'FontWeight','bold','FontSize',FSize);
kC1_check =
uicontrol(TABS(2), 'Style','popupmenu','String',{'Const','Polynomial','Power'}, 'units','normali
zed',...
    'Position',[X0+(DX*numx)+0.12 Y0-(DY*numy) X1
Y1], 'FontSize',FSize,'Callback',@kC1CHECKER);
A_kC1_lab=uicontrol(TABS(2), 'Style','text','String','p0','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
A_kC1_lab2=uicontrol(TABS(2), 'Style','text','String','A','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
A_kC1=uicontrol(TABS(2), 'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*numy) X1 Y1], 'FontSize',FSize,'Visible','off');
B_kC1_lab=uicontrol(TABS(2), 'Style','text','String','p1','units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
B_kC1_lab2=uicontrol(TABS(2), 'Style','text','String','B','units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*(numy-0.8)) X1 Y1], 'FontSize',FSize,'Visible','off');
B_kC1=uicontrol(TABS(2), 'Style','edit','String',1,'units','normalized',...

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kGap_check =
uicontrol(TABS(2), 'Style','popupmenu','String',{'Constant','Polynomial','Power'},'units',{'normalized',...
    'Position',[X0+(DX*numx)+0.12 Y0-(DY*numy) X1
Y1],'FontSize',FSize,'Callback',@kGapCHECKER);
A_kGap_lab0=uicontrol(TABS(2),'Style','text','String','kGap','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','on');
A_kGap_lab=uicontrol(TABS(2),'Style','text','String','p0','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
A_kGap_lab2=uicontrol(TABS(2),'Style','text','String','A','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
A_kGap=uicontrol(TABS(2),'Style','edit','String',0.13,'units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','on');
B_kGap_lab=uicontrol(TABS(2),'Style','text','String','p1','units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
B_kGap_lab2=uicontrol(TABS(2),'Style','text','String','B','units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
B_kGap=uicontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');
C_kGap_lab=uicontrol(TABS(2),'Style','text','String','p2','units','normalized',...
    'Position',[X0+(DX*0)+0.45 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
C_kGap_lab2=uicontrol(TABS(2),'Style','text','String','C','units','normalized',...
    'Position',[X0+(DX*0)+0.45 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
C_kGap=uicontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.45 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');
D_kGap_lab=uicontrol(TABS(2),'Style','text','String','p3','units','normalized',...
    'Position',[X0+(DX*0)+0.56 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
D_kGap=uicontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.56 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');
E_kGap_lab=uicontrol(TABS(2),'Style','text','String','p4','units','normalized',...
    'Position',[X0+(DX*0)+0.67 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
E_kGap=uicontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.67 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');
F_kGap_lab=uicontrol(TABS(2),'Style','text','String','p5','units','normalized',...
    'Position',[X0+(DX*0)+0.78 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
F_kGap=uicontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.78 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');

numy=numy+2;
uicontrol(TABS(2),'Style','text','String','Thermal Bond','units','normalized',...
    'Position',[X0+(DX*numx) Y0-(DY*numy) X1 Y1],'FontWeight','bold','FontSize',FSize);
kBond_check =
uicontrol(TABS(2), 'Style','popupmenu','String',{'Constant','Polynomial','Power'},'units',{'normalized',...
    'Position',[X0+(DX*numx)+0.12 Y0-(DY*numy) X1
Y1],'FontSize',FSize,'Callback',@kBondCHECKER);
A_kBond_lab0=uicontrol(TABS(2),'Style','text','String','kBond','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','on');
A_kBond_lab=uicontrol(TABS(2),'Style','text','String','p0','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
A_kBond_lab2=uicontrol(TABS(2),'Style','text','String','A','units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
A_kBond=uicontrol(TABS(2),'Style','edit','String',60,'units','normalized',...
    'Position',[X0+(DX*0)+0.23 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','on');
B_kBond_lab=uicontrol(TABS(2),'Style','text','String','p1','units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
B_kBond_lab2=uicontrol(TABS(2),'Style','text','String','B','units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
B_kBond=uicontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.34 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');
C_kBond_lab=uicontrol(TABS(2),'Style','text','String','p2','units','normalized',...
    'Position',[X0+(DX*0)+0.45 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
C_kBond_lab2=uicontrol(TABS(2),'Style','text','String','C','units','normalized',...
    'Position',[X0+(DX*0)+0.45 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
C_kBond=uicontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.45 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');
D_kBond_lab=uicontrol(TABS(2),'Style','text','String','p3','units','normalized',...
    'Position',[X0+(DX*0)+0.56 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
D_kBond=uicontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.56 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');
E_kBond_lab=uicontrol(TABS(2),'Style','text','String','p4','units','normalized',...

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    'Position',[X0+(DX*0)+0.67 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
E_kBond=icontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.67 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');
F_kBond_lab=icontrol(TABS(2),'Style','text','String','p5','units','normalized',...
    'Position',[X0+(DX*0)+0.78 Y0-(DY*(numy-0.8)) X1 Y1],'FontSize',FSize,'Visible','off');
F_kBond=icontrol(TABS(2),'Style','edit','String',1,'units','normalized',...
    'Position',[X0+(DX*0)+0.78 Y0-(DY*numy) X1 Y1],'FontSize',FSize,'Visible','off');

numy=numy+2.5;
uicontrol(TABS(2),'Style','text','String','Heat Generation Behavior','units','normalized',...
    'Position',[X0+(DX*numx) Y0-(DY*numy) X1*2 Y1],'FontWeight','bold','FontSize',FSize+1);
QCos_Check = uicontrol(TABS(2),'Style','popupmenu','String',{'Constant','Cosine
Profile'},'units','normalized',...
    'Position',[X0+(DX*numx)+0.2 Y0-(DY*numy) X1 Y1],'FontSize',FSize);

numy=numy+2;
uicontrol(TABS(2),'Style','text','String','Nusselt Correlation','units','normalized',...
    'Position',[X0+(DX*numx) Y0-(DY*numy) X1*2 Y1],'FontWeight','bold','FontSize',FSize+1);
NuCor_Check = uicontrol(TABS(2),'Style','popupmenu','String',{'Dittus-Boelter (1930)','Modified
Dittus-Boelter (2017)','Seider-Tate (1963)', 'Gnielinski (1975)', 'AWeiss
(2020)'},'units','normalized',...
    'Position',[X0+(DX*numx)+0.2 Y0-(DY*numy) X1 Y1],'FontSize',FSize);

function kBCHECKER(~,~,~)
    switch kB_check.Value
        case 1

set([A_kB,B_kB,C_kB,D_kB,E_kB,F_kB,A_kB_lab,A_kB_lab2,B_kB_lab,B_kB_lab2,C_kB_lab,C_kB_lab2,D_kB_
lab,E_kB_lab,F_kB_lab],'Visible','off')
        case 2

set([A_kB,B_kB,C_kB,D_kB,E_kB,F_kB,A_kB_lab,B_kB_lab,C_kB_lab,D_kB_lab,E_kB_lab,F_kB_lab],'Visibl
e','on')
            set([A_kB_lab2,B_kB_lab2,C_kB_lab2],'Visible','off')
        case 3
            set([A_kB,B_kB,C_kB,A_kB_lab2,B_kB_lab2,C_kB_lab2],'Visible','on')

set([D_kB,E_kB,F_kB,A_kB_lab,B_kB_lab,C_kB_lab,D_kB_lab,E_kB_lab,F_kB_lab],'Visible','off')
        end
    end
function kC1CHECKER(~,~,~)
    switch kC1_check.Value
        case 1

set([A_kC1,B_kC1,C_kC1,D_kC1,E_kC1,F_kC1,A_kC1_lab,A_kC1_lab2,B_kC1_lab,B_kC1_lab2,C_kC1_lab,C_kC
1_lab2,D_kC1_lab,E_kC1_lab,F_kC1_lab],'Visible','off')
        case 2

set([A_kC1,B_kC1,C_kC1,D_kC1,E_kC1,F_kC1,A_kC1_lab,B_kC1_lab,C_kC1_lab,D_kC1_lab,E_kC1_lab,F_kC1_
lab],'Visible','on')
            set([A_kC1_lab2,B_kC1_lab2,C_kC1_lab2],'Visible','off')
        case 3
            set([A_kC1,B_kC1,C_kC1,A_kC1_lab2,B_kC1_lab2,C_kC1_lab2],'Visible','on')

set([D_kC1,E_kC1,F_kC1,A_kC1_lab,B_kC1_lab,C_kC1_lab,D_kC1_lab,E_kC1_lab,F_kC1_lab],'Visible','of
f')
        end
    end
function kC2CHECKER(~,~,~)
    switch kC2_check.Value
        case 1

set([A_kC2,B_kC2,C_kC2,D_kC2,E_kC2,F_kC2,A_kC2_lab,A_kC2_lab2,B_kC2_lab,B_kC2_lab2,C_kC2_lab,C_kC
2_lab2,D_kC2_lab,E_kC2_lab,F_kC2_lab],'Visible','off')
        case 2

set([A_kC2,B_kC2,C_kC2,D_kC2,E_kC2,F_kC2,A_kC2_lab,B_kC2_lab,C_kC2_lab,D_kC2_lab,E_kC2_lab,F_kC2_
lab],'Visible','on')
            set([A_kC2_lab2,B_kC2_lab2,C_kC2_lab2],'Visible','off')
        case 3
            set([A_kC2,B_kC2,C_kC2,A_kC2_lab2,B_kC2_lab2,C_kC2_lab2],'Visible','on')

```

```

set([D_kC2,E_kC2,F_kC2,A_kC2_lab,B_kC2_lab,C_kC2_lab,D_kC2_lab,E_kC2_lab,F_kC2_lab], 'Visible', 'off')
    end
end
function kRCHECKER(~,~,~)
    switch kR_check.Value
        case 1

set([A_kR,B_kR,C_kR,D_kR,E_kR,F_kR,A_kR_lab,A_kR_lab2,B_kR_lab,B_kR_lab2,C_kR_lab,C_kR_lab2,D_kR_lab,E_kR_lab,F_kR_lab], 'Visible', 'off')
        case 2

set([A_kR,B_kR,C_kR,D_kR,E_kR,F_kR,A_kR_lab,B_kR_lab,C_kR_lab,D_kR_lab,E_kR_lab,F_kR_lab], 'Visible', 'on')
            set([A_kR_lab2,B_kR_lab2,C_kR_lab2], 'Visible', 'off')
        case 3
            set([A_kR,B_kR,C_kR,A_kR_lab2,B_kR_lab2,C_kR_lab2], 'Visible', 'on')

set([D_kR,E_kR,F_kR,A_kR_lab,B_kR_lab,C_kR_lab,D_kR_lab,E_kR_lab,F_kR_lab], 'Visible', 'off')
    end
end
function kSCHECKER(~,~,~)
    switch kS_check.Value
        case 1

set([A_kS,B_kS,C_kS,D_kS,E_kS,F_kS,A_kS_lab,A_kS_lab2,B_kS_lab,B_kS_lab2,C_kS_lab,C_kS_lab2,D_kS_lab,E_kS_lab,F_kS_lab], 'Visible', 'off')
        case 2

set([A_kS,B_kS,C_kS,D_kS,E_kS,F_kS,A_kS_lab,B_kS_lab,C_kS_lab,D_kS_lab,E_kS_lab,F_kS_lab], 'Visible', 'on')
            set([A_kS_lab2,B_kS_lab2,C_kS_lab2], 'Visible', 'off')
        case 3
            set([A_kS,B_kS,C_kS,A_kS_lab2,B_kS_lab2,C_kS_lab2], 'Visible', 'on')

set([D_kS,E_kS,F_kS,A_kS_lab,B_kS_lab,C_kS_lab,D_kS_lab,E_kS_lab,F_kS_lab], 'Visible', 'off')
    end
end
function kGapCHECKER(~,~,~)
    switch kGap_check.Value
        case 1

set([A_kGap,B_kGap,C_kGap,D_kGap,E_kGap,F_kGap,A_kGap_lab0,A_kGap_lab,A_kGap_lab2,B_kGap_lab,B_kGap_lab2,C_kGap_lab,C_kGap_lab2,D_kGap_lab,E_kGap_lab,F_kGap_lab], 'Visible', 'off')
            set([A_kGap,A_kGap_lab0], 'Visible', 'on')
        case 2

set([A_kGap,B_kGap,C_kGap,D_kGap,E_kGap,F_kGap,A_kGap_lab,B_kGap_lab,C_kGap_lab,D_kGap_lab,E_kGap_lab,F_kGap_lab], 'Visible', 'on')
            set([A_kGap_lab0,A_kGap_lab2,B_kGap_lab2,C_kGap_lab2], 'Visible', 'off')
        case 3
            set([A_kGap,B_kGap,C_kGap,A_kGap_lab2,B_kGap_lab2,C_kGap_lab2], 'Visible', 'on')

set([D_kGap,E_kGap,F_kGap,A_kGap_lab0,A_kGap_lab,B_kGap_lab,C_kGap_lab,D_kGap_lab,E_kGap_lab,F_kGap_lab], 'Visible', 'off')
    end
end
function kBondCHECKER(~,~,~)
    switch kBond_check.Value
        case 1

set([A_kBond,B_kBond,C_kBond,D_kBond,E_kBond,F_kBond,A_kBond_lab0,A_kBond_lab,A_kBond_lab2,B_kBond_lab,B_kBond_lab2,C_kBond_lab,C_kBond_lab2,D_kBond_lab,E_kBond_lab,F_kBond_lab], 'Visible', 'off')
            set([A_kBond,A_kBond_lab0], 'Visible', 'on')
        case 2

set([A_kBond,B_kBond,C_kBond,D_kBond,E_kBond,F_kBond,A_kBond_lab,B_kBond_lab,C_kBond_lab,D_kBond_lab,E_kBond_lab,F_kBond_lab], 'Visible', 'on')
            set([A_kBond_lab0,A_kBond_lab2,B_kBond_lab2,C_kBond_lab2], 'Visible', 'off')
        case 3

```

```
set([A_kBond,B_kBond,C_kBond,A_kBond_lab2,B_kBond_lab2,C_kBond_lab2],'Visible','on')

set([D_kBond,E_kBond,F_kBond,A_kBond_lab0,A_kBond_lab,B_kBond_lab,C_kBond_lab,D_kBond_lab,E_kBond_lab,F_kBond_lab],'Visible','off')
    end
end

end
```


6.2 Go.m

```

function Go(~,~,~)
%Tab1 Elements
global Tc1_max_Label Tc2_max_Label Tinf_max_Label q_Label Stat_Label...
    text_Tinf_in text_DP text_Pinf DISCs BondCheck GapCheck text_Ts_limit...
    text_Tc2_limit text_Tc1_limit text_kS text_kR text_kC2 text_kC1...
    text_kB text_DS text_DR text_DC2 text_DC1 text_DBi text_DBo NuCor_Check...
    text_LS text_LC text_LB axT FSize x0 c LocS_Cent kC1 kGap kC2 kBond kR kS
%Tab2 Elements
global A_kBond A_kGap

set(Stat_Label, 'String', 'Go Running');

%Lengths of components [m]
LB=str2double(get(text_LB, 'String')); %Basket length (Active fuel height [Dwg: 606951])
LC=str2double(get(text_LC, 'String')); %Capsule 1 length = Capsule 2 length = Rodlet clad length
LS=str2double(get(text_LS, 'String')); %Sample length
L=[LB LC LS];

LocS_Cent=0.5*L(1); %Sample axial centerline location
LocS_Top=LocS_Cent-(L(end)/2); %Sample top location
LocC_Top=LocS_Cent-(L(2)/2); %Capsule1/Capsule2/Rodlet top location

dx=str2double(DISCs.String(DISCs.Value)); %Axial discretizations (number of points the geometry
is seperated into, axially)
z=linspace(0,L(1),dx); %Top (z=0) to bottom (z=Length of basket)
dz=abs(z(2)-z(1)); %Spacing between each axial point

DBo=str2double(get(text_DBo, 'String')); %Basket OD (constant)
DBi=str2double(get(text_DBi, 'String')); %Basket ID
DC1=str2double(get(text_DC1, 'String')); %Capsule 1 OD (variable)
DC2=str2double(get(text_DC2, 'String')); %Capsule 1 ID = Capsule 2 OD
DR=str2double(get(text_DR, 'String')); %Capsule 2 ID = Rodlet clad OD
DS=str2double(get(text_DS, 'String')); %Sample OD = Rodlet clad ID
D=[DBo DBi DC1 DC2 DR DS];

%Gas gap and thermal bond thicknesses
tGap=str2double(get(GapCheck, 'String')); %Gas gap thickness
tBond=str2double(get(BondCheck, 'String')); %Thermal bond thickness

Ainf_1=(0.25*pi*D(2)^2); %Area of coolant channel (before capsule)
Ainf_2=(0.25*pi*D(2)^2)-(0.25*pi*D(3)^2); %Area of coolant annulus (where capsule exists)

PlotGeo

%Conductivities of the components [W/m-K]
kB=str2double(get(text_kB, 'String')); %Basket conductivity
kC1=str2double(get(text_kC1, 'String')); %Capsule 1 conductivity
kGap=str2double(get(A_kGap, 'String')); %Gas gap conductivity
kC2=str2double(get(text_kC2, 'String')); %Capsule 2 conductivity
kBond=str2double(get(A_kBond, 'String')); %Thermal bond conductivity
kR=str2double(get(text_kR, 'String')); %Rodlet clad conductivity
kS=str2double(get(text_kS, 'String')); %Sample conductivity
k=[kB kC1 kGap kC2 kBond kR kS];

Ts_limit=str2double(get(text_Ts_limit, 'String'))+273.15; %Sample temp limit
Tc2_limit=str2double(get(text_Tc2_limit, 'String'))+273.15; %capsule 2 temp limit
Tc1_limit=str2double(get(text_Tc1_limit, 'String'))+273.15; %capsule 1 temp limit

%Thermal resistances due to conduction
if tGap<=0; RGap=0; tGap=0;
else
    RGap=log((D(4)+(2*tGap))/D(4))/(2*pi); %through gas gap
end
if tBond<=0; RBond=0; tBond=0;
else
    RBond=log((D(5)+(2*tBond))/D(5))/(2*pi); %through thermal bond
end
Rs=1/(4*pi); %through the sample
Rr=log(D(5)/D(end))/(2*pi); %through the rodlet clad

```

```

Rc2=log(D(4)/(D(5)+(2*tBond)))/(2*pi); %through capsule 2
Rc1=log(D(3)/(D(4)+(2*tGap)))/(2*pi); %through capsule 1

%           Rr=log(D(5)/(D(end)+(2*0.0001)))/(2*pi*L(end)); %through the rodlet clad
%           Rextra=log((D(end)+(2*0.0001))/D(end))/(2*pi*L(end)); %through a spacer

CenterZ=find(abs(z-LocS_Cent)<dz); %The location of the axial centerline

%Temperature of the water coolant in the annulus, based on in and out temps
Tinf_in=str2double(get(text_Tinf_in,'String'))+273.15; %Inlet water temp (from the top)
Tinf_out=70+273.15; %Outlet water temp (at the bottom)
%           Tinf=linspace(Tinf_in,Tinf_out,dx); %Linear distribution of the axial water temp
Tinf=ones(dx,1).*273.15; Tinf(1)=Tinf_in;

Pinf=str2double(get(text_Pinf,'String')); %Pressure of the water [MPa]
DP=str2double(get(text_DP,'String'))*1E6; %Pressure Drop [Pa]
Kc=0.5; Ke=1; Re_Kf=4E6;
f=(-4.*log((0.27.*0.26E-3./D(2))+(7./Re_Kf).^0.9)).^-2;
Kf=4*f*L(1)/D(2);
Vin=sqrt(2*DP/(PROP(Pinf,Tinf_in,'rho')*(Kc+Ke+Kf))); %Inlet velocity of the water [m/s]

%           P=16.5E3; c=0.058/0.0254; x0=-0.6*0.0254; %From IN-1260, Table VIII (pg 137 in THAT)
c=1; x0=0; %Custom constants for a cosine-shaped heat profile of the sample

%Initializing temperatures of the components [K]
Ts=ones(length(Tinf),1).*273.15; %Sample temp
Tr=ones(length(Tinf),1).*273.15; %Rodlet clad temp
Tc2=ones(length(Tinf),1).*273.15; %Capsule 2 temp
Tc1=ones(length(Tinf),1).*273.15; %Capsule 1 temp
Tinf_max=Tinf_out; %Initial Guess
while abs(max(Tinf)-Tinf_max)>0.1
    Tinf_max=max(Tinf);
    M=PROP(Pinf,Tinf_max,'rho')*Vin*Ainf_2;
    for i=2:max(CenterZ)

        %logical check
        Check1=(z(i)>=LocC_Top && z(i)<LocS_Top); %checks if we reached the capsule
        Check2=(z(i)>=LocS_Top); %checks if we reached the sample
        Check=num2str([Check1 Check2]);
        switch Check
            case '1 0'
                SIGNAL=1; %Signal for usage in a switch statement
                vinf=M/(PROP(Pinf,Tinf(i-1),'rho')*Ainf_2);
                Dhyd=D(2)-D(3);
                Deq=D(2)-((D(3)*L(2))/L(1)); %Equivalent diameter of annulus
            case '0 1'
                SIGNAL=2; %Signal for usage in a switch statement
                vinf=M/(PROP(Pinf,Tinf(i-1),'rho')*Ainf_2);
                Dhyd=D(2)-D(3);
                Deq=D(2)-((D(3)*L(2))/L(1)); %Equivalent diameter of annulus
            otherwise
                SIGNAL=0;
                vinf=M/(PROP(Pinf,Tinf(i-1),'rho')*Ainf_1);
                [Dhyd,Deq]=deal(D(2));
        end

        Re=PROP(Pinf,Tinf(i-1),'rho')*vinf*Dhyd/PROP(Pinf,Tinf(i-1),'mu'); %Reynolds #
        switch NuCor_Check.Value
            case 1; Nu=0.023*(Re^0.8)*(PROP(Pinf,Tinf(i-1),'Pr')^0.4); %Dittus-Boelter
            case 2; Nu=0.023*(Re^0.8)*(PROP(Pinf,Tinf(i-1),'Pr')^0.4)*(1+(0.912*(Re^-
0.1)*(PROP(Pinf,Tinf(i-1),'Pr')^0.4)*(1-(2.0043*exp(-Dhyd/D(3)))))); %Corrected Dittus-Boelter
            case 3; Nu=0.027*(Re^0.8)*(PROP(Pinf,Tinf(i-1),'Pr')^(1/3))*((PROP(Pinf,Tinf(i-
1),'mu')/PROP(Pinf,Tinf(i-1)+200,'mu'))^(0.14)); %Seider-Tate Turbulent appx (1936)
            case 4; f_Nu=(0.79*log(Re)-1.64)^-2; Nu=((f_Nu/8)*(Re-1000)*PROP(Pinf,Tinf(i-
1),'Pr'))/(1+(12.7*((f_Nu/8)^0.5)*((PROP(Pinf,Tinf(i-1),'Pr')^(2/3))-1))); %Gnielinski (1975)
            case 5; Nu=0.027*(Re^0.9)*(PROP(Pinf,Tinf(i-1),'Pr')^(0.7)-1)*((PROP(Pinf,Tinf(i-
1),'mu')/PROP(Pinf,Tinf(i-1)+200,'mu'))^(0.14))/abs(1+(20*((f/8)^0.3)*((PROP(Pinf,Tinf(i-
1),'Pr')^(1/4))))); %My custom correlation
        end
        hinf=Nu*PROP(Pinf,Tinf(i-1),'k')/Dhyd; %convection heat transfer coeff.
        Rinf=1/(hinf*pi*Deq); %Thermal resistance due to convection
    end
end

```

```

    if i==2
        Q=QFinder(Tinf_max,Tc1_limit,Tc2_limit,Ts_limit,Rinf,Rc1,RGap,Rc2,RBond,Rr,Rs);
    end
    Tinf(i)=Tinf(i-1)+(dz.*Q./(M.*PROP(Pinf,Tinf(i-1),'cp')) .* (sin(c.*(abs(z(i))-LocS_Cent-x0))+sin(c.*(LocS_Cent-x0))));

    switch SIGNAL
        case 1
            [Tc1(i),Tc2(i),~,~,~] = TempSolver(z(i),Q,Tinf(i),Tc1(i-1),Tc2(i-1),Tr(i-1),Ts(i-1),Rinf,Rc1,RGap,Rc2,RBond,Rr,Rs);
        case 2
            [Tc1(i),Tc2(i),Tr(i),Ts(i),~] = TempSolver(z(i),Q,Tinf(i),Tc1(i-1),Tc2(i-1),Tr(i-1),Ts(i-1),Rinf,Rc1,RGap,Rc2,RBond,Rr,Rs);
    end
end
end
for iii=max(CenterZ)+1:dx
    Tinf(iii)=Tinf(iii-1)+(dz.*Q./(M.*PROP(Pinf,Tinf(iii-1),'cp')) .* (sin(c.*(abs(z(iii))-LocS_Cent-x0))+sin(c.*(LocS_Cent-x0))));
end
figure();plot(Tinf-273.15,z,'b');xlabel('T_\infty [^oC]');ylabel('z [m]');
xlim([min(Tinf-273.15) max(Tinf-273.15)]);ylim([0 max(z)])
set(gca,'FontName','Cambria','FontSize',12,'YDir','reverse')
saveas(gcf,'CoolantTempDistribution.fig');saveas(gcf,'CoolantTempDistribution.jpg');close(gcf)
idx1=length(find(Tc1~=273.15)); idx2=length(find(Ts~=273.15));
% disp([max(Tc1) max(Tc2)])
axes(axT);cla; set(gca,'Visible','on')
hold on
plot(z(1:i),Tinf(1:i)-273.15,'-','Color',[68 114 196]./255)
plot(z(i-idx1:i),Tc1(i-idx1:i)-273.15,'-','Color',[201 201 201]./255)
plot(z(i-idx1:i),Tc2(i-idx1:i)-273.15,'-','Color',[165 165 165]./255)
plot(z(i-idx1:i),Tr(i-idx1:i)-273.15,'-','Color',[38 38 38]./255)
plot(z(i-idx2:i),Ts(i-idx2:i)-273.15,'-','Color',[1 0 0])
hold off
xlim([0 z(i)])
xlabel('z [m]'); ylabel('Temperature [^oC]')
legend('T_\infty','T_{c1}','T_{c2}','T_r','T_s','Location','eastoutside')
set(gca,'FontName','Cambria','FontSize',11);

set(Tc1_max_Label,'String',num2str(max(Tc1)-273.15));
set(Tc2_max_Label,'String',num2str(max(Tc2)-273.15));
set(q_Label,'String',[num2str(0.01*Q),' W/cm'],'FontName','Cambria','FontSize',FSize);
set(Tinf_max_Label,'String',[num2str(max(Tinf)-273.15),' ^oC'],'FontName','Cambria','FontSize',FSize);
OutputData
set(Stat_Label,'String','Go done');

end

```

6.3 Go2.m

```

function Go2(~,~,~)
global Tc1_max_Label Tc2_max_Label Tinf_max_Label q_Label Stat_Label...
    text_Tinf_in text_DP text_Pinf BondCheck GapCheck text_Ts_limit...
    text_DS text_DR text_DC2 text_DC1 text_DBi text_DBo text_LB Stat_Go2_Label

set(Stat_Label, 'String', 'Go2 Running');

Op1=[pwd, '\Heat_and_Pressure_Limits\'];
Op2=[pwd, '\Coolant_Max_Temps\'];
Op3=[pwd, '\SampleStats\'];
Op4=[pwd, '\tBondStats\'];

DBi=get(text_DBi, 'String'); %Basket ID (variable)
DC1=get(text_DC1, 'String'); %Capsule 1 OD (variable)
DC2=get(text_DC2, 'String'); %Capsule 2 OD (variable)
DS=get(text_DS, 'String'); %Sample OD (variable)
tBond=get(BondCheck, 'String'); %Thermal bond thickness (variable)
Ts=get(text_Ts_limit, 'String'); %Sample temperature limit (variable)
if DBi=='?'
    thik=0.0008; %Minimum thickness of basket [m]
    thikAn=0.0001; %Minimum thickness of the annulus [m]
    Sy=170; %Yield Strength of Basket [MPa]
    DBo=str2double(get(text_DBo, 'String'));
    DC1=str2double(DC1);
    Frac=100*round((DC1+(2*thikAn))/(DBo-(2*thik)),2);
    ct=0;
    for q=Frac:99
        set(Stat_Go2_Label, 'String', [num2str(100*ct/(99-Frac)), '% Done']);
        ct=ct+1;

        set(text_DBi, 'String', num2str(q*0.01*(DBo-(2*thik))));
        Go
        Dint(ct)=str2double(get(text_DBi, 'String'));
        QLim(ct)=cell2mat(textscan(get(q_Label, 'String'), '%f'));
        PLim(ct)=(Sy*0.5*(DBo-Dint(ct)))/((0.5*Dint(ct))+(0.6*0.5*(DBo-Dint(ct)))); %Pressure
limit of Basket [MPa]
        Tinf_max(ct)=cell2mat(textscan(get(Tinf_max_Label, 'String'), '%f'));
    end
    figure('Units', 'pixels', 'Position', [308 102 862 570])
    ax1=axes('Position', [0.1 0.1 0.8 0.8]); a=plot(ax1, Dint, QLim, 'k');
    xlabel(ax1, 'ID_{Basket} [m]'); ylabel(ax1, 'q' [W/cm]);
    ylim([min(QLim), max(QLim)]); xlim([min(Dint), max(Dint)])

set(ax1, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'w', 'XAxisLocation', 'bottom', 'YAxisLocation', 'left');

    ax2=axes('Position', ax1.Position); b=plot(ax2, Dint./0.0254, PLim, '-.k');
    xlabel(ax2, 'ID_{Basket} [in]'); ylabel(ax2, 'Pressure [MPa]');
    ylim([min(PLim), max(PLim)]); xlim([min(Dint./0.0254), max(Dint./0.0254)])

set(ax2, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'none', 'XAxisLocation', 'top', 'YAxisLocation', 'right')

    legend([a b], {'q' Limit', 'Pressure Limit'}, 'Location', 'south')
    set([ax1 ax2], 'FontName', 'Cambria', 'FontSize', 12);
    saveas(gcf, [Op1, 'Basket_Sens.fig']); saveas(gcf, [Op1, 'Basket_Sens.jpg']);

    figure('Units', 'pixels', 'Position', [308 102 862 570])
    ax1=axes('Position', [0.1 0.1 0.8 0.8]); plot(ax1, Dint, Tinf_max, 'k');
    xlabel(ax1, 'ID_{Basket} [m]'); ylabel(ax1, 'T_{\infty, max} [^oC]'); xlim([min(Dint), max(Dint)])

set(ax1, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'w', 'XAxisLocation', 'bottom', 'YAxisLocation', 'left');

    ax2=axes('Position', ax1.Position); plot(ax2, Dint./0.0254, Tinf_max, 'Color', 'none');
    xlabel(ax2, 'ID_{Basket} [in]'); xlim([min(Dint./0.0254), max(Dint./0.0254)])

set(ax2, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'none', 'XAxisLocation', 'top', 'YAxisLocation', 'right', 'YTick', [])

```

```

set([ax1 ax2], 'FontName', 'Cambria', 'FontSize', 12);
saveas(gcf, [Op2, 'Basket_Tinf.fig']); saveas(gcf, [Op2, 'Basket_Tinf.jpg']);
elseif DC1=='?'
thik=0.0008; %Minimum thickness of capsule 1 [m]
thikAn=0.0001; %Minimum thickness of annulus [m]
Sy=170; %Yield Strength of Capsule 1 [MPa]
DBi=str2double(get(text_DBi, 'String'));
tGap=str2double(get(GapCheck, 'String'));
DC2=str2double(get(text_DC2, 'String'));
Frac=100*round((DC2+(2*(tGap+thik)))/(DBi-(2*thikAn)), 2);
ct=0;
for q=Frac:99
set(Stat_Go2_Label, 'String', [num2str(100*ct/(99-Frac)), '% Done']);
ct=ct+1;

set(text_DC1, 'String', num2str(q*0.01*(DBi-(2*thikAn))));
% set(text_DC2, 'String', num2str(str2double(get(text_DC1, 'String'))-thik-
1E-5));
% set(text_DR, 'String', num2str(str2double(get(text_DC2, 'String'))-thik-
1E-5));
Go
Dint(ct)=str2double(get(text_DC1, 'String'));
QLim(ct)=cell2mat(textscan(get(q_Label, 'String'), '%f'));
PLim(ct)=(Sy*0.5*(Dint(ct)-(DC2+(2*tGap)))/((0.5*(DC2+(2*tGap)))+(0.6*0.5*(Dint(ct)-
(DC2+(2*tGap))))); %Pressure limit of Capsule 1 [MPa]
Tinf_max(ct)=cell2mat(textscan(get(Tinf_max_Label, 'String'), '%f'));
end
figure('Units', 'pixels', 'Position', [308 102 862 570])
ax1=axes('Position', [0.1 0.1 0.8 0.8]); a=plot(ax1, Dint, QLim, 'k');
xlabel(ax1, 'OD_{Capsule 1} [m]'); ylabel(ax1, 'q' [W/cm]);
ylim([min(QLim), max(QLim)]); xlim([min(Dint), max(Dint)])

set(ax1, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'w', 'XAxisLocation', 'bottom', 'YAxisLocation', 'left');

ax2=axes('Position', ax1.Position); b=plot(ax2, Dint./0.0254, PLim, '-.k');
xlabel(ax2, 'OD_{Capsule 1} [in]'); ylabel(ax2, 'Pressure [MPa]');
ylim([min(PLim), max(PLim)]); xlim([min(Dint./0.0254), max(Dint./0.0254)])

set(ax2, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'none', 'XAxisLocation', 'top', 'YAxisLocation', 'right')

legend([a b], {'q' Limit', 'Pressure Limit'}, 'Location', 'south')
set([ax1 ax2], 'FontName', 'Cambria', 'FontSize', 12);
saveas(gcf, [Op1, 'Cap1_Sens.fig']); saveas(gcf, [Op1, 'Cap1_Sens.jpg']);

figure('Units', 'pixels', 'Position', [308 102 862 570])
ax1=axes('Position', [0.1 0.1 0.8 0.8]); plot(ax1, Dint, Tinf_max, 'k');
xlabel(ax1, 'OD_{Capsule 1} [m]'); ylabel(ax1, 'T_{\infty, max}
[^\circ C]'); xlim([min(Dint), max(Dint)])

set(ax1, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'w', 'XAxisLocation', 'bottom', 'YAxisLocation', 'left');

ax2=axes('Position', ax1.Position); plot(ax2, Dint./0.0254, Tinf_max, 'Color', 'none');
xlabel(ax2, 'OD_{Capsule 1} [in]'); xlim([min(Dint./0.0254), max(Dint./0.0254)])

set(ax2, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'none', 'XAxisLocation', 'top', 'YAxisLocation', 'right', 'YTick', [])

set([ax1 ax2], 'FontName', 'Cambria', 'FontSize', 12);
saveas(gcf, [Op2, 'Cap1_Tinf.fig']); saveas(gcf, [Op2, 'Cap1_Tinf.jpg']);
elseif DC2=='?'
thik=0.0008; %Minimum thickness of capsule 1 [m]
Sy=170; %Yield Strength of Capsule 2 [MPa]
DC1=str2double(get(text_DC1, 'String'));
tGap=str2double(get(GapCheck, 'String'));
tBond=str2double(get(BondCheck, 'String'));
DR=str2double(get(text_DR, 'String'));
Frac=100*round((DR+(2*tBond))/(DC1-(2*(tGap+thik))), 2);

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```

ct=0;
for q=Frac:99
set(Stat_Go2_Label, 'String', [num2str(100*ct/(99-Frac)), '% Done']);
ct=ct+1;

set(text_DC2, 'String', num2str(q*0.01*(DC1-(2*(tGap+thik))));
%
set(text_DC1, 'String',
num2str(str2double(get(text_DC2, 'String'))+thik+1E-5));
%
set(text_DR, 'String', num2str(str2double(get(text_DC2, 'String'))-thik-
1E-5));
Go
Dint(ct)=str2double(get(text_DC2, 'String'));
QLim(ct)=cell2mat(textscan(get(q_Label, 'String'), '%f'));
PLim(ct)=(Sy*0.5*(Dint(ct)-(DR+(2*tBond)))/((0.5*(DR+(2*tBond)))+(0.6*0.5*(Dint(ct)-
(DR+(2*tBond))))); %Pressure limit of Capsule 2 [MPa]
Tinf_max(ct)=cell2mat(textscan(get(Tinf_max_Label, 'String'), '%f'));
end
figure('Units', 'pixels', 'Position', [308 102 862 570])
ax1=axes('Position', [0.1 0.1 0.8 0.8]); a=plot(ax1, Dint, QLim, 'k');
xlabel(ax1, 'OD_{Capsule 2} [m]'); ylabel(ax1, 'q' [W/cm]);
ylim([min(QLim), max(QLim)]); xlim([min(Dint), max(Dint)])

set(ax1, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'w', 'XAxisLocation', 'bottom', 'YAxisLocation', 'left');

ax2=axes('Position', ax1.Position); b=plot(ax2, Dint./0.0254, PLim, '-.k');
xlabel(ax2, 'OD_{Capsule 2} [in]'); ylabel(ax2, 'Pressure [MPa]');
ylim([min(PLim), max(PLim)]); xlim([min(Dint./0.0254), max(Dint./0.0254)])

set(ax2, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'none', 'XAxisLocation', 'top', 'YAxisLocation', 'right');

legend([a b], {'q' Limit', 'Pressure Limit'}, 'Location', 'south')
set([ax1 ax2], 'FontName', 'Cambria', 'FontSize', 12);
saveas(gcf, [Op1, 'Cap2_Sens.fig']); saveas(gcf, [Op1, 'Cap2_Sens.jpg']);

figure('Units', 'pixels', 'Position', [308 102 862 570])
ax1=axes('Position', [0.1 0.1 0.8 0.8]); plot(ax1, Dint, Tinf_max, 'k');
xlabel(ax1, 'OD_{Capsule 2} [m]'); ylabel(ax1, 'T_{\infty, max}
[^\circ C]'); xlim([min(Dint), max(Dint)])

set(ax1, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'w', 'XAxisLocation', 'bottom', 'YAxisLocation', 'left');

ax2=axes('Position', ax1.Position); plot(ax2, Dint./0.0254, Tinf_max, 'Color', 'none');
xlabel(ax2, 'OD_{Capsule 2} [in]'); xlim([min(Dint./0.0254), max(Dint./0.0254)])

set(ax2, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'none', 'XAxisLocation', 'top', 'YAxisLocation', 'right', 'YTick', []);

set([ax1 ax2], 'FontName', 'Cambria', 'FontSize', 12);
saveas(gcf, [Op2, 'Cap2_Tinf.fig']); saveas(gcf, [Op2, 'Cap2_Tinf.jpg']);
elseif DS=='?'
DBi=str2double(get(text_DBi, 'String'));
tGap=str2double(get(GapCheck, 'String'));
tBond=str2double(get(BondCheck, 'String'));
thikAn=0.0001; %Minimum thickness of annulus [m]
thik=0.0008; %Minimum thickness of capsules and rodlet [m]
Sy_R=400; %Yield Strength of Rodlet [MPa]
Sy_C=170; %Yield Strength of Capsules [MPa]
MaxDs=DBi-(thikAn*2)-(thik*6)-(tGap*2)-(tBond*2); %Maximum sample diameter
Frac=100*round(MaxDs/DBi, 2);
ct=0;
for q=1:Frac
set(Stat_Go2_Label, 'String', [num2str(100*ct/(Frac-1)), '% Done']);
ct=ct+1;

Dint(ct)=DBi*q*0.01;
set(text_DS, 'String', num2str(Dint(ct)));
set(text_DR, 'String', num2str(Dint(ct)+(thik*2)));
set(text_DC2, 'String', num2str(Dint(ct)+(thik*4)+(tBond*2)));

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set(text_DC1, 'String', num2str(Dint(ct)+(thik*6)+(tBond*2)+(tGap*2)));

Go

QLim(ct)=cell2mat(textscan(get(q_Label,'String'),'%f'));
Tinf_max(ct)=cell2mat(textscan(get(Tinf_max_Label,'String'),'%f'));
PLim_R(ct)=(Sy_R*thik)/(((0.5*str2double(get(text_DR,'String')))-thik)+(0.6*thik));
PLim_C2(ct)=(Sy_C*thik)/(((0.5*str2double(get(text_DC2,'String')))-thik)+(0.6*thik));
PLim_C1(ct)=(Sy_C*thik)/(((0.5*str2double(get(text_DC1,'String')))-thik)+(0.6*thik));
end
figure('Units','pixels','Position',[308 102 862 570])
ax1=axes('Position',[0.1 0.1 0.8 0.8]); a=plot(ax1,Dint,QLim,'k');
xlabel(ax1,'OD_{Sample} [m]'); ylabel(ax1,'q' [W/cm]);
ylim([min(QLim),max(QLim)]);xlim([min(Dint),max(Dint)])

set(ax1,'YColor','k','XColor','k','Box','off','Color','w','XAxisLocation','bottom','YAxisLocation','left');

ax2=axes('Position',ax1.Position);b=plot(ax2,Dint./0.0254,Tinf_max,'-.k');
xlabel(ax2,'OD_{Sample} [in]'); ylabel(ax2,'T_{\infty}');
ylim([min(Tinf_max),max(Tinf_max)]);xlim([min(Dint./0.0254),max(Dint./0.0254)])

set(ax2,'YColor','k','XColor','k','Box','off','Color','none','XAxisLocation','top','YAxisLocation','right')

legend([a b],{'q' Limit','T_{\infty, max}'},'Location','best')
set([ax1 ax2],'FontName','Cambria','FontSize',12);
saveas(gcf,[Op3,'Sample_Sens.fig']); saveas(gcf,[Op3,'Sample_Sens.jpg']);

figure('Units','pixels','Position',[308 102 862 570])
plot(Dint,PLim_R,'k',Dint,PLim_C2,'--k',Dint,PLim_C1,'-.k')
xlabel('OD_{Sample} [m]'); ylabel('Pressure Limit [MPa]');
xlim([min(Dint),max(Dint)]);legend('Rodlet','Capsule 2','Capsule 1')
set(gca,'FontName','Cambria','FontSize',12);
saveas(gcf,[Op3,'Sample_PlimsComps.fig']); saveas(gcf,[Op3,'Sample_PlimsComps.jpg']);
elseif tBond=='?'

DBi=str2double(get(text_DBi,'String'));
tGap=str2double(get(GapCheck,'String'));
DR=str2double(get(text_DR,'String'));
Sy_C=170; %Yield Strength of Capsules [MPa]
thikAn=0.0002; %Minimum thickness of annulus [m]
thik=0.0008; %Minimum thickness of capsules and rodlet [m]
Min_tBond=1E-5; %Minimum bond thickness [m]
Max_tBond=(DBi-(2*tGap)-(4*thik)-(2*thikAn)-DR)/2; %Max bond thickness
FracH=round(Max_tBond/DBi,2)/(100*Min_tBond);
FracL=round(Min_tBond/DBi,2)/(100*Min_tBond);

if Ts=='?'
Ts=500:100:2000;
for qq=1:length(Ts)
set(text_Ts_limit,'String',num2str(Ts(qq)));
ct=0;
for q=FracL:FracH
set(Stat_Go2_Label,'String',[num2str(qq),'/',num2str(length(Ts)),' ',num2str(100*ct/((FracH-FracL))),'% Done']);
ct=ct+1;

set(BondCheck,'String',num2str(DBi*q*Min_tBond*100));
tInt(ct,qq)=str2double(get(BondCheck,'String'));
set(text_DC1,'String',num2str(DR+(2*tInt(ct))+(2*tGap)+(4*thik)));
set(text_DC2,'String',num2str(DR+(2*tInt(ct))+(2*thik)));

Go

Tc1_max(ct,qq)=str2double(get(Tc1_max_Label,'String'));
Tc2_max(ct,qq)=str2double(get(Tc2_max_Label,'String'));
QLim(ct,qq)=cell2mat(textscan(get(q_Label,'String'),'%f'));
Tinf_max(ct,qq)=cell2mat(textscan(get(Tinf_max_Label,'String'),'%f'));
%
PLim_C2(ct)=(Sy_C*thik)/(((0.5*str2double(get(text_DC2,'String')))-thik)+(0.6*thik));

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%
PLim_C1(ct)=(Sy_C*thik)/(((0.5*str2double(get(text_DC1,'String')))-thik)+(0.6*thik));
end
figure('Units','pixels','Position',[308 102 862 570])
ax1=axes('Position',[0.1 0.1 0.8 0.8]); a=plot(ax1,tInt(:,qq),QLim(:,qq),'k');
xlabel(ax1,'t_{Bond} [m]'); ylabel(ax1,'q' [W/cm]');
ylim([min(QLim(:,qq)),max(QLim(:,qq))]); xlim([min(tInt(:,qq)),max(tInt(:,qq))])

set(ax1,'YColor','k','XColor','k','Box','off','Color','w','XAxisLocation','bottom','YAxisLocation','left');

ax2=axes('Position',ax1.Position); b=plot(ax2,tInt(:,qq)./0.0254,Tinf_max(:,qq),'-
.k');
xlabel(ax2,'t_{Bond} [in]'); ylabel(ax2,'T_{\infty}');

ylim([min(Tinf_max(:,qq)),max(Tinf_max(:,qq))]); xlim([min(tInt(:,qq)./0.0254),max(tInt(:,qq)./0.0
254)])

set(ax2,'YColor','k','XColor','k','Box','off','Color','none','XAxisLocation','top','YAxisLocation','right')

legend([a b],{'q' Limit','T_{\infty, max}'},'Location','best')
set([ax1 ax2],'FontName','Cambria','FontSize',12);
mkdir(Op4,[num2str(Ts(qq)),'_Ts\']);
OpC=[Op4,num2str(Ts(qq)),'_Ts\'];
saveas(gcf,[OpC,'tBond_Sens.fig']);
saveas(gcf,[OpC,'tBond_Sens.jpg']);
end
figure('Units','pixels','Position',[323 159 754 501]); hold on
for qq=1:length(Ts)
plot3(Tinf_max(:,qq),QLim(:,qq),tInt(:,qq),'DisplayName',['T_{s, limit} =
',num2str(Ts(qq)),' ^{\circ}C']);
if qq==1; legend('-DynamicLegend','Location','eastoutside'); end
end
hold off; grid on; view(-35,25); legend('boxoff')
xlabel('t_{Bond} [m]'); xlabel('T_{\infty, max} [^{\circ}C]'); ylabel('q'_{limit} [W/cm]');
set(gca,'FontName','Cambria','FontSize',11);
saveas(gcf,[Op4,'TsVary_Line.fig']); saveas(gcf,[Op4,'TsVary_Line.jpg']);

LB=str2double(get(text_LB,'String')); %Basket height [m]
DBi=DBi/0.3048; %Basket ID [ft]
DR=DR/0.3048; %Rodlet OD [ft]
tGap=tGap/0.3048; %Gap thickness [ft]
thik=thik/0.3048; %Min capsules thickness [ft]
DC1=DR+(2.*tGap)+(4.*thik)+(2.*tInt./0.3048); %All capl diameters (heated diameter) [ft]
Dhyd=DBi-DC1; %Hydraulic diameters (correspond to each tBond) [ft]
P=str2double(get(text_Pinf,'String')); %Coolant pressure [MPa]
DP=str2double(get(text_DP,'String')); %Total pressure drop [MPa]
Kc=0.5; Ke=1; Re_Kf=4E6;
f=(-4.*log((0.27.*0.26E-3./DBi)+(7./Re_Kf).^0.9)).^-2;
Kf=4*f*LB/(DBi*0.3048);
S=size(Tinf_max);
for i=1:S(1)
for q=1:S(2)
V(i,q)=sqrt(2.*DP/(PROP(P,Tinf_max(i,q),'rho').*(Kc+Ke+Kf)))/0.3048; %Inlet
velocity of the water [ft/s]
end
end

CHF=1.8.*((12915.*(Dhyd./(Dhyd+DC1)))+(127.*V./(Dhyd.^0.35)).*((60.*log(P*145.038))-
(80.8.*((P*145.038)/((P*145.038)-135)))-(0.25*V)-Tinf_max);
CHF=CHF.*11356.538527./3600; %Converting CHF from BTU/hr-ft2 to W/m2
DNBR=CHF./(100.*QLim./(pi.*DC1)); %Departure from nucleate boiling ratio
%
close all
Styles=[{'k-s'},{'k-^'},{'k-o'}]; COLS=['b','r','k','g','m','y'];

figure('Units','pixels','Position',[242 106 904 564]); hold on;
for i=1:length(Ts)
if i==13; Style=Styles(3); ct=1; elseif i==7; Style=Styles(2); ct=1; elseif
i==1; Style=Styles(1); ct=1; end

```



```

plot(tInt(:,i),DNBR(:,i),Style{:},'MarkerSize',5,'MarkerFaceColor',COLS(ct),'DisplayName',['T_{s,
limit} = ',num2str(Ts(i),' ^oC')]
    if i==1; legend('-DynamicLegend','Location','eastoutside');end
    ct=ct+1;
end
hold off; legend('boxoff')
xlim([min(min(tInt)) max(max(tInt))]);
xlabel('t_{Bond} [m]');ylabel('DNBR');
set(gca,'FontName','Cambria','FontSize',11)

axes('Units','normalized','Position',[0.522,0.676,0.216,0.24]); hold on
for i=3:6
    if i==13;Style=Styles(3);ct=1;elseif i==7;Style=Styles(2);ct=1;elseif
i==3;Style=Styles(1);ct=1;end
    plot(tInt(:,i),DNBR(:,i),Style{:},'MarkerSize',5,'MarkerFaceColor',COLS(ct))
    ct=ct+1;
end
hold off
xlim([2.5E-4 5E-4]);xlabel('t_{Bond} [m]');ylabel('DNBR');
set(gca,'FontName','Cambria','FontSize',10)

saveas(gcf,[pwd,'\DNBR_and_FIR\DNBR.fig']); saveas(gcf,[pwd,'\DNBR_and_FIR\DNBR.jpg'])

Tsat=223.95; %Water saturation temp [C] at 2.5 MPa from Cengel Thermo. Book (8th ed)
Tin=str2double(get(text_Tinf_in,'String')); %Water inlet temp [C]
FIR=(Tsat-Tin)./(Tinf_max-Tin); %Flow instability ratio

Styles=[{'k-s'},{'k-^'},{'k-o'}];COLS=['b','r','k','g','m','y'];

figure('Units','pixels','Position',[242 106 904 564]); hold on;
for i=1:length(Ts)
    if i==13;Style=Styles(3);ct=1;elseif i==7;Style=Styles(2);ct=1;elseif
i==1;Style=Styles(1);ct=1;end

plot(tInt(:,i),FIR(:,i),Style{:},'MarkerSize',5,'MarkerFaceColor',COLS(ct),'DisplayName',['T_{s,
limit} = ',num2str(Ts(i),' ^oC')]
    if i==1; legend('-DynamicLegend','Location','eastoutside');end
    ct=ct+1;
end
hold off; legend('boxoff')
xlim([min(min(tInt)) max(max(tInt))]);
xlabel('t_{Bond} [m]');ylabel('FIR');
set(gca,'FontName','Cambria','FontSize',11)

axes('Units','normalized','Position',[0.522,0.676,0.216,0.24]); hold on
for i=3:6
    if i==13;Style=Styles(3);ct=1;elseif i==7;Style=Styles(2);ct=1;elseif
i==3;Style=Styles(1);ct=1;end
    plot(tInt(:,i),FIR(:,i),Style{:},'MarkerSize',5,'MarkerFaceColor',COLS(ct))
    ct=ct+1;
end
hold off
xlim([2.5E-4 5E-4]);xlabel('t_{Bond} [m]');ylabel('FIR');
set(gca,'FontName','Cambria','FontSize',10)

saveas(gcf,[pwd,'\DNBR_and_FIR\FIR.fig']); saveas(gcf,[pwd,'\DNBR_and_FIR\FIR.jpg'])

headers={'tBond [m]' 'Ts_limit [C]' 'Tc1_max [C]' 'Tc2_max [C]' 'Tinf_max [C]' 'q''_limit
[W/cm]' 'DNBR' 'FIR'};
textHeader = strjoin(headers,','); %delimiter, comma in csv
%write header to file
fid = fopen('tBondSensitivity.csv','w');
fprintf(fid,'%s\n',textHeader);
fclose(fid);

dlmwrite('tBondSensitivity.csv',[reshape(tInt',[prod(S),1]), repmat(Ts',[S(1),1]), reshape(Tc1_max',
[prod(S),1]), reshape(Tc2_max',[prod(S),1]), reshape(Tinf_max',[prod(S),1]), reshape(QLim',[prod(S),
1]), reshape(DNBR',[prod(S),1]), reshape(FIR',[prod(S),1])], '-append');

```

```

else
    ct=0;
    for q=FracL:FracH
        set(Stat_Go2_Label, 'String', [num2str(100*ct/(FracH-FracL)), '% Done']);
        ct=ct+1;

        set(BondCheck, 'String', num2str(DBi*q*Min_tBond*100));
        tInt(ct)=str2double(get(BondCheck, 'String'));
        set(text_DC1, 'String', num2str(DR+(2*tInt(ct))+(2*tGap)+(4*thik)));
        set(text_DC2, 'String', num2str(DR+(2*tInt(ct))+(2*thik)));

        Go

        QLim(ct)=cell2mat(textscan(get(q_Label, 'String'), '%f'));
        Tinf_max(ct)=cell2mat(textscan(get(Tinf_max_Label, 'String'), '%f'));
        PLim_C2(ct)=(Sy_C*thik)/(((0.5*str2double(get(text_DC2, 'String')))-thik)+(0.6*thik));
        PLim_C1(ct)=(Sy_C*thik)/(((0.5*str2double(get(text_DC1, 'String')))-thik)+(0.6*thik));
    end
    figure('Units', 'pixels', 'Position', [308 102 862 570])
    ax1=axes('Position', [0.1 0.1 0.8 0.8]); a=plot(ax1, tInt, QLim, 'k');
    xlabel(ax1, 't_{Bond} [m]'); ylabel(ax1, 'q' [W/cm]);
    ylim([min(QLim), max(QLim)]); xlim([min(tInt), max(tInt)])

set(ax1, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'w', 'XAxisLocation', 'bottom', 'YAxisLocation', 'left');

    ax2=axes('Position', ax1.Position); b=plot(ax2, tInt./0.0254, Tinf_max, '-.k');
    xlabel(ax2, 't_{Bond} [in]'); ylabel(ax2, 'T_{\infty}');
    ylim([min(Tinf_max), max(Tinf_max)]); xlim([min(tInt./0.0254), max(tInt./0.0254)])

set(ax2, 'YColor', 'k', 'XColor', 'k', 'Box', 'off', 'Color', 'none', 'XAxisLocation', 'top', 'YAxisLocation', 'right')

    legend([a b], {'q' Limit', 'T_{\infty} max'}), 'Location', 'best')
    set([ax1 ax2], 'FontName', 'Cambria', 'FontSize', 12);
    saveas(gcf, [Op4, 'tBond_Sens.fig']); saveas(gcf, [Op4, 'tBond_Sens.jpg']);

    figure('Units', 'pixels', 'Position', [308 102 862 570])
    plot(tInt, PLim_C2, '--k', tInt, PLim_C1, '-.k')
    xlabel('t_{Bond} [m]'); ylabel('Pressure Limit [MPa]');
    xlim([min(tInt), max(tInt)]); legend('Capsule 2', 'Capsule 1')
    set(gca, 'FontName', 'Cambria', 'FontSize', 12);
    saveas(gcf, [Op4, 'tBond_PlimsComps.fig']); saveas(gcf, [Op4, 'tBond_PlimsComps.jpg']);
end
else
    errorldg(['Must set one of the following to ? (question mark sign)', newline, ...
        ' - Basket ID', newline, ' - Capsule 1 OD', newline, ' - Capsule 2 OD', ...
        newline, ' - Sample OD', newline, ' - tBond', newline, ' - tBond and Ts limit'])
end

set(Stat_Label, 'String', 'Go2 Done');
end

```

6.4 Go3.m

```

function Go3(~,~,~)
%Tab1 Elements
global Tc1_max_Label Tc2_max_Label Tinf_max_Label q_Label NuCor_Check...
    Stat_Label Q_PRIME text_Tinf_in text_DP text_Pinf DISCs BondCheck...
    GapCheck text_kS text_kR text_kC2 text_kC1 text_kB text_DS text_DR...
    text_DC2 text_DC1 text_DBi text_DBo text_LS text_LC text_LB axT_FSize...
    x0 c LocS_Cent kC1 kGap kC2 kBond kR kS
%Tab2 Elements
global A_kBond A_kGap

set(Stat_Label, 'String', ' Go(q) running');

%Lengths of components [m]
LB=str2double(get(text_LB,'String')); %Basket length (Active fuel height [Dwg: 606951])
LC=str2double(get(text_LC,'String')); %Capsule 1 length = Capsule 2 length = Rodlet clad length
LS=str2double(get(text_LS,'String')); %Sample length
L=[LB LC LS];

LocS_Cent=0.5*L(1); %Sample axial centerline location
LocS_Top=LocS_Cent-(L(end)/2); %Sample top location
LocC_Top=LocS_Cent-(L(2)/2); %Capsule1/Capsule2/Rodlet top location

dx=str2double(DISCs.String{DISCs.Value}); %Axial discretizations (number of points the geometry
is seperated into, axially)
z=linspace(0,L(1),dx); %Top (z=0) to bottom (z=Length of basket)
dz=abs(z(2)-z(1)); %Spacing between each axial point

DBo=str2double(get(text_DBo,'String')); %Basket OD (constant)
DBi=str2double(get(text_DBi,'String')); %Basket ID
DC1=str2double(get(text_DC1,'String')); %Capsule 1 OD (variable)
DC2=str2double(get(text_DC2,'String')); %Capsule 1 ID = Capsule 2 OD
DR=str2double(get(text_DR,'String')); %Capsule 2 ID = Rodlet clad OD
DS=str2double(get(text_DS,'String')); %Sample OD = Rodlet clad ID
D=[DBo DBi DC1 DC2 DR DS];

%Gas gap and thermal bond thicknesses
tGap=str2double(get(GapCheck,'String')); %Gas gap thickness
tBond=str2double(get(BondCheck,'String')); %Thermal bond thickness

Ainf_1=(0.25*pi*D(2)^2); %Area of coolant channel (before capsule)
Ainf_2=(0.25*pi*D(2)^2)-(0.25*pi*D(3)^2); %Area of coolant annulus (where capsule exists)

PlotGeo

%Conductivities of the components [W/m-K]
kB=str2double(get(text_kB,'String')); %Basket conductivity
kC1=str2double(get(text_kC1,'String')); %Capsule 1 conductivity
kGap=str2double(get(A_kGap,'String')); %Gas gap conductivity
kC2=str2double(get(text_kC2,'String')); %Capsule 2 conductivity
kBond=str2double(get(A_kBond,'String')); %Thermal bond conductivity
kR=str2double(get(text_kR,'String')); %Rodlet clad conductivity
kS=str2double(get(text_kS,'String')); %Sample conductivity
% k=[kB kC1 kGap kC2 kBond kR kS];

Q=str2double(get(Q_PRIME,'String'))*100; %[W/m]
%     Ts_limit=str2double(get(text_Ts_limit,'String'))+273.15-100; %Sample temp limit
%     Tc2_limit=str2double(get(text_Tc2_limit,'String'))+273.15-100; %capsule 2 temp limit
%     Tc1_limit=str2double(get(text_Tc1_limit,'String'))+273.15-100; %capsule 1 temp limit

%Thermal resistances due to conduction
if tGap<=0; RGap=0; tGap=0;
else
    RGap=log((D(4)+(2*tGap))/D(4))/(2*pi); %through gas gap
end
if tBond<=0; RBond=0; tBond=0;
else
    RBond=log((D(5)+(2*tBond))/D(5))/(2*pi); %through thermal bond

```

```

end
Rs=1/(4*pi); %through the sample
Rr=log(D(5)/D(end))/(2*pi); %through the rodlet clad
Rc2=log(D(4)/(D(5)+(2*tBond)))/(2*pi); %through capsule 2
Rc1=log(D(3)/(D(4)+(2*tGap)))/(2*pi); %through capsule 1

%           Rr=log(D(5)/(D(end)+(2*0.0001)))/(2*pi*L(end)); %through the rodlet clad
%           Rxtra=log((D(end)+(2*0.0001))/D(end))/(2*pi*L(end)); %through a spacer

CenterZ=find(abs(z-LocS_Cent)<dz); %The location of the axial centerline

%Temperature of the water coolant in the annulus, based on in and out temps
Tinf_in=str2double(get(text_Tinf_in,'String'))+273.15; %Inlet water temp (from the top)
Tinf_out=70+273.15; %Outlet water temp (at the bottom)
%           Tinf=linspace(Tinf_in,Tinf_out,dx); %Linear distribution of the axial water temp
Tinf=ones(dx,1).*273.15; Tinf(1)=Tinf_in;

Pinf=str2double(get(text_Pinf,'String')); %Pressure of the water [MPa]
DP=str2double(get(text_DP,'String'))*1E6; %Pressure Drop [Pa]
Kc=0.5; Ke=1; Re_Kf=4E6;
f=(-4.*log((0.27.*0.26E-3./D(2))+(7./Re_Kf).^0.9)).^-2;
Kf=4*f*L(1)/D(2);
Vin=sqrt(2*DP/(PROP(Pinf,Tinf_in,'rho')*(Kc+Ke+Kf))); %Inlet velocity of the water [m/s]

P=Q*dz;
c=1; x0=0; %Custom cosine fit for sample power

%Initializing temperatures of the components [K]
Ts=ones(length(Tinf),1).*273.15; %Sample temp
Tr=ones(length(Tinf),1).*273.15; %Rodlet clad temp
Tc2=ones(length(Tinf),1).*273.15; %Capsule 2 temp
Tc1=ones(length(Tinf),1).*273.15; %Capsule 1 temp
Tinf_max=Tinf_out; %Initial Guess
while abs(max(Tinf)-Tinf_max)>0.1
    Tinf_max=max(Tinf);
    M=PROP(Pinf,Tinf_max,'rho')*Vin*Ainf_2;
    for i=2:max(CenterZ)

        %logical check
        Check1=(z(i)>=LocC_Top && z(i)<LocS_Top); %checks if we reached the capsule
        Check2=(z(i)>=LocS_Top); %checks if we reached the sample
        Check=num2str([Check1 Check2]);
        switch Check
            case '1 0'
                SIGNAL=1; %Signal for usage in a switch statement
                vinf=M/(PROP(Pinf,Tinf(i-1),'rho')*Ainf_2);
                Dhyd=D(2)-D(3);
                Deq=D(2)-((D(3)*L(2))/L(1)); %Equivalent diameter of annulus=
            case '0 1'
                SIGNAL=2; %Signal for usage in a switch statement
                vinf=M/(PROP(Pinf,Tinf(i-1),'rho')*Ainf_2);
                Dhyd=D(2)-D(3);
                Deq=D(2)-((D(3)*L(2))/L(1)); %Equivalent diameter of annulus=
            otherwise
                SIGNAL=0;
                vinf=M/(PROP(Pinf,Tinf(i-1),'rho')*Ainf_1);
                [Dhyd,Deq]=deal(D(2));
        end

        Re=PROP(Pinf,Tinf(i-1),'rho')*vinf*Dhyd/PROP(Pinf,Tinf(i-1),'mu'); %Reynolds #
        switch NuCor_Check.Value
            case 1; Nu=0.023*(Re^0.8)*(PROP(Pinf,Tinf(i-1),'Pr')^0.4); %Dittus-Boelter
            case 2; Nu=0.023*(Re^0.8)*(PROP(Pinf,Tinf(i-1),'Pr')^0.4)*(1+(0.912*(Re^-
0.1)*(PROP(Pinf,Tinf(i-1),'Pr')^0.4)*(1-(2.0043*exp(-Dhyd/D(3)))))); %Corrected Dittus-Boelter
            case 3; Nu=0.027*(Re^0.8)*(PROP(Pinf,Tinf(i-1),'Pr')^(1/3))*((PROP(Pinf,Tinf(i-
1),'mu')/PROP(Pinf,Tinf(i-1)+200,'mu'))^(0.14)); %Seider-Tate Turbulent appx (1936)
            case 4; f_Nu=(0.79*log(Re)-1.64)^-2; Nu=((f_Nu/8)*(Re-1000)*PROP(Pinf,Tinf(i-
1),'Pr'))/(1+(12.7*(f_Nu/8)^0.5)*((PROP(Pinf,Tinf(i-1),'Pr')^(2/3))-1)); %Gnielinski (1975)
            case 5; Nu=0.027*(Re^0.9)*(PROP(Pinf,Tinf(i-1),'Pr')^(1/3))-1*((PROP(Pinf,Tinf(i-
1),'mu')/PROP(Pinf,Tinf(i-1)+200,'mu'))^(0.14))/abs(1+(20*((f/8)^0.3)*((PROP(Pinf,Tinf(i-
1),'Pr')^(1/4))))); %My custom correlation

```

```

end
hinf=Nu*PROP(Pinf,Tinf(i-1),'k')/Dhyd; %convection heat transfer coeff.
Rinf=1/(hinf*pi*Deq); %Thermal resistance due to convection

Tinf(i)=Tinf(i-1)+(P./(M.*PROP(Pinf,Tinf(i-1),'cp')) .* (sin(c.*(abs(z(i))-LocS_Cent)-
x0))+sin(c.*(LocS_Cent-x0)));

switch SIGNAL
case 1
    [Tc1(i),Tc2(i),~,~,~] = TempSolver(z(i),Q,Tinf(i),Tc1(i-1),Tc2(i-1),Tr(i-1),Ts(i-
1),Rinf,Rc1,RGap,Rc2,RBond,Rr,Rs);
case 2
    [Tc1(i),Tc2(i),Tr(i),Ts(i),k] = TempSolver(z(i),Q,Tinf(i),Tc1(i-1),Tc2(i-1),Tr(i-
1),Ts(i-1),Rinf,Rc1,RGap,Rc2,RBond,Rr,Rs);
end
end
end
for iii=max(CenterZ)+1:dx
    Tinf(iii)=Tinf(iii-1)+(P./(M.*PROP(Pinf,Tinf(iii-1),'cp')) .* (sin(c.*(abs(z(iii))-LocS_Cent)-
x0))+sin(c.*(LocS_Cent-x0)));
end
% disp([Tc1(i) (Tc2(i)-(Q*cos(c*(abs(z(i))-LocS_Cent)-x0))*(Rc2/k(3)))) Tr(i) Ts(i)]-273.15)
% disp([Tc1(i) (Tc2(i)-(Q*cos(c*(abs(z(i))-LocS_Cent)-x0))*(Rc2/kC2)))) Tr(i) Ts(i)]-273.15 - [96
216 281 410]) ./[96 216 281 410])
% disp([Re Nu])
% disp([Tc1(i) (Tc2(i)-(Q*cos(c*(abs(z(i))-LocS_Cent)-x0))*(Rc2/kC2)))) Tr(i) Ts(i)]-273.15 - [106
275 374 546]) ./[106 275 374 546])
% disp([kC1 kC2 kR kS])
figure();plot(Tinf-273.15,z,'b');xlabel('T_\infty [^oC]');ylabel('z [m]');
xlim([min(Tinf-273.15) max(Tinf-273.15)]);ylim([0 max(z)])
set(gca,'FontName','Cambria','FontSize',12,'YDir','reverse')
saveas(gcf,'CoolantTempDistribution.fig');saveas(gcf,'CoolantTempDistribution.jpg');close(gcf)
idx1=length(find(Tc1~=273.15)); idx2=length(find(Ts~=273.15));
% disp([i idx1 idx2])
axes(axT);cla; set(gca,'Visible','on')
hold on
plot(z(1:i),Tinf(1:i)-273.15,'-','Color',[68 114 196]./255)
plot(z(i-idx1:i),Tc1(i-idx1:i)-273.15,'-','Color',[201 201 201]./255)
plot(z(i-idx1:i),Tc2(i-idx1:i)-273.15,'-','Color',[165 165 165]./255)
plot(z(i-idx2:i),Tr(i-idx2:i)-273.15,'-','Color',[38 38 38]./255)
plot(z(i-idx2:i),Ts(i-idx2:i)-273.15,'-','Color',[1 0 0])
hold off
xlim([0 z(i)])
xlabel('z [m]'); ylabel('Temperature [^oC]')
legend('T_\infty','T_{c1}','T_{c2}','T_r','T_s','Location','eastoutside')
set(gca,'FontName','Cambria','FontSize',11);

set(Tc1_max_Label,'String',num2str(max(Tc1)-273.15));
set(Tc2_max_Label,'String',num2str(max(Tc2)-273.15));
set(q_Label,'String',[num2str(0.01*Q),' W/cm'],'FontName','Cambria','FontSize',FSize);
set(Tinf_max_Label,'String',[num2str(max(Tinf)-273.15),'
^oC'],'FontName','Cambria','FontSize',FSize);
OutputData
set(Stat_Label,'String','Go done');

end

```

6.5 PlotGeo.m

```
function PlotGeo(~,~,~)
%Tabl Elements
global Stat_Label BondCheck GapCheck text_DS text_DR text_DC2 text_DC1...
text_DBi text_DBo axG FSize

axes(axG);cla
th=0:5:360;
DBo=str2double(get(text_DBo,'String')); %Basket OD (constant)
DBi=str2double(get(text_DBi,'String')); %Basket ID
DC1=str2double(get(text_DC1,'String')); %Capsule 1 OD (variable)
DC2=str2double(get(text_DC2,'String')); %Capsule 1 ID = Capsule 2 OD
DR=str2double(get(text_DR,'String')); %Capsule 2 ID = Rodlet clad OD
DS=str2double(get(text_DS,'String')); %Sample OD = Rodlet clad ID
tGap=str2double(get(GapCheck,'String')); %Gas gap thickness
tBond=str2double(get(BondCheck,'String')); %Thermal bond thickness
%
figure();
xBo=DBo*cosd(th)/2; xBi=DBi*cosd(th)/2; xC1o=DC1*cosd(th)/2; xGap=(DC2+(2*tGap))*cosd(th)/2;
xC1i=DC2*cosd(th)/2; xBond=(DR+(2*tBond))*cosd(th)/2; xC2i=DR*cosd(th)/2; xS=DS*cosd(th)/2;
yBo=DBo*sind(th)/2; yBi=DBi*sind(th)/2; yC1o=DC1*sind(th)/2; yGap=(DC2+(2*tGap))*sind(th)/2;
yC1i=DC2*sind(th)/2; yBond=(DR+(2*tBond))*sind(th)/2; yC2i=DR*sind(th)/2; yS=DS*sind(th)/2;
plot(xBo,yBo,'k',xBi,yBi,'k',xC1o,yC1o,'k',xC1i,yC1i,'k',xC2i,yC2i,'k',xS,yS,'k');
PL=fill(xBo,yBo,[127 127 127]./255,xBi,yBi,[68 114 196]./255,...
        xC1o,yC1o,[201 201 201]./255,xGap,yGap,[229 255 204]./255,...
        xC1i,yC1i,[165 165 165]./255,xBond,yBond,[1 1 0],...
        xC2i,yC2i,[38 38 38]./255,xS,yS,[1 0 0]);
legend(PL,{'Basket','Water Channel','Capsule 1','Gas Gap','Capsule 2','Thermal Bond','Rodlet
Clad','Sample'},'Location','eastoutside')
xlabel('meters');ylabel('meters'); legend('Boxoff')
%
set(gcf,'color','w'); %Make figure background white
%
set(gca,'XColor','none','YColor','none') %Remove axes
set(gca,'FontName','Cambria','FontSize',FSize); %Set font name and size
axis image
saveas(gcf,'OptimalGeometrySetup.fig')
set(Stat_Label,'String','Geometry Plotted');
end
```

6.6 OutputData.m

```
function OutputData(~,~,~)
%Tabl Elements
global axT q_Label

LINES=axT.Children;
for i=1:length(LINES)
    CLine=LINES(i);
    z{i}=CLine.XData'; T{i}=CLine.YData';
end
z=flipud(z{5});
for i=1:length(T)
    t=zeros(size(z));
    Tcur=flipud(T{i});
    for q=1:length(Tcur)
        t(q)=Tcur(q);
    end
    switch i
        case 1; Ts=t;
        case 2; Tr=t;
        case 3; Tc1=t;
        case 4; Tc2=t;
        otherwise; Tinf=t;
    end
end
qlim=zeros(size(z));qlim(1)=cell2mat(textscan(get(q_Label,'String'),'%f'));

headers={'z [m]' 'Tinf [°C]' 'Tc1 [°C]' 'Tc2 [°C]' 'Tr [°C]' 'Ts [°C]','q'_Limit [W/cm]'};
textHeader = strjoin(headers,',' ); %delimiter, comma in csv
%write header to file
fid = fopen('Data.csv','w');
fprintf(fid,'%s\n',textHeader);
fclose(fid);
dlmwrite('Data.csv',[z,Tinf,Tc2,Tc1,Tr,Ts,qlim],'-append')
end
```

6.7 TempSolver.m

```

function [Tc1_out,Tc2_out,Tr_out,Ts_out,k] =
TempSolver(z,Q,Tinf,Tc1_in,Tc2_in,Tr_in,Ts_in,Rinf,Rc1,RGap,Rc2,RBond,Rr,Rs)
global QCos_Check F_kBond E_kBond D_kBond C_kBond B_kBond A_kBond...
kBond_check F_kGap E_kGap D_kGap C_kGap B_kGap A_kGap kGap_check...
F_kS E_kS D_kS C_kS B_kS A_kS kS_check F_kR E_kR D_kR C_kR B_kR A_kR...
kR_check F_kC2 E_kC2 D_kC2 C_kC2 B_kC2 A_kC2 kC2_check F_kC1 E_kC1...
D_kC1 C_kC1 B_kC1 A_kC1 kC1_check x0 c LocS_Cent kC1 kGap kC2 kBond kR kS
ct=0;

Tgap=mean([Tc1_in Tc2_in]);
Tbond=mean([Tc2_in Tr_in]);

while ct<5
    if Tc1_in>273.15
        A=str2double(get(A_kC1,'String')); B=str2double(get(B_kC1,'String'));
        C=str2double(get(C_kC1,'String')); D=str2double(get(D_kC1,'String'));
        E=str2double(get(E_kC1,'String')); F=str2double(get(F_kC1,'String'));
        switch kC1_check.Value
            case 2; kC1=A+(B*Tc1_in)+(C*(Tc1_in^2))+(D*(Tc1_in^3))+(E*(Tc1_in^4))+(F*(Tc1_in^5));
            case 3; kC1=A*(B^(C*Tc1_in));
        end
        A=str2double(get(A_kGap,'String')); B=str2double(get(B_kGap,'String'));
        C=str2double(get(C_kGap,'String')); D=str2double(get(D_kGap,'String'));
        E=str2double(get(E_kGap,'String')); F=str2double(get(F_kGap,'String'));
        switch kGap_check.Value
            case 1; kGap=A;
            case 2; kGap=A+(B*Tgap)+(C*(Tgap^2))+(D*(Tgap^3))+(E*(Tgap^4))+(F*(Tgap^5));
            case 3; kGap=A*(B^(C*Tgap));
        end
    end
    if Tc2_in>273.15
        A=str2double(get(A_kC2,'String')); B=str2double(get(B_kC2,'String'));
        C=str2double(get(C_kC2,'String')); D=str2double(get(D_kC2,'String'));
        E=str2double(get(E_kC2,'String')); F=str2double(get(F_kC2,'String'));
        switch kC2_check.Value
            case 2; kC2=A+(B*Tc2_in)+(C*(Tc2_in^2))+(D*(Tc2_in^3))+(E*(Tc2_in^4))+(F*(Tc2_in^5));
            case 3; kC2=A*(B^(C*Tc2_in));
        end
        A=str2double(get(A_kBond,'String')); B=str2double(get(B_kBond,'String'));
        C=str2double(get(C_kBond,'String')); D=str2double(get(D_kBond,'String'));
        E=str2double(get(E_kBond,'String')); F=str2double(get(F_kBond,'String'));
        switch kBond_check.Value
            case 1; kBond=A;
            case 2; kBond=A+(B*Tbond)+(C*(Tbond^2))+(D*(Tbond^3))+(E*(Tbond^4))+(F*(Tbond^5));
            case 3; kBond=A*(B^(C*Tbond));
        end
    end
    if Tr_in>273.15
        A=str2double(get(A_kR,'String')); B=str2double(get(B_kR,'String'));
        C=str2double(get(C_kR,'String')); D=str2double(get(D_kR,'String'));
        E=str2double(get(E_kR,'String')); F=str2double(get(F_kR,'String'));
        switch kR_check.Value
            case 2; kR=A+(B*Tr_in)+(C*(Tr_in^2))+(D*(Tr_in^3))+(E*(Tr_in^4))+(F*(Tr_in^5));
            case 3; kR=A*(B^(C*Tr_in));
        end
    end
    if Ts_in>273.15
        A=str2double(get(A_kS,'String')); B=str2double(get(B_kS,'String'));
        C=str2double(get(C_kS,'String')); D=str2double(get(D_kS,'String'));
        E=str2double(get(E_kS,'String')); F=str2double(get(F_kS,'String'));
        switch kS_check.Value
            case 2; kS=A+(B*Ts_in)+(C*(Ts_in^2))+(D*(Ts_in^3))+(E*(Ts_in^4))+(F*(Ts_in^5));
            case 3; kS=A*(B^(C*Ts_in));
        end
    end
    k=[kC1,kGap,kC2,kBond,kR,kS];

    switch QCos_Check.Value

```



```

case 1 %ForQConstant
    Tc1_out=(Q*(Rinf+(Rc1/kC1)))+Tinf;
    Tc2_out=(Q*(Rinf+(Rc1/kC1)+(RGap/kGap)+(Rc2/kC2)))+Tinf;
    Tr_out=(Q*(Rinf+(Rc1/kC1)+(RGap/kGap)+(Rc2/kC2)+(RBond/kBond)+(Rr/kR)))+Tinf;
    Ts_out=(Q*(Rinf+(Rc1/kC1)+(RGap/kGap)+(Rc2/kC2)+(RBond/kBond)+(Rr/kR)+(Rs/kS)))+Tinf;
case 2 %ForQCosine
    Tc1_out=( (Q*cos(c*(abs(z-LocS_Cent)-x0)) )*(Rinf+(Rc1/kC1)))+Tinf;
    Tc2_out=( (Q*cos(c*(abs(z-LocS_Cent)-
x0)) )*(Rinf+(Rc1/kC1)+(RGap/kGap)+(Rc2/kC2)))+Tinf;
    Tr_out=( (Q*cos(c*(abs(z-LocS_Cent)-
x0)) )*(Rinf+(Rc1/kC1)+(RGap/kGap)+(Rc2/kC2)+(RBond/kBond)+(Rr/kR)))+Tinf;
    Ts_out=( (Q*cos(c*(abs(z-LocS_Cent)-
x0)) )*(Rinf+(Rc1/kC1)+(RGap/kGap)+(Rc2/kC2)+(RBond/kBond)+(Rr/kR)+(Rs/kS)))+Tinf;
end

Tgap=mean([Tc1_out Tc2_out]);
Tbond=mean([Tc2_out Tr_out]);

ct=ct+1;
end
end

```

6.8 QFinder.m

```

function Q = QFinder(Tinf_max,Tc1_limit,Tc2_limit,Ts_limit,Rinf,Rc1,RGap,Rc2,RBond,Rr,Rs)
global F_kBond E_kBond D_kBond C_kBond B_kBond A_kBond...
kBond_check F_kGap E_kGap D_kGap C_kGap B_kGap A_kGap kGap_check...
F_kS E_kS D_kS C_kS B_kS A_kS kS_check F_kR E_kR D_kR C_kR B_kR A_kR...
kR_check F_kC2 E_kC2 D_kC2 C_kC2 B_kC2 A_kC2 kC2_check F_kC1 E_kC1...
D_kC1 C_kC1 B_kC1 A_kC1 kC1_check kC1 kGap kC2 kBond kR kS

Tc1_in=Tc1_limit;
Tc2_in=Tc2_limit;
Tr_in=mean([Tc2_limit,Ts_limit]);
Ts_in=Ts_limit;

if Tc1_in>273.15
A=str2double(get(A_kC1,'String')); B=str2double(get(B_kC1,'String'));
C=str2double(get(C_kC1,'String')); D=str2double(get(D_kC1,'String'));
E=str2double(get(E_kC1,'String')); F=str2double(get(F_kC1,'String'));
switch kC1_check.Value
case 2; kC1=A+(B*Tc1_in)+(C*(Tc1_in^2))+(D*(Tc1_in^3))+(E*(Tc1_in^4))+(F*(Tc1_in^5));
case 3; kC1=A*(B^(C*Tc1_in));
end
A=str2double(get(A_kGap,'String')); B=str2double(get(B_kGap,'String'));
C=str2double(get(C_kGap,'String')); D=str2double(get(D_kGap,'String'));
E=str2double(get(E_kGap,'String')); F=str2double(get(F_kGap,'String'));
switch kGap_check.Value
case 1; kGap=A;
case 2; kGap=A+(B*Tc1_in)+(C*(Tc1_in^2))+(D*(Tc1_in^3))+(E*(Tc1_in^4))+(F*(Tc1_in^5));
case 3; kGap=A*(B^(C*Tc1_in));
end
end
if Tc2_in>273.15
A=str2double(get(A_kC2,'String')); B=str2double(get(B_kC2,'String'));
C=str2double(get(C_kC2,'String')); D=str2double(get(D_kC2,'String'));
E=str2double(get(E_kC2,'String')); F=str2double(get(F_kC2,'String'));
switch kC2_check.Value
case 2; kC2=A+(B*Tc2_in)+(C*(Tc2_in^2))+(D*(Tc2_in^3))+(E*(Tc2_in^4))+(F*(Tc2_in^5));
case 3; kC2=A*(B^(C*Tc2_in));
end
A=str2double(get(A_kBond,'String')); B=str2double(get(B_kBond,'String'));
C=str2double(get(C_kBond,'String')); D=str2double(get(D_kBond,'String'));
E=str2double(get(E_kBond,'String')); F=str2double(get(F_kBond,'String'));
switch kBond_check.Value
case 1; kBond=A;
case 2; kBond=A+(B*Tc2_in)+(C*(Tc2_in^2))+(D*(Tc2_in^3))+(E*(Tc2_in^4))+(F*(Tc2_in^5));
case 3; kBond=A*(B^(C*Tc2_in));
end
end
if Tr_in>273.15
A=str2double(get(A_kR,'String')); B=str2double(get(B_kR,'String'));
C=str2double(get(C_kR,'String')); D=str2double(get(D_kR,'String'));
E=str2double(get(E_kR,'String')); F=str2double(get(F_kR,'String'));
switch kR_check.Value
case 2; kR=A+(B*Tr_in)+(C*(Tr_in^2))+(D*(Tr_in^3))+(E*(Tr_in^4))+(F*(Tr_in^5));
case 3; kR=A*(B^(C*Tr_in));
end
end
if Ts_in>273.15
A=str2double(get(A_kS,'String')); B=str2double(get(B_kS,'String'));
C=str2double(get(C_kS,'String')); D=str2double(get(D_kS,'String'));
E=str2double(get(E_kS,'String')); F=str2double(get(F_kS,'String'));
switch kS_check.Value
case 2; kS=A+(B*Ts_in)+(C*(Ts_in^2))+(D*(Ts_in^3))+(E*(Ts_in^4))+(F*(Ts_in^5));
case 3; kS=A*(B^(C*Ts_in));
end
end

q(1)=(Tc1_limit-Tinf_max)/(Rinf+(Rc1/kC1)); %Heat generated by capsule 1
q(2)=(Tc2_limit-Tinf_max)/(Rinf+(Rc1/kC1)+(RGap/kGap)+(Rc2/kC2)); %Heat generated by capsule 2
q(3)=(Ts_limit-Tinf_max)/(Rinf+(Rc1/kC1)+(RGap/kGap)+(Rc2/kC2)+(RBond/kBond)+(Rr/kR)+(Rs/kS));
%Heat generated by sample

```

```
Q=min(q);  
end
```

6.9 PROP.m

```
function Outp=PROP(P,T,Property)
% PROP(P,T,'Property')
% P=Pressure [MPa]
% T=Temperature [K]
% Property = desired property, choose from the following:
% - 'rho'      Mass density [m3/kg]
% - 'mu'      Dynamic viscosity [Pa-s]
% - 'k'       Thermal conductivity [W/m-K]
% - 'cp'     Specific heat with constant pressure [J/kg-K]
% - 'cv'     Specific heat with constant volume [J/kg-K]
% - 'h'      Enthalpy [J/kg]
% - 's'      Entropy [J/kg]
% - 'Pr'     Prandtl Number
% NOTE: must use property file in 'Water_#MPa.txt' format, such that
% #=exact pressure float in MPa. The data for making such file can be
% copy-pasted from NIST:
% Eric W. Lemmon, Mark O. McLinden and Daniel G. Friend, "Thermophysical
% Properties of Fluid Systems" in NIST Chemistry WebBook, NIST Standard
% Reference Database Number 69, Eds. P.J. Linstrom and W.G. Mallard,
% National Institute of Standards and Technology, Gaithersburg MD,20899,
% https://doi.org/10.18434/T4D303, (retrieved June 29, 2020).

A=textscan(fopen(['Water_',num2str(P),'MPa.txt']),...
'%f %f %f %f %f %f %f %f %f %f %f %f %s','HeaderLines',1);fclose all;
switch Property
case 'rho' %Mass density [m3/kg]
    A=[A{1} A{3}]; [~,idx]=min(abs(A(:,1)-T));
    Outp=A(idx,2);
case 'mu' %Dynamic viscosity [Pa-s]
    A=[A{1} A{12}]; [~,idx]=min(abs(A(:,1)-T));
    Outp=A(idx,2);
case 'k' %Thermal conductivity [W/m-K]
    A=[A{1} A{13}]; [~,idx]=min(abs(A(:,1)-T));
    Outp=A(idx,2);
case 'cp' %Specific heat with constant pressure [J/kg-K]
    A=[A{1} A{9}]; [~,idx]=min(abs(A(:,1)-T));
    Outp=A(idx,2).*1E3;
case 'cv' %Specific heat with constant volume [J/kg-K]
    A=[A{1} A{8}]; [~,idx]=min(abs(A(:,1)-T));
    Outp=A(idx,2).*1E3;
case 'h' %Enthalpy [J/kg]
    A=[A{1} A{6}]; [~,idx]=min(abs(A(:,1)-T));
    Outp=A(idx,2).*1E3;
case 's' %Entropy [J/kg]
    A=[A{1} A{7}]; [~,idx]=min(abs(A(:,1)-T));
    Outp=A(idx,2).*1E3;
case 'Pr'
    A=[A{1} A{9} A{12} A{13}]; [~,idx]=min(abs(A(:,1)-T));
    Outp=A(idx,2)*1E3*A(idx,3)/A(idx,4);
otherwise
    error('ERROR! Property is not found! consult the PROP.m function')
end
end
```

6.10 Water_2.5MPa.txt [From Reference 19]

Temperature (K)	Pressure (MPa)	Density (kg/m ³)	Volume (m ³ /kg)	Internal Energy (kJ/kg)	Enthalpy (kJ/kg)	Entropy (J/g*K)	Cv						
(J/g*K)	Cp (J/g*K)	Sound Spd. (m/s)	Joule-Thomson (K/MPa)	Viscosity (Pa*s)	Therm. Cond. (W/m*K)	Phase							
274.00	2.5000	1001.1	0.00099890	3.5781	6.0754	0.013073	4.2041	4.2051	1410.5	-0.24039	0.0017342	0.56399	liquid
275.66	2.5000	1001.2	0.00099885	10.555	13.052	0.038459	4.2005	4.2006	1418.5	-0.23882	0.0016404	0.56711	liquid
277.32	2.5000	1001.2	0.00099884	17.525	20.022	0.063666	4.1966	4.1966	1426.3	-0.23731	0.0015545	0.57024	liquid
278.98	2.5000	1001.1	0.00099888	24.488	26.985	0.088701	4.1924	4.1932	1433.7	-0.23585	0.0014755	0.57337	liquid
280.64	2.5000	1001.0	0.00099896	31.446	33.943	0.11357	4.1880	4.1901	1440.9	-0.23442	0.0014028	0.57650	liquid
282.30	2.5000	1000.9	0.00099908	38.399	40.896	0.13827	4.1834	4.1874	1447.7	-0.23304	0.0013357	0.57962	liquid
283.96	2.5000	1000.8	0.00099923	45.347	47.846	0.16282	4.1785	4.1850	1454.3	-0.23170	0.0012736	0.58273	liquid
285.62	2.5000	1000.6	0.00099943	52.292	54.791	0.18720	4.1735	4.1830	1460.7	-0.23039	0.0012160	0.58582	liquid
287.28	2.5000	1000.4	0.00099965	59.234	61.733	0.21144	4.1682	4.1812	1466.8	-0.22911	0.0011624	0.58890	liquid
288.94	2.5000	1000.1	0.00099991	66.173	68.673	0.23553	4.1628	4.1796	1472.6	-0.22786	0.0011126	0.59195	liquid
290.60	2.5000	999.80	0.0010002	73.109	75.610	0.25947	4.1571	4.1783	1478.2	-0.22664	0.0010661	0.59498	liquid
292.26	2.5000	999.49	0.0010005	80.043	82.545	0.28326	4.1513	4.1772	1483.5	-0.22545	0.0010227	0.59797	liquid
293.92	2.5000	999.14	0.0010009	86.976	89.478	0.30692	4.1454	4.1762	1488.7	-0.22428	0.00098207	0.60093	liquid
295.58	2.5000	998.76	0.0010012	93.907	96.410	0.33044	4.1393	4.1754	1493.6	-0.22314	0.00094398	0.60385	liquid
297.24	2.5000	998.36	0.0010016	100.84	103.34	0.35382	4.1330	4.1747	1498.2	-0.22201	0.00090822	0.60672	liquid
298.90	2.5000	997.93	0.0010021	107.76	110.27	0.37707	4.1266	4.1742	1502.7	-0.22090	0.00087459	0.60956	liquid
300.56	2.5000	997.47	0.0010025	114.69	117.20	0.40018	4.1201	4.1738	1507.0	-0.21982	0.00084294	0.61234	liquid
302.22	2.5000	997.00	0.0010030	121.62	124.13	0.42317	4.1134	4.1735	1511.0	-0.21875	0.00081310	0.61507	liquid
303.88	2.5000	996.49	0.0010035	128.55	131.05	0.44603	4.1066	4.1733	1514.9	-0.21769	0.00078494	0.61776	liquid
305.54	2.5000	995.96	0.0010041	135.47	137.98	0.46876	4.0997	4.1732	1518.6	-0.21666	0.00075832	0.62039	liquid
307.20	2.5000	995.41	0.0010046	142.40	144.91	0.49138	4.0927	4.1731	1522.1	-0.21563	0.00073314	0.62296	liquid
308.86	2.5000	994.84	0.0010052	149.32	151.84	0.51387	4.0856	4.1732	1525.4	-0.21462	0.00070929	0.62548	liquid
310.52	2.5000	994.25	0.0010058	156.25	158.76	0.53623	4.0783	4.1733	1528.5	-0.21362	0.00068668	0.62794	liquid
312.18	2.5000	993.64	0.0010064	163.18	165.69	0.55849	4.0709	4.1734	1531.4	-0.21263	0.00066521	0.63034	liquid
313.84	2.5000	993.00	0.0010070	170.10	172.62	0.58062	4.0635	4.1736	1534.2	-0.21165	0.00064482	0.63268	liquid
315.50	2.5000	992.35	0.0010077	177.03	179.55	0.60264	4.0559	4.1739	1536.8	-0.21068	0.00062543	0.63497	liquid
317.16	2.5000	991.67	0.0010084	183.96	186.48	0.62454	4.0483	4.1743	1539.3	-0.20972	0.00060698	0.63719	liquid
318.82	2.5000	990.98	0.0010091	190.88	193.41	0.64633	4.0406	4.1746	1541.6	-0.20877	0.00058940	0.63935	liquid
320.48	2.5000	990.26	0.0010098	197.81	200.34	0.66801	4.0328	4.1751	1543.7	-0.20783	0.00057263	0.64145	liquid
322.14	2.5000	989.53	0.0010106	204.74	207.27	0.68959	4.0249	4.1755	1545.7	-0.20689	0.00055664	0.64349	liquid
323.80	2.5000	988.78	0.0010113	211.67	214.20	0.71105	4.0169	4.1760	1547.6	-0.20596	0.00054137	0.64548	liquid
325.46	2.5000	988.02	0.0010121	218.60	221.13	0.73240	4.0089	4.1766	1549.3	-0.20504	0.00052677	0.64740	liquid
327.12	2.5000	987.23	0.0010129	225.53	228.07	0.75365	4.0008	4.1772	1550.9	-0.20412	0.00051282	0.64926	liquid
328.78	2.5000	986.43	0.0010138	232.47	235.00	0.77480	3.9927	4.1778	1552.3	-0.20320	0.00049946	0.65106	liquid
330.44	2.5000	985.61	0.0010146	239.40	241.94	0.79584	3.9845	4.1785	1553.6	-0.20229	0.00048668	0.65281	liquid
332.10	2.5000	984.78	0.0010155	246.34	248.87	0.81678	3.9762	4.1792	1554.7	-0.20138	0.00047442	0.65449	liquid
333.76	2.5000	983.93	0.0010163	253.27	255.81	0.83762	3.9679	4.1799	1555.8	-0.20047	0.00046267	0.65612	liquid
335.42	2.5000	983.06	0.0010172	260.21	262.75	0.85836	3.9595	4.1807	1556.7	-0.19957	0.00045140	0.65769	liquid
337.08	2.5000	982.18	0.0010181	267.15	269.69	0.87900	3.9511	4.1815	1557.5	-0.19867	0.00044058	0.65921	liquid
338.74	2.5000	981.28	0.0010191	274.09	276.63	0.89955	3.9427	4.1824	1558.1	-0.19776	0.00043019	0.66068	liquid
340.40	2.5000	980.37	0.0010200	281.03	283.58	0.92000	3.9342	4.1833	1558.7	-0.19686	0.00042020	0.66209	liquid
342.06	2.5000	979.44	0.0010210	287.97	290.52	0.94035	3.9257	4.1842	1559.1	-0.19596	0.00041060	0.66344	liquid
343.72	2.5000	978.50	0.0010220	294.91	297.47	0.96061	3.9172	4.1852	1559.4	-0.19506	0.00040136	0.66475	liquid
345.38	2.5000	977.54	0.0010230	301.86	304.42	0.98077	3.9086	4.1862	1559.6	-0.19416	0.00039247	0.66600	liquid
347.04	2.5000	976.56	0.0010240	308.81	311.37	1.0008	3.9001	4.1873	1559.7	-0.19326	0.00038391	0.66721	liquid
348.70	2.5000	975.58	0.0010250	315.76	318.32	1.0208	3.8915	4.1884	1559.7	-0.19235	0.00037566	0.66837	liquid
350.36	2.5000	974.58	0.0010261	322.71	325.27	1.0407	3.8828	4.1895	1559.6	-0.19145	0.00036771	0.66948	liquid
352.02	2.5000	973.56	0.0010272	329.66	332.23	1.0605	3.8742	4.1907	1559.4	-0.19054	0.00036004	0.67054	liquid
353.68	2.5000	972.53	0.0010282	336.62	339.19	1.0803	3.8656	4.1919	1559.1	-0.18963	0.00035264	0.67155	liquid
355.34	2.5000	971.49	0.0010293	343.57	346.15	1.0999	3.8569	4.1932	1558.7	-0.18871	0.00034551	0.67253	liquid
357.00	2.5000	970.43	0.0010305	350.53	353.11	1.1194	3.8483	4.1945	1558.1	-0.18780	0.00033862	0.67346	liquid
358.66	2.5000	969.36	0.0010316	357.49	360.07	1.1389	3.8397	4.1959	1557.5	-0.18687	0.00033196	0.67434	liquid
360.32	2.5000	968.28	0.0010328	364.46	367.04	1.1583	3.8310	4.1973	1556.8	-0.18595	0.00032553	0.67519	liquid
361.98	2.5000	967.18	0.0010339	371.42	374.01	1.1776	3.8224	4.1988	1556.0	-0.18502	0.00031931	0.67599	liquid
363.64	2.5000	966.08	0.0010351	378.39	380.98	1.1968	3.8137	4.2003	1555.1	-0.18408	0.00031330	0.67675	liquid
365.30	2.5000	964.95	0.0010363	385.36	387.95	1.2159	3.8051	4.2019	1554.1	-0.18314	0.00030748	0.67748	liquid
366.96	2.5000	963.82	0.0010375	392.33	394.93	1.2350	3.7965	4.2036	1553.1	-0.18219	0.00030185	0.67817	liquid
368.62	2.5000	962.67	0.0010388	399.31	401.91	1.2539	3.7879	4.2053	1551.9	-0.18123	0.00029640	0.67881	liquid
370.28	2.5000	961.51	0.0010400	406.29	408.89	1.2728	3.7793	4.2070	1550.7	-0.18027	0.00029112	0.67943	liquid
371.94	2.5000	960.34	0.0010413	413.27	415.88	1.2917	3.7707	4.2088	1549.3	-0.17931	0.00028601	0.68001	liquid
373.60	2.5000	959.15	0.0010426	420.26	422.86	1.3104	3.7622	4.2107	1547.9	-0.17833	0.00028106	0.68055	liquid
375.26	2.5000	957.95	0.0010439	427.25	429.85	1.3291	3.7536	4.2126	1546.4	-0.17735	0.00027626	0.68106	liquid
376.92	2.5000	956.74	0.0010452	434.24	436.85	1.3477	3.7451	4.2146	1544.8	-0.17636	0.00027160	0.68153	liquid
378.58	2.5000	955.52	0.0010466	441.23	443.85	1.3662	3.7366	4.2167	1543.2	-0.17536	0.00026708	0.68198	liquid
380.24	2.5000	954.28	0.0010479	448.23	450.85	1.3847	3.7281	4.2188	1541.4	-0.17435	0.00026270	0.68239	liquid
381.90	2.5000	953.03	0.0010493	455.23	457.85	1.4030	3.7197	4.2210	1539.6	-0.17333	0.00025845	0.68277	liquid
383.56	2.5000	951.77	0.0010507	462.24	464.86	1.4214	3.7113	4.2232	1537.7	-0.17231	0.00025432	0.68311	liquid
385.22	2.5000	950.50	0.0010521	469.24	471.88	1.4396	3.7029	4.2256	1535.7	-0.17127	0.00025031	0.68343	liquid
386.88	2.5000	949.22	0.0010535	476.26	478.89	1.4578	3.6946	4.2280	1533.7	-0.17022	0.00024641	0.68372	liquid
388.54	2.5000	947.92	0.0010549	483.27	485.91	1.4759	3.6862	4.2304	1531.6	-0.16916	0.00024263	0.68398	liquid
390.20	2.5000	946.61	0.0010564	490.30	492.94	1.4939	3.6779	4.2330	1529.4	-0.16810	0.00023895	0.68421	liquid
391.86	2.5000	945.29	0.0010579	497.32	499.97	1.5119	3.6697	4.2356	1527.1	-0.16702	0.00023537	0.68441	liquid
393.52	2.5000	943.96	0.0010594	504.35	507.00	1.5298	3.6615	4.2383	1524.7	-0.16593	0.00023189	0.68459	liquid
395.18	2.5000	942.61	0.0010609	511.38	514.04	1.5477	3.6533	4.2410	1522.3	-0.16482	0.000		

423.40	2.5000	917.92	0.0010894	631.78	634.51	1.8421	3.5202	4.3012	1470.8	-0.14382	0.00018265	0.68337	liquid
425.06	2.5000	916.36	0.0010913	638.92	641.65	1.8589	3.5128	4.3056	1467.2	-0.14243	0.00018050	0.68307	liquid
426.72	2.5000	914.78	0.0010932	646.07	648.80	1.8757	3.5054	4.3101	1463.5	-0.14101	0.00017840	0.68275	liquid
428.38	2.5000	913.20	0.0010951	653.22	655.96	1.8925	3.4980	4.3147	1459.7	-0.13958	0.00017635	0.68241	liquid
430.04	2.5000	911.60	0.0010970	660.38	663.13	1.9092	3.4907	4.3195	1455.9	-0.13812	0.00017435	0.68204	liquid
431.70	2.5000	909.99	0.0010989	667.55	670.30	1.9258	3.4834	4.3243	1452.1	-0.13664	0.00017239	0.68165	liquid
433.36	2.5000	908.36	0.0011009	674.73	677.48	1.9424	3.4762	4.3293	1448.1	-0.13514	0.00017047	0.68123	liquid
435.02	2.5000	906.73	0.0011029	681.92	684.67	1.9590	3.4691	4.3344	1444.1	-0.13362	0.00016860	0.68080	liquid
436.68	2.5000	905.08	0.0011049	689.11	691.87	1.9755	3.4619	4.3396	1440.1	-0.13207	0.00016676	0.68034	liquid
438.34	2.5000	903.42	0.0011069	696.31	699.08	1.9920	3.4549	4.3449	1436.0	-0.13049	0.00016497	0.67985	liquid
440.00	2.5000	901.74	0.0011090	703.52	706.30	2.0084	3.4478	4.3503	1431.8	-0.12889	0.00016321	0.67935	liquid
441.66	2.5000	900.05	0.0011110	710.75	713.52	2.0248	3.4409	4.3559	1427.5	-0.12726	0.00016149	0.67882	liquid
443.32	2.5000	898.35	0.0011132	717.98	720.76	2.0411	3.4339	4.3616	1423.2	-0.12561	0.00015981	0.67826	liquid
444.98	2.5000	896.64	0.0011153	725.22	728.00	2.0575	3.4270	4.3675	1418.9	-0.12393	0.00015816	0.67768	liquid
446.64	2.5000	894.91	0.0011174	732.47	735.26	2.0737	3.4202	4.3734	1414.5	-0.12222	0.00015654	0.67708	liquid
448.30	2.5000	893.17	0.0011196	739.73	742.52	2.0900	3.4134	4.3796	1410.0	-0.12048	0.00015496	0.67646	liquid
449.96	2.5000	891.41	0.0011218	746.99	749.80	2.1062	3.4067	4.3858	1405.4	-0.11871	0.00015340	0.67581	liquid
451.62	2.5000	889.64	0.0011240	754.28	757.09	2.1223	3.4000	4.3922	1400.8	-0.11691	0.00015188	0.67513	liquid
453.28	2.5000	887.86	0.0011263	761.57	764.38	2.1385	3.3933	4.3988	1396.2	-0.11508	0.00015039	0.67444	liquid
454.94	2.5000	886.06	0.0011286	768.87	771.69	2.1545	3.3867	4.4055	1391.4	-0.11322	0.00014893	0.67371	liquid
456.60	2.5000	884.25	0.0011309	776.18	779.01	2.1706	3.3801	4.4124	1386.6	-0.11132	0.00014749	0.67297	liquid
458.26	2.5000	882.42	0.0011332	783.51	786.34	2.1866	3.3736	4.4194	1381.8	-0.10939	0.00014609	0.67220	liquid
459.92	2.5000	880.58	0.0011356	790.84	793.68	2.2026	3.3672	4.4266	1376.9	-0.10742	0.00014471	0.67140	liquid
461.58	2.5000	878.73	0.0011380	798.19	801.03	2.2186	3.3607	4.4340	1371.9	-0.10541	0.00014335	0.67058	liquid
463.24	2.5000	876.86	0.0011404	805.55	808.40	2.2345	3.3544	4.4415	1366.9	-0.10337	0.00014202	0.66973	liquid
464.90	2.5000	874.97	0.0011429	812.92	815.78	2.2504	3.3481	4.4492	1361.8	-0.10129	0.00014071	0.66886	liquid
466.56	2.5000	873.07	0.0011454	820.31	823.17	2.2663	3.3418	4.4571	1356.6	-0.099168	0.00013943	0.66794	liquid
468.22	2.5000	871.16	0.0011479	827.71	830.58	2.2821	3.3355	4.4652	1351.4	-0.097005	0.00013817	0.66704	liquid
469.88	2.5000	869.23	0.0011504	835.12	838.00	2.2979	3.3294	4.4735	1346.1	-0.094800	0.00013693	0.66609	liquid
471.54	2.5000	867.28	0.0011530	842.55	845.43	2.3137	3.3232	4.4819	1340.8	-0.092551	0.00013572	0.66511	liquid
473.20	2.5000	865.32	0.0011556	849.99	852.88	2.3295	3.3171	4.4906	1335.3	-0.090256	0.00013452	0.66411	liquid
474.86	2.5000	863.34	0.0011583	857.44	860.34	2.3452	3.3111	4.4995	1329.9	-0.087916	0.00013334	0.66308	liquid
476.52	2.5000	861.34	0.0011610	864.91	867.82	2.3610	3.3051	4.5086	1324.3	-0.085526	0.00013219	0.66202	liquid
478.18	2.5000	859.33	0.0011637	872.40	875.31	2.3767	3.2992	4.5179	1318.7	-0.083088	0.00013105	0.66094	liquid
479.84	2.5000	857.30	0.0011665	879.90	882.82	2.3923	3.2933	4.5275	1313.1	-0.080598	0.00012993	0.65982	liquid
481.50	2.5000	855.25	0.0011692	887.42	890.34	2.4080	3.2874	4.5372	1307.3	-0.078055	0.00012883	0.65868	liquid
483.16	2.5000	853.19	0.0011721	894.95	897.88	2.4236	3.2816	4.5473	1301.5	-0.075458	0.00012775	0.65751	liquid
484.82	2.5000	851.11	0.0011749	902.50	905.44	2.4392	3.2759	4.5575	1295.7	-0.072804	0.00012668	0.65631	liquid
486.48	2.5000	849.01	0.0011778	910.07	913.01	2.4548	3.2702	4.5681	1289.8	-0.070092	0.00012563	0.65508	liquid
488.14	2.5000	846.89	0.0011808	917.65	920.60	2.4704	3.2645	4.5789	1283.8	-0.067320	0.00012459	0.65382	liquid
489.80	2.5000	844.75	0.0011838	925.25	928.21	2.4860	3.2589	4.5900	1277.7	-0.064485	0.00012357	0.65253	liquid
491.46	2.5000	842.60	0.0011868	932.87	935.84	2.5015	3.2534	4.6013	1271.6	-0.061586	0.00012257	0.65121	liquid
493.12	2.5000	840.42	0.0011899	940.51	943.49	2.5171	3.2479	4.6130	1265.4	-0.058620	0.00012158	0.64986	liquid
494.78	2.5000	838.22	0.0011930	948.17	951.16	2.5326	3.2424	4.6249	1259.1	-0.055584	0.00012060	0.64847	liquid
496.44	2.5000	836.01	0.0011962	955.85	958.84	2.5481	3.2370	4.6372	1252.8	-0.052477	0.00011964	0.64706	liquid
497.10	2.5000	833.12	0.0011994	958.91	961.91	2.5543	3.2349	4.6422	1250.2	-0.051221	0.00011926	0.64648	liquid
497.10	2.5000	12.508	0.079949	2602.1	2801.9	6.2558	2.2483	3.4050	504.67	19.935	1.6550e-05	0.045025	vapor
498.10	2.5000	12.462	0.080245	2604.7	2805.3	6.2626	2.2228	3.3595	505.86	19.794	1.6597e-05	0.045004	vapor
499.76	2.5000	12.387	0.080731	2609.0	2810.8	6.2736	2.1849	3.2915	507.76	19.563	1.6676e-05	0.044974	vapor
501.42	2.5000	12.314	0.081209	2613.2	2816.2	6.2844	2.1517	3.2313	509.59	19.335	1.6754e-05	0.044951	vapor
503.08	2.5000	12.243	0.081682	2617.4	2821.6	6.2950	2.1224	3.1776	511.35	19.111	1.6832e-05	0.044935	vapor
504.74	2.5000	12.173	0.082149	2621.4	2826.8	6.3054	2.0963	3.1293	513.05	18.891	1.6910e-05	0.044925	vapor
506.40	2.5000	12.105	0.082611	2625.4	2832.0	6.3156	2.0729	3.0856	514.70	18.675	1.6987e-05	0.044921	vapor
508.06	2.5000	12.038	0.083069	2629.4	2837.0	6.3257	2.0517	3.0457	516.31	18.463	1.7065e-05	0.044922	vapor
509.72	2.5000	11.973	0.083522	2633.3	2842.1	6.3355	2.0325	3.0091	517.88	18.254	1.7142e-05	0.044929	vapor
511.38	2.5000	11.909	0.083971	2637.1	2847.0	6.3453	2.0149	2.9752	519.41	18.049	1.7219e-05	0.044942	vapor
513.04	2.5000	11.846	0.084416	2640.9	2851.9	6.3548	1.9986	2.9438	520.92	17.848	1.7297e-05	0.044959	vapor
514.70	2.5000	11.785	0.084857	2644.7	2856.8	6.3643	1.9836	2.9146	522.39	17.650	1.7374e-05	0.044981	vapor
516.36	2.5000	11.724	0.085295	2648.4	2861.6	6.3736	1.9696	2.8871	523.84	17.455	1.7450e-05	0.045007	vapor
518.02	2.5000	11.665	0.085729	2652.1	2866.4	6.3829	1.9565	2.8614	525.27	17.264	1.7527e-05	0.045038	vapor
519.68	2.5000	11.606	0.086161	2655.7	2871.1	6.3920	1.9443	2.8370	526.68	17.075	1.7604e-05	0.045073	vapor
521.34	2.5000	11.549	0.086589	2659.3	2875.8	6.4010	1.9327	2.8141	528.06	16.890	1.7680e-05	0.045112	vapor
523.00	2.5000	11.492	0.087015	2662.9	2880.5	6.4099	1.9218	2.7923	529.43	16.708	1.7757e-05	0.045155	vapor
524.66	2.5000	11.437	0.087438	2666.5	2885.1	6.4187	1.9115	2.7715	530.78	16.528	1.7833e-05	0.045202	vapor
526.32	2.5000	11.382	0.087858	2670.0	2889.7	6.4275	1.9017	2.7518	532.11	16.351	1.7909e-05	0.045252	vapor
527.98	2.5000	11.328	0.088276	2673.5	2894.2	6.4361	1.8924	2.7330	533.43	16.177	1.7985e-05	0.045306	vapor
529.64	2.5000	11.275	0.088691	2677.0	2898.7	6.4446	1.8836	2.7150	534.74	16.006	1.8061e-05	0.045364	vapor
531.30	2.5000	11.223	0.089104	2680.5	2903.2	6.4531	1.8751	2.6978	536.03	15.837	1.8137e-05	0.045424	vapor
532.96	2.5000	11.171	0.089515	2683.9	2907.7	6.4615	1.8670	2.6814	537.30	15.671	1.8213e-05	0.045488	vapor
534.62	2.5000	11.121	0.089924	2687.3	2912.1	6.4698	1.8593	2.6656	538.57	15.507	1.8288e-05	0.045556	vapor
536.28	2.5000	11.070	0.090330	2690.7	2916.6	6.4781	1.8519	2.6504	539.82	15.345	1.8364e-05	0.045626	vapor
537.94	2.5000	11.021	0.090735	2694.1	2920.9	6.4862	1.8448	2.6359	541.06	15.186	1.8440e-05	0.045699	vapor
539.60	2.5000	10.972	0.091137	2697.5	2925.3	6.4943	1.8380	2.6219	542.30	15.030	1.8515e-05	0.045775	vapor
541.26	2.5000	10.924	0.091538	2700.8	2929.6	6.5024	1.8315	2.6084	543.52	14.875	1.8590e-05	0.045854	vapor
542.92	2.5000	10.877	0.091937	2704.1	2934.0	6.5103	1.8252	2.5955	544.73	14.723	1.8666e-05	0.045935	vapor
544.58	2.5000	10.830	0.092334	2707.4	2938.3	6.5182	1.8192	2.5830	545.93	14.573	1.		

577.78	2.5000	10.003	0.099973	2770.8	3020.8	6.6653	1.7371	2.4067	568.22	11.984	2.0229e-05	0.048159	vapor
579.44	2.5000	9.9659	0.10034	2773.9	3024.8	6.6722	1.7344	2.4006	569.26	11.872	2.0303e-05	0.048285	vapor
581.10	2.5000	9.9294	0.10071	2777.0	3028.7	6.6791	1.7318	2.3946	570.30	11.763	2.0377e-05	0.048412	vapor
582.76	2.5000	9.8933	0.10108	2780.0	3032.7	6.6859	1.7293	2.3889	571.33	11.654	2.0450e-05	0.048541	vapor
584.42	2.5000	9.8575	0.10145	2783.1	3036.7	6.6927	1.7269	2.3833	572.36	11.547	2.0524e-05	0.048672	vapor
586.08	2.5000	9.8221	0.10181	2786.1	3040.6	6.6994	1.7246	2.3779	573.38	11.442	2.0598e-05	0.048804	vapor
587.74	2.5000	9.7870	0.10218	2789.1	3044.6	6.7062	1.7224	2.3727	574.40	11.338	2.0671e-05	0.048937	vapor
589.40	2.5000	9.7522	0.10254	2792.1	3048.5	6.7129	1.7202	2.3676	575.41	11.235	2.0745e-05	0.049072	vapor
591.06	2.5000	9.7178	0.10290	2795.2	3052.4	6.7195	1.7182	2.3627	576.42	11.134	2.0818e-05	0.049207	vapor
592.72	2.5000	9.6837	0.10327	2798.2	3056.3	6.7261	1.7162	2.3579	577.42	11.034	2.0891e-05	0.049345	vapor
594.38	2.5000	9.6499	0.10363	2801.2	3060.2	6.7327	1.7143	2.3533	578.42	10.936	2.0965e-05	0.049483	vapor
596.04	2.5000	9.6164	0.10399	2804.2	3064.2	6.7393	1.7125	2.3488	579.41	10.839	2.1038e-05	0.049623	vapor
597.70	2.5000	9.5832	0.10435	2807.2	3068.0	6.7458	1.7108	2.3445	580.40	10.743	2.1111e-05	0.049764	vapor
599.36	2.5000	9.5503	0.10471	2810.2	3071.9	6.7523	1.7091	2.3403	581.38	10.648	2.1184e-05	0.049906	vapor
601.02	2.5000	9.5177	0.10507	2813.1	3075.8	6.7588	1.7075	2.3362	582.36	10.555	2.1257e-05	0.050050	vapor
602.68	2.5000	9.4854	0.10543	2816.1	3079.7	6.7652	1.7059	2.3322	583.33	10.462	2.1330e-05	0.050194	vapor
604.34	2.5000	9.4534	0.10578	2819.1	3083.6	6.7716	1.7045	2.3284	584.30	10.371	2.1403e-05	0.050340	vapor
606.00	2.5000	9.4216	0.10614	2822.1	3087.4	6.7780	1.7030	2.3246	585.27	10.281	2.1476e-05	0.050487	vapor
607.66	2.5000	9.3901	0.10649	2825.0	3091.3	6.7843	1.7017	2.3210	586.23	10.193	2.1549e-05	0.050635	vapor
609.32	2.5000	9.3589	0.10685	2828.0	3095.1	6.7907	1.7004	2.3175	587.19	10.105	2.1622e-05	0.050784	vapor
610.98	2.5000	9.3279	0.10720	2831.0	3099.0	6.7970	1.6991	2.3141	588.14	10.019	2.1695e-05	0.050934	vapor
612.64	2.5000	9.2973	0.10756	2833.9	3102.8	6.8032	1.6980	2.3108	589.09	9.9334	2.1767e-05	0.051085	vapor
614.30	2.5000	9.2668	0.10791	2836.9	3106.6	6.8095	1.6968	2.3076	590.04	9.8492	2.1840e-05	0.051237	vapor
615.96	2.5000	9.2366	0.10826	2839.8	3110.5	6.8157	1.6957	2.3045	590.98	9.7660	2.1913e-05	0.051390	vapor
617.62	2.5000	9.2067	0.10862	2842.8	3114.3	6.8219	1.6947	2.3014	591.92	9.6839	2.1986e-05	0.051544	vapor
619.28	2.5000	9.1770	0.10897	2845.7	3118.1	6.8281	1.6937	2.2985	592.85	9.6028	2.2058e-05	0.051698	vapor
620.94	2.5000	9.1475	0.10932	2848.6	3121.9	6.8342	1.6928	2.2957	593.79	9.5227	2.2131e-05	0.051854	vapor
622.60	2.5000	9.1183	0.10967	2851.6	3125.7	6.8404	1.6919	2.2929	594.71	9.4435	2.2203e-05	0.052011	vapor
624.26	2.5000	9.0893	0.11002	2854.5	3129.5	6.8465	1.6910	2.2902	595.64	9.3654	2.2276e-05	0.052169	vapor
625.92	2.5000	9.0605	0.11037	2857.4	3133.3	6.8525	1.6902	2.2877	596.56	9.2883	2.2348e-05	0.052327	vapor
627.58	2.5000	9.0320	0.11072	2860.3	3137.1	6.8586	1.6895	2.2851	597.47	9.2120	2.2420e-05	0.052487	vapor
629.24	2.5000	9.0037	0.11107	2863.3	3140.9	6.8646	1.6888	2.2827	598.39	9.1368	2.2493e-05	0.052647	vapor
630.90	2.5000	8.9755	0.11141	2866.2	3144.7	6.8706	1.6881	2.2803	599.30	9.0624	2.2565e-05	0.052807	vapor
632.56	2.5000	8.9477	0.11176	2869.1	3148.5	6.8766	1.6874	2.2780	600.20	8.9889	2.2637e-05	0.052970	vapor
634.22	2.5000	8.9200	0.11211	2872.0	3152.3	6.8826	1.6868	2.2758	601.11	8.9163	2.2709e-05	0.053132	vapor
635.88	2.5000	8.8925	0.11245	2874.9	3156.1	6.8885	1.6863	2.2737	602.01	8.8446	2.2781e-05	0.053296	vapor
637.54	2.5000	8.8652	0.11280	2877.8	3159.8	6.8945	1.6857	2.2716	602.91	8.7738	2.2854e-05	0.053460	vapor
639.20	2.5000	8.8382	0.11315	2880.7	3163.6	6.9004	1.6852	2.2695	603.80	8.7037	2.2926e-05	0.053625	vapor
640.86	2.5000	8.8113	0.11349	2883.6	3167.4	6.9063	1.6848	2.2676	604.69	8.6346	2.2998e-05	0.053791	vapor
642.52	2.5000	8.7847	0.11383	2886.5	3171.1	6.9121	1.6843	2.2657	605.58	8.5662	2.3070e-05	0.053958	vapor
644.18	2.5000	8.7582	0.11418	2889.4	3174.9	6.9180	1.6839	2.2638	606.47	8.4986	2.3142e-05	0.054125	vapor
645.84	2.5000	8.7319	0.11452	2892.3	3178.6	6.9238	1.6836	2.2621	607.35	8.4319	2.3213e-05	0.054293	vapor
647.50	2.5000	8.7058	0.11487	2895.2	3182.4	6.9296	1.6832	2.2603	608.23	8.3659	2.3285e-05	0.054462	vapor
649.16	2.5000	8.6799	0.11521	2898.1	3186.1	6.9354	1.6829	2.2587	609.11	8.3006	2.3357e-05	0.054631	vapor
650.82	2.5000	8.6542	0.11555	2901.0	3189.9	6.9411	1.6827	2.2570	609.98	8.2362	2.3429e-05	0.054801	vapor
652.48	2.5000	8.6287	0.11589	2903.9	3193.6	6.9469	1.6824	2.2555	610.85	8.1724	2.3501e-05	0.054972	vapor
654.14	2.5000	8.6033	0.11623	2906.8	3197.4	6.9526	1.6822	2.2540	611.72	8.1094	2.3572e-05	0.055143	vapor
655.80	2.5000	8.5781	0.11658	2909.7	3201.1	6.9583	1.6820	2.2525	612.59	8.0472	2.3644e-05	0.055315	vapor
657.46	2.5000	8.5531	0.11692	2912.6	3204.9	6.9640	1.6818	2.2511	613.45	7.9856	2.3716e-05	0.055488	vapor
659.12	2.5000	8.5283	0.11726	2915.5	3208.6	6.9697	1.6817	2.2497	614.31	7.9247	2.3787e-05	0.055661	vapor
660.78	2.5000	8.5037	0.11760	2918.3	3212.3	6.9754	1.6816	2.2484	615.17	7.8645	2.3859e-05	0.055835	vapor
662.44	2.5000	8.4792	0.11794	2921.2	3216.1	6.9810	1.6815	2.2471	616.02	7.8050	2.3930e-05	0.056010	vapor
664.10	2.5000	8.4548	0.11828	2924.1	3219.8	6.9866	1.6814	2.2459	616.88	7.7461	2.4002e-05	0.056185	vapor
665.76	2.5000	8.4307	0.11861	2927.0	3223.5	6.9922	1.6813	2.2447	617.73	7.6879	2.4073e-05	0.056361	vapor
667.42	2.5000	8.4067	0.11895	2929.9	3227.2	6.9978	1.6813	2.2435	618.57	7.6304	2.4144e-05	0.056537	vapor
669.08	2.5000	8.3828	0.11929	2932.7	3231.0	7.0034	1.6813	2.2424	619.42	7.5734	2.4216e-05	0.056714	vapor
670.74	2.5000	8.3592	0.11963	2935.6	3234.7	7.0089	1.6813	2.2413	620.26	7.5171	2.4287e-05	0.056892	vapor
672.40	2.5000	8.3356	0.11997	2938.5	3238.4	7.0145	1.6814	2.2403	621.10	7.4615	2.4358e-05	0.057070	vapor
674.06	2.5000	8.3123	0.12030	2941.4	3242.1	7.0200	1.6814	2.2393	621.94	7.4064	2.4430e-05	0.057248	vapor
675.72	2.5000	8.2891	0.12064	2944.2	3245.8	7.0255	1.6815	2.2383	622.78	7.3519	2.4501e-05	0.057428	vapor
677.38	2.5000	8.2660	0.12098	2947.1	3249.6	7.0310	1.6816	2.2374	623.61	7.2980	2.4572e-05	0.057607	vapor
679.04	2.5000	8.2431	0.12131	2950.0	3253.3	7.0365	1.6817	2.2365	624.44	7.2447	2.4643e-05	0.057788	vapor
680.70	2.5000	8.2203	0.12165	2952.9	3257.0	7.0419	1.6818	2.2357	625.27	7.1920	2.4714e-05	0.057968	vapor
682.36	2.5000	8.1977	0.12199	2955.7	3260.7	7.0474	1.6820	2.2349	626.10	7.1398	2.4785e-05	0.058150	vapor
684.02	2.5000	8.1752	0.12232	2958.6	3264.4	7.0528	1.6822	2.2341	626.92	7.0882	2.4856e-05	0.058331	vapor
685.68	2.5000	8.1529	0.12266	2961.5	3268.1	7.0582	1.6823	2.2333	627.75	7.0371	2.4927e-05	0.058514	vapor
687.34	2.5000	8.1307	0.12299	2964.3	3271.8	7.0636	1.6826	2.2326	628.57	6.9866	2.4998e-05	0.058697	vapor
689.00	2.5000	8.1086	0.12333	2967.2	3275.5	7.0690	1.6828	2.2319	629.38	6.9365	2.5069e-05	0.058880	vapor
690.66	2.5000	8.0867	0.12366	2970.1	3279.2	7.0744	1.6830	2.2312	630.20	6.8871	2.5140e-05	0.059064	vapor
692.32	2.5000	8.0649	0.12399	2972.9	3282.9	7.0797	1.6833	2.2306	631.01	6.8381	2.5210e-05	0.059248	vapor
693.98	2.5000	8.0433	0.12433	2975.8	3286.6	7.0851	1.6835	2.2300	631.83	6.7896	2.5281e-05	0.059433	vapor
695.64	2.5000	8.0217	0.12466	2978.7	3290.3	7.0904	1.6838	2.2294	632.64	6.7417	2.5352e-05	0.059618	vapor
697.30	2.5000	8.0004	0.12499	2981.5	3294.0	7.0957	1.6841	2.2289	633.44	6.6942	2.5423e-05	0.059804	vapor
698.96	2.5000	7.9791	0.12533	2984.4	3297.7	7.1010	1.6844	2.2284	634.25	6.6472	2.5493e-05	0.059990	vapor
700.62	2.5000	7.9580	0.12566	2987.3	3301.4	7.1063	1.6848	2.2279	635.05	6.6007	2.5564e-05	0.060177	vapor
702.28	2.5000	7.9370	0.12599	2990.1	3305.1	7.1116	1.6851	2.2274	635.85	6.5547	2.5634e-05	0.060364	vapor
703.94	2.5000	7.9161	0.12632	2993.0	3308.8	7.1168	1.6855	2.2270	636.				

735.48	2.5000	7.5418	0.13259	3047.5	3379.0	7.2143	1.6945	2.2229	651.50	5.7239	2.7038e-05	0.064193	vapor
737.14	2.5000	7.5232	0.13292	3050.4	3382.7	7.2193	1.6950	2.2228	652.27	5.6864	2.7108e-05	0.064389	vapor
738.80	2.5000	7.5047	0.13325	3053.2	3386.4	7.2243	1.6956	2.2228	653.03	5.6493	2.7178e-05	0.064585	vapor
740.46	2.5000	7.4863	0.13358	3056.1	3390.0	7.2293	1.6962	2.2228	653.79	5.6125	2.7247e-05	0.064781	vapor
742.12	2.5000	7.4680	0.13390	3059.0	3393.7	7.2343	1.6968	2.2229	654.55	5.5761	2.7317e-05	0.064978	vapor
743.78	2.5000	7.4498	0.13423	3061.8	3397.4	7.2393	1.6974	2.2229	655.31	5.5400	2.7387e-05	0.065175	vapor
745.44	2.5000	7.4317	0.13456	3064.7	3401.1	7.2442	1.6981	2.2230	656.06	5.5042	2.7456e-05	0.065372	vapor
747.10	2.5000	7.4137	0.13489	3067.6	3404.8	7.2492	1.6987	2.2231	656.82	5.4688	2.7526e-05	0.065570	vapor
748.76	2.5000	7.3958	0.13521	3070.5	3408.5	7.2541	1.6993	2.2231	657.57	5.4337	2.7595e-05	0.065768	vapor
750.42	2.5000	7.3780	0.13554	3073.3	3412.2	7.2590	1.7000	2.2232	658.32	5.3989	2.7665e-05	0.065966	vapor
752.08	2.5000	7.3603	0.13586	3076.2	3415.9	7.2639	1.7006	2.2234	659.07	5.3644	2.7734e-05	0.066165	vapor
753.74	2.5000	7.3426	0.13619	3079.1	3419.6	7.2688	1.7013	2.2235	659.82	5.3302	2.7804e-05	0.066364	vapor
755.40	2.5000	7.3251	0.13652	3082.0	3423.3	7.2737	1.7020	2.2236	660.57	5.2964	2.7873e-05	0.066563	vapor
757.06	2.5000	7.3077	0.13684	3084.8	3427.0	7.2786	1.7026	2.2238	661.31	5.2628	2.7943e-05	0.066763	vapor
758.72	2.5000	7.2903	0.13717	3087.7	3430.6	7.2835	1.7033	2.2240	662.06	5.2296	2.8012e-05	0.066963	vapor
760.38	2.5000	7.2731	0.13749	3090.6	3434.3	7.2883	1.7040	2.2242	662.80	5.1967	2.8081e-05	0.067163	vapor
762.04	2.5000	7.2559	0.13782	3093.5	3438.0	7.2932	1.7047	2.2244	663.54	5.1640	2.8150e-05	0.067364	vapor
763.70	2.5000	7.2388	0.13814	3096.4	3441.7	7.2980	1.7054	2.2246	664.28	5.1316	2.8220e-05	0.067565	vapor
765.36	2.5000	7.2218	0.13847	3099.2	3445.4	7.3029	1.7061	2.2248	665.02	5.0996	2.8289e-05	0.067766	vapor
767.02	2.5000	7.2049	0.13879	3102.1	3449.1	7.3077	1.7068	2.2251	665.75	5.0678	2.8358e-05	0.067968	vapor
768.68	2.5000	7.1881	0.13912	3105.0	3452.8	7.3125	1.7076	2.2253	666.49	5.0362	2.8427e-05	0.068169	vapor
770.34	2.5000	7.1714	0.13944	3107.9	3456.5	7.3173	1.7083	2.2256	667.22	5.0050	2.8496e-05	0.068372	vapor
772.00	2.5000	7.1547	0.13977	3110.8	3460.2	7.3221	1.7090	2.2259	667.96	4.9740	2.8565e-05	0.068574	vapor
773.66	2.5000	7.1382	0.14009	3113.7	3463.9	7.3269	1.7098	2.2261	668.69	4.9433	2.8634e-05	0.068777	vapor
775.32	2.5000	7.1217	0.14042	3116.5	3467.6	7.3316	1.7105	2.2264	669.42	4.9129	2.8703e-05	0.068980	vapor
776.98	2.5000	7.1053	0.14074	3119.4	3471.3	7.3364	1.7113	2.2268	670.15	4.8828	2.8772e-05	0.069184	vapor
778.64	2.5000	7.0890	0.14106	3122.3	3475.0	7.3412	1.7120	2.2271	670.87	4.8529	2.8841e-05	0.069387	vapor
780.30	2.5000	7.0728	0.14139	3125.2	3478.7	7.3459	1.7128	2.2274	671.60	4.8232	2.8910e-05	0.069591	vapor
781.96	2.5000	7.0566	0.14171	3128.1	3482.4	7.3506	1.7136	2.2278	672.32	4.7938	2.8978e-05	0.069796	vapor
783.62	2.5000	7.0405	0.14203	3131.0	3486.1	7.3554	1.7143	2.2281	673.05	4.7647	2.9047e-05	0.070000	vapor
785.28	2.5000	7.0246	0.14236	3133.9	3489.8	7.3601	1.7151	2.2285	673.77	4.7358	2.9116e-05	0.070205	vapor
786.94	2.5000	7.0086	0.14268	3136.8	3493.5	7.3648	1.7159	2.2288	674.49	4.7071	2.9185e-05	0.070410	vapor
788.60	2.5000	6.9928	0.14300	3139.7	3497.2	7.3695	1.7167	2.2292	675.21	4.6787	2.9253e-05	0.070616	vapor
790.26	2.5000	6.9771	0.14333	3142.5	3500.9	7.3742	1.7175	2.2296	675.93	4.6506	2.9322e-05	0.070821	vapor
791.92	2.5000	6.9614	0.14365	3145.4	3504.6	7.3788	1.7183	2.2300	676.64	4.6226	2.9391e-05	0.071027	vapor
793.58	2.5000	6.9458	0.14397	3148.3	3508.3	7.3835	1.7191	2.2304	677.36	4.5949	2.9459e-05	0.071234	vapor
795.24	2.5000	6.9303	0.14429	3151.2	3512.0	7.3882	1.7199	2.2309	678.07	4.5675	2.9528e-05	0.071440	vapor
796.90	2.5000	6.9148	0.14462	3154.1	3515.7	7.3928	1.7208	2.2313	678.78	4.5402	2.9596e-05	0.071647	vapor
798.56	2.5000	6.8994	0.14494	3157.0	3519.4	7.3975	1.7216	2.2318	679.50	4.5132	2.9664e-05	0.071854	vapor
800.22	2.5000	6.8841	0.14526	3159.9	3523.1	7.4021	1.7224	2.2322	680.21	4.4864	2.9733e-05	0.072061	vapor
801.88	2.5000	6.8689	0.14558	3162.8	3526.8	7.4067	1.7233	2.2327	680.91	4.4599	2.9801e-05	0.072269	vapor
803.54	2.5000	6.8537	0.14591	3165.7	3530.5	7.4113	1.7241	2.2331	681.62	4.4335	2.9870e-05	0.072477	vapor
805.20	2.5000	6.8387	0.14623	3168.6	3534.2	7.4160	1.7249	2.2336	682.33	4.4074	2.9938e-05	0.072685	vapor
806.86	2.5000	6.8236	0.14655	3171.5	3537.9	7.4206	1.7258	2.2341	683.03	4.3815	3.0006e-05	0.072893	vapor
808.52	2.5000	6.8087	0.14687	3174.4	3541.6	7.4251	1.7266	2.2346	683.74	4.3558	3.0074e-05	0.073101	vapor
810.18	2.5000	6.7938	0.14719	3177.4	3545.3	7.4297	1.7275	2.2351	684.44	4.3303	3.0143e-05	0.073311	vapor
811.84	2.5000	6.7790	0.14751	3180.3	3549.0	7.4343	1.7284	2.2356	685.14	4.3050	3.0211e-05	0.073520	vapor
813.50	2.5000	6.7643	0.14783	3183.2	3552.8	7.4389	1.7292	2.2361	685.84	4.2799	3.0279e-05	0.073729	vapor
815.16	2.5000	6.7496	0.14816	3186.1	3556.5	7.4434	1.7301	2.2367	686.54	4.2551	3.0347e-05	0.073939	vapor
816.82	2.5000	6.7350	0.14848	3189.0	3560.2	7.4480	1.7310	2.2372	687.24	4.2304	3.0415e-05	0.074149	vapor
818.48	2.5000	6.7205	0.14880	3191.9	3563.9	7.4525	1.7318	2.2377	687.94	4.2059	3.0483e-05	0.074359	vapor
820.14	2.5000	6.7061	0.14912	3194.8	3567.6	7.4571	1.7327	2.2383	688.63	4.1816	3.0551e-05	0.074569	vapor
821.80	2.5000	6.6917	0.14944	3197.7	3571.3	7.4616	1.7336	2.2389	689.33	4.1575	3.0619e-05	0.074780	vapor
823.46	2.5000	6.6773	0.14976	3200.6	3575.0	7.4661	1.7345	2.2394	690.02	4.1336	3.0687e-05	0.074991	vapor
825.12	2.5000	6.6631	0.15008	3203.6	3578.8	7.4706	1.7354	2.2400	690.71	4.1099	3.0755e-05	0.075202	vapor
826.78	2.5000	6.6489	0.15040	3206.5	3582.5	7.4751	1.7363	2.2406	691.41	4.0864	3.0822e-05	0.075413	vapor
828.44	2.5000	6.6348	0.15072	3209.4	3586.2	7.4796	1.7372	2.2412	692.10	4.0631	3.0890e-05	0.075625	vapor
830.10	2.5000	6.6207	0.15104	3212.3	3589.9	7.4841	1.7381	2.2418	692.79	4.0399	3.0958e-05	0.075836	vapor
831.76	2.5000	6.6067	0.15136	3215.2	3593.6	7.4886	1.7390	2.2424	693.47	4.0170	3.1026e-05	0.076048	vapor
833.42	2.5000	6.5928	0.15168	3218.2	3597.4	7.4931	1.7399	2.2430	694.16	3.9942	3.1093e-05	0.076260	vapor
835.08	2.5000	6.5789	0.15200	3221.1	3601.1	7.4975	1.7408	2.2436	694.85	3.9716	3.1161e-05	0.076473	vapor
836.74	2.5000	6.5651	0.15232	3224.0	3604.8	7.5020	1.7418	2.2442	695.53	3.9491	3.1228e-05	0.076686	vapor
838.40	2.5000	6.5513	0.15264	3226.9	3608.5	7.5064	1.7427	2.2448	696.21	3.9269	3.1296e-05	0.076898	vapor
840.06	2.5000	6.5376	0.15296	3229.9	3612.3	7.5109	1.7436	2.2455	696.90	3.9048	3.1364e-05	0.077111	vapor
841.72	2.5000	6.5240	0.15328	3232.8	3616.0	7.5153	1.7445	2.2461	697.58	3.8828	3.1431e-05	0.077325	vapor
843.38	2.5000	6.5104	0.15360	3235.7	3619.7	7.5197	1.7455	2.2468	698.26	3.8611	3.1498e-05	0.077538	vapor
845.04	2.5000	6.4969	0.15392	3238.7	3623.5	7.5241	1.7464	2.2474	698.94	3.8395	3.1566e-05	0.077752	vapor
846.70	2.5000	6.4835	0.15424	3241.6	3627.2	7.5285	1.7473	2.2481	699.62	3.8181	3.1633e-05	0.077966	vapor
848.36	2.5000	6.4701	0.15456	3244.5	3630.9	7.5330	1.7483	2.2487	700.29	3.7968	3.1701e-05	0.078180	vapor
850.02	2.5000	6.4567	0.15488	3247.5	3634.7	7.5373	1.7492	2.2494	700.97	3.7757	3.1768e-05	0.078394	vapor
851.68	2.5000	6.4435	0.15520	3250.4	3638.4	7.5417	1.7502	2.2501	701.65	3.7548	3.1835e-05	0.078609	vapor
853.34	2.5000	6.4303	0.15551	3253.3	3642.1	7.5461	1.7511	2.2508	702.32	3.7340	3.1902e-05	0.078824	vapor
855.00	2.5000	6.4171	0.15583	3256.3	3645.9	7.5505	1.7521	2.2514	702.99	3.7134	3.1970e-05	0.079039	vapor
856.66	2.5000	6.4040	0.15615	3259.2	3649.6	7.5549	1.7530	2.2521	703.67	3.6930	3.2037e-05	0.079254	vapor
858.32	2.5000	6.3910	0.15647	3262.2	3653.3	7.5592	1.7540	2.2528	704.34	3.6726	3.2104e-05	0.079469	vapor
859.98	2.5000	6.3780	0.15679	3265.1	3657.1	7.5636	1.7550	2.2535	705.01	3.6525	3.2171e-05	0.079685	vapor
861.64	2.5000	6.3651	0.15711	3268.0	3660.8	7.5679	1.7559	2.2542	705.6				

893.18	2.5000	6.1295	0.16314	3324.3	3732.1	7.6492	1.7747	2.2686	718.21	3.2791	3.3505e-05	0.084034	vapor
894.84	2.5000	6.1176	0.16346	3327.3	3735.9	7.6534	1.7757	2.2694	718.86	3.2618	3.3571e-05	0.084253	vapor
896.50	2.5000	6.1058	0.16378	3330.2	3739.7	7.6576	1.7767	2.2702	719.51	3.2447	3.3637e-05	0.084473	vapor
898.16	2.5000	6.0940	0.16410	3333.2	3743.4	7.6618	1.7778	2.2710	720.16	3.2276	3.3704e-05	0.084692	vapor
899.82	2.5000	6.0823	0.16441	3336.2	3747.2	7.6660	1.7788	2.2719	720.80	3.2107	3.3770e-05	0.084912	vapor
901.48	2.5000	6.0706	0.16473	3339.2	3751.0	7.6702	1.7798	2.2727	721.45	3.1939	3.3836e-05	0.085132	vapor
903.14	2.5000	6.0589	0.16505	3342.1	3754.8	7.6744	1.7808	2.2735	722.10	3.1772	3.3902e-05	0.085352	vapor
904.80	2.5000	6.0473	0.16536	3345.1	3758.5	7.6786	1.7818	2.2743	722.74	3.1606	3.3968e-05	0.085572	vapor
906.46	2.5000	6.0358	0.16568	3348.1	3762.3	7.6827	1.7829	2.2751	723.38	3.1442	3.4034e-05	0.085793	vapor
908.12	2.5000	6.0243	0.16600	3351.1	3766.1	7.6869	1.7839	2.2760	724.03	3.1279	3.4100e-05	0.086013	vapor
909.78	2.5000	6.0128	0.16631	3354.1	3769.9	7.6911	1.7849	2.2768	724.67	3.1116	3.4166e-05	0.086234	vapor
911.44	2.5000	6.0014	0.16663	3357.1	3773.6	7.6952	1.7860	2.2777	725.31	3.0955	3.4232e-05	0.086455	vapor
913.10	2.5000	5.9900	0.16694	3360.1	3777.4	7.6994	1.7870	2.2785	725.95	3.0795	3.4298e-05	0.086676	vapor
914.76	2.5000	5.9787	0.16726	3363.1	3781.2	7.7035	1.7880	2.2793	726.59	3.0636	3.4364e-05	0.086897	vapor
916.42	2.5000	5.9674	0.16758	3366.1	3785.0	7.7076	1.7891	2.2802	727.23	3.0479	3.4430e-05	0.087118	vapor
918.08	2.5000	5.9562	0.16789	3369.0	3788.8	7.7118	1.7901	2.2810	727.87	3.0322	3.4496e-05	0.087340	vapor
919.74	2.5000	5.9450	0.16821	3372.0	3792.6	7.7159	1.7911	2.2819	728.51	3.0166	3.4561e-05	0.087561	vapor
921.40	2.5000	5.9338	0.16852	3375.0	3796.4	7.7200	1.7922	2.2827	729.14	3.0012	3.4627e-05	0.087783	vapor
923.06	2.5000	5.9227	0.16884	3378.0	3800.1	7.7241	1.7932	2.2836	729.78	2.9858	3.4693e-05	0.088005	vapor
924.72	2.5000	5.9117	0.16916	3381.0	3803.9	7.7282	1.7943	2.2845	730.41	2.9706	3.4759e-05	0.088227	vapor
926.38	2.5000	5.9007	0.16947	3384.0	3807.7	7.7323	1.7953	2.2853	731.05	2.9554	3.4824e-05	0.088449	vapor
928.04	2.5000	5.8897	0.16979	3387.1	3811.5	7.7364	1.7963	2.2862	731.68	2.9404	3.4890e-05	0.088671	vapor
929.70	2.5000	5.8788	0.17010	3390.1	3815.3	7.7405	1.7974	2.2871	732.31	2.9255	3.4955e-05	0.088894	vapor
931.36	2.5000	5.8679	0.17042	3393.1	3819.1	7.7446	1.7984	2.2880	732.94	2.9106	3.5021e-05	0.089116	vapor
933.02	2.5000	5.8570	0.17074	3396.1	3822.9	7.7486	1.7995	2.2888	733.58	2.8959	3.5086e-05	0.089339	vapor
934.68	2.5000	5.8462	0.17105	3399.1	3826.7	7.7527	1.8005	2.2897	734.21	2.8813	3.5151e-05	0.089562	vapor
936.34	2.5000	5.8355	0.17137	3402.1	3830.5	7.7568	1.8016	2.2906	734.83	2.8667	3.5217e-05	0.089785	vapor
938.00	2.5000	5.8247	0.17168	3405.1	3834.3	7.7608	1.8027	2.2915	735.46	2.8523	3.5282e-05	0.090008	vapor
939.66	2.5000	5.8141	0.17200	3408.1	3838.1	7.7649	1.8037	2.2924	736.09	2.8379	3.5348e-05	0.090231	vapor
941.32	2.5000	5.8034	0.17231	3411.2	3841.9	7.7689	1.8048	2.2933	736.72	2.8237	3.5413e-05	0.090454	vapor
942.98	2.5000	5.7928	0.17263	3414.2	3845.7	7.7730	1.8058	2.2942	737.34	2.8095	3.5478e-05	0.090678	vapor
944.64	2.5000	5.7823	0.17294	3417.2	3849.5	7.7770	1.8069	2.2951	737.97	2.7955	3.5543e-05	0.090902	vapor
946.30	2.5000	5.7717	0.17326	3420.2	3853.4	7.7810	1.8079	2.2960	738.59	2.7815	3.5608e-05	0.091125	vapor
947.96	2.5000	5.7613	0.17357	3423.2	3857.2	7.7851	1.8090	2.2969	739.22	2.7676	3.5674e-05	0.091349	vapor
949.62	2.5000	5.7508	0.17389	3426.3	3861.0	7.7891	1.8101	2.2978	739.84	2.7538	3.5739e-05	0.091573	vapor
951.28	2.5000	5.7404	0.17420	3429.3	3864.8	7.7931	1.8111	2.2987	740.46	2.7402	3.5804e-05	0.091797	vapor
952.94	2.5000	5.7301	0.17452	3432.3	3868.6	7.7971	1.8122	2.2996	741.08	2.7265	3.5869e-05	0.092022	vapor
954.60	2.5000	5.7197	0.17483	3435.4	3872.4	7.8011	1.8133	2.3005	741.70	2.7130	3.5934e-05	0.092246	vapor
956.26	2.5000	5.7095	0.17515	3438.4	3876.3	7.8051	1.8143	2.3014	742.32	2.6996	3.5999e-05	0.092470	vapor
957.92	2.5000	5.6992	0.17546	3441.4	3880.1	7.8091	1.8154	2.3023	742.94	2.6863	3.6064e-05	0.092695	vapor
959.58	2.5000	5.6890	0.17578	3444.5	3883.9	7.8131	1.8165	2.3033	743.56	2.6730	3.6129e-05	0.092920	vapor
961.24	2.5000	5.6788	0.17609	3447.5	3887.7	7.8171	1.8176	2.3042	744.18	2.6599	3.6193e-05	0.093145	vapor
962.90	2.5000	5.6687	0.17641	3450.5	3891.5	7.8211	1.8186	2.3051	744.80	2.6468	3.6258e-05	0.093370	vapor
964.56	2.5000	5.6586	0.17672	3453.6	3895.4	7.8250	1.8197	2.3060	745.41	2.6338	3.6323e-05	0.093595	vapor
966.22	2.5000	5.6486	0.17704	3456.6	3899.2	7.8290	1.8208	2.3070	746.03	2.6209	3.6388e-05	0.093820	vapor
967.88	2.5000	5.6386	0.17735	3459.7	3903.0	7.8329	1.8218	2.3079	746.64	2.6081	3.6452e-05	0.094045	vapor
969.54	2.5000	5.6286	0.17766	3462.7	3906.9	7.8369	1.8229	2.3088	747.26	2.5953	3.6517e-05	0.094271	vapor
971.20	2.5000	5.6186	0.17798	3465.8	3910.7	7.8409	1.8240	2.3098	747.87	2.5826	3.6582e-05	0.094496	vapor
972.86	2.5000	5.6087	0.17829	3468.8	3914.5	7.8448	1.8251	2.3107	748.48	2.5701	3.6646e-05	0.094722	vapor
974.52	2.5000	5.5989	0.17861	3471.9	3918.4	7.8487	1.8262	2.3117	749.09	2.5576	3.6711e-05	0.094948	vapor
976.18	2.5000	5.5890	0.17892	3474.9	3922.2	7.8527	1.8272	2.3126	749.71	2.5451	3.6775e-05	0.095174	vapor
977.84	2.5000	5.5792	0.17924	3478.0	3926.0	7.8566	1.8283	2.3135	750.32	2.5328	3.6840e-05	0.095400	vapor
979.50	2.5000	5.5695	0.17955	3481.0	3929.9	7.8605	1.8294	2.3145	750.93	2.5205	3.6904e-05	0.095626	vapor
981.16	2.5000	5.5597	0.17986	3484.1	3933.7	7.8645	1.8305	2.3154	751.54	2.5083	3.6969e-05	0.095852	vapor
982.82	2.5000	5.5500	0.18018	3487.1	3937.6	7.8684	1.8316	2.3164	752.14	2.4962	3.7033e-05	0.096078	vapor
984.48	2.5000	5.5404	0.18049	3490.2	3941.4	7.8723	1.8326	2.3173	752.75	2.4842	3.7097e-05	0.096305	vapor
986.14	2.5000	5.5308	0.18081	3493.3	3945.3	7.8762	1.8337	2.3183	753.36	2.4723	3.7162e-05	0.096531	vapor
987.80	2.5000	5.5212	0.18112	3496.3	3949.1	7.8801	1.8348	2.3192	753.96	2.4604	3.7226e-05	0.096758	vapor
989.46	2.5000	5.5116	0.18144	3499.4	3953.0	7.8840	1.8359	2.3202	754.57	2.4486	3.7290e-05	0.096985	vapor
991.12	2.5000	5.5021	0.18175	3502.5	3956.8	7.8879	1.8370	2.3212	755.17	2.4368	3.7354e-05	0.097212	vapor
992.78	2.5000	5.4926	0.18206	3505.5	3960.7	7.8918	1.8381	2.3221	755.78	2.4252	3.7419e-05	0.097439	vapor
994.44	2.5000	5.4832	0.18238	3508.6	3964.5	7.8956	1.8392	2.3231	756.38	2.4136	3.7483e-05	0.097666	vapor
996.10	2.5000	5.4737	0.18269	3511.7	3968.4	7.8995	1.8403	2.3240	756.99	2.4021	3.7547e-05	0.097893	vapor
997.76	2.5000	5.4644	0.18300	3514.7	3972.2	7.9034	1.8413	2.3250	757.59	2.3906	3.7611e-05	0.098120	vapor
999.42	2.5000	5.4550	0.18332	3517.8	3976.1	7.9072	1.8424	2.3260	758.19	2.3793	3.7675e-05	0.098348	vapor
1001.1	2.5000	5.4457	0.18363	3520.9	3980.0	7.9111	1.8435	2.3269	758.79	2.3679	3.7739e-05	0.098575	vapor
1002.7	2.5000	5.4364	0.18395	3524.0	3983.8	7.9150	1.8446	2.3279	759.39	2.3567	3.7803e-05	0.098803	vapor
1004.4	2.5000	5.4272	0.18426	3527.1	3987.7	7.9188	1.8457	2.3289	759.99	2.3456	3.7867e-05	0.099031	vapor
1006.1	2.5000	5.4179	0.18457	3530.1	3991.6	7.9227	1.8468	2.3299	760.59	2.3345	3.7930e-05	0.099258	vapor
1007.7	2.5000	5.4087	0.18489	3533.2	3995.4	7.9265	1.8479	2.3308	761.19	2.3234	3.7994e-05	0.099486	vapor
1009.4	2.5000	5.3996	0.18520	3536.3	3999.3	7.9303	1.8490	2.3318	761.78	2.3125	3.8058e-05	0.099714	vapor
1011.0	2.5000	5.3905	0.18551	3539.4	4003.2	7.9342	1.8501	2.3328	762.38	2.3016	3.8122e-05	0.099942	vapor
1012.7	2.5000	5.3814	0.18583	3542.5	4007.0	7.9380	1.8512	2.3338	762.98	2.2908	3.8186e-05	0.10017	vapor
1014.4	2.5000	5.3723	0.18614	3545.6	4010.9	7.9418	1.8523	2.3347	763.57	2.2800	3.8249e-05	0.10040	vapor
1016.0	2.5000	5.3633	0.18645	3548.7	4014.8	7.9456	1.8534	2.3357	764.17	2.2693	3.8313e-05	0.10063	vapor
1017.7	2.5000	5.3543	0.18677	3551.8	4018.7	7.9495	1.8545	2.3367	764.76	2.2587	3.8377e-05	0.10086	vapor
1019.3	2.5000	5.3453	0.18708	3554.9	4022.6	7.9533	1.8556	2.3377	765.36				

1050.9	2.5000	5.1807	0.19302	3614.0	4096.6	8.0248	1.8765	2.3566	776.52	2.0590	3.9641e-05	0.10545	vapor
1052.5	2.5000	5.1723	0.19334	3617.2	4100.5	8.0285	1.8776	2.3576	777.10	2.0496	3.9704e-05	0.10568	vapor
1054.2	2.5000	5.1640	0.19365	3620.3	4104.4	8.0322	1.8787	2.3586	777.68	2.0403	3.9767e-05	0.10591	vapor
1055.9	2.5000	5.1557	0.19396	3623.4	4108.3	8.0359	1.8798	2.3596	778.26	2.0310	3.9830e-05	0.10614	vapor
1057.5	2.5000	5.1474	0.19427	3626.6	4112.2	8.0396	1.8809	2.3606	778.84	2.0218	3.9892e-05	0.10637	vapor
1059.2	2.5000	5.1391	0.19459	3629.7	4116.2	8.0433	1.8820	2.3616	779.42	2.0126	3.9955e-05	0.10660	vapor
1060.8	2.5000	5.1309	0.19490	3632.8	4120.1	8.0470	1.8831	2.3626	780.00	2.0035	4.0018e-05	0.10683	vapor
1062.5	2.5000	5.1227	0.19521	3636.0	4124.0	8.0507	1.8842	2.3637	780.58	1.9944	4.0081e-05	0.10706	vapor
1064.2	2.5000	5.1145	0.19552	3639.1	4127.9	8.0544	1.8853	2.3647	781.15	1.9854	4.0143e-05	0.10729	vapor
1065.8	2.5000	5.1063	0.19584	3642.3	4131.9	8.0581	1.8864	2.3657	781.73	1.9765	4.0206e-05	0.10752	vapor
1067.5	2.5000	5.0982	0.19615	3645.4	4135.8	8.0618	1.8875	2.3667	782.31	1.9676	4.0268e-05	0.10775	vapor
1069.1	2.5000	5.0901	0.19646	3648.6	4139.7	8.0655	1.8886	2.3677	782.88	1.9587	4.0331e-05	0.10799	vapor
1070.8	2.5000	5.0820	0.19677	3651.7	4143.7	8.0691	1.8897	2.3687	783.46	1.9499	4.0393e-05	0.10822	vapor
1072.5	2.5000	5.0740	0.19708	3654.9	4147.6	8.0728	1.8908	2.3697	784.03	1.9412	4.0456e-05	0.10845	vapor
1074.1	2.5000	5.0659	0.19740	3658.0	4151.5	8.0765	1.8919	2.3707	784.61	1.9325	4.0518e-05	0.10868	vapor
1075.8	2.5000	5.0579	0.19771	3661.2	4155.5	8.0801	1.8930	2.3718	785.18	1.9238	4.0580e-05	0.10891	vapor
1077.4	2.5000	5.0500	0.19802	3664.3	4159.4	8.0838	1.8941	2.3728	785.75	1.9152	4.0643e-05	0.10914	vapor
1079.1	2.5000	5.0420	0.19833	3667.5	4163.3	8.0875	1.8952	2.3738	786.32	1.9067	4.0705e-05	0.10938	vapor
1080.8	2.5000	5.0341	0.19865	3670.7	4167.3	8.0911	1.8963	2.3748	786.90	1.8982	4.0767e-05	0.10961	vapor
1082.4	2.5000	5.0262	0.19896	3673.8	4171.2	8.0948	1.8974	2.3758	787.47	1.8897	4.0830e-05	0.10984	vapor
1084.1	2.5000	5.0183	0.19927	3677.0	4175.2	8.0984	1.8985	2.3768	788.04	1.8813	4.0892e-05	0.11007	vapor
1085.7	2.5000	5.0105	0.19958	3680.2	4179.1	8.1020	1.8996	2.3779	788.61	1.8729	4.0954e-05	0.11030	vapor
1087.4	2.5000	5.0027	0.19989	3683.3	4183.1	8.1057	1.9007	2.3789	789.18	1.8646	4.1016e-05	0.11054	vapor
1089.1	2.5000	4.9949	0.20021	3686.5	4187.0	8.1093	1.9018	2.3799	789.75	1.8564	4.1078e-05	0.11077	vapor
1090.7	2.5000	4.9871	0.20052	3689.7	4191.0	8.1129	1.9029	2.3809	790.31	1.8481	4.1140e-05	0.11100	vapor
1092.4	2.5000	4.9794	0.20083	3692.8	4194.9	8.1165	1.9040	2.3819	790.88	1.8400	4.1202e-05	0.11123	vapor
1094.0	2.5000	4.9716	0.20114	3696.0	4198.9	8.1202	1.9051	2.3830	791.45	1.8318	4.1264e-05	0.11147	vapor
1095.7	2.5000	4.9639	0.20145	3699.2	4202.8	8.1238	1.9062	2.3840	792.02	1.8237	4.1326e-05	0.11170	vapor
1097.4	2.5000	4.9563	0.20176	3702.4	4206.8	8.1274	1.9073	2.3850	792.58	1.8157	4.1388e-05	0.11193	vapor
1099.0	2.5000	4.9486	0.20208	3705.5	4210.7	8.1310	1.9085	2.3860	793.15	1.8077	4.1450e-05	0.11216	vapor
1100.7	2.5000	4.9410	0.20239	3708.7	4214.7	8.1346	1.9096	2.3871	793.71	1.7998	4.1512e-05	0.11240	vapor
1102.3	2.5000	4.9334	0.20270	3711.9	4218.7	8.1382	1.9107	2.3881	794.28	1.7919	4.1573e-05	0.11263	vapor
1104.0	2.5000	4.9258	0.20301	3715.1	4222.6	8.1418	1.9118	2.3891	794.84	1.7840	4.1635e-05	0.11286	vapor
1105.7	2.5000	4.9183	0.20332	3718.3	4226.6	8.1454	1.9129	2.3901	795.41	1.7762	4.1697e-05	0.11310	vapor
1107.3	2.5000	4.9108	0.20363	3721.5	4230.6	8.1490	1.9140	2.3912	795.97	1.7684	4.1759e-05	0.11333	vapor
1109.0	2.5000	4.9033	0.20395	3724.7	4234.5	8.1525	1.9151	2.3922	796.53	1.7607	4.1820e-05	0.11356	vapor
1110.6	2.5000	4.8958	0.20426	3727.9	4238.5	8.1561	1.9162	2.3932	797.10	1.7530	4.1882e-05	0.11380	vapor
1112.3	2.5000	4.8883	0.20457	3731.1	4242.5	8.1597	1.9173	2.3942	797.66	1.7453	4.1944e-05	0.11403	vapor
1114.0	2.5000	4.8809	0.20488	3734.3	4246.5	8.1633	1.9184	2.3953	798.22	1.7377	4.2005e-05	0.11426	vapor
1115.6	2.5000	4.8735	0.20519	3737.5	4250.4	8.1668	1.9195	2.3963	798.78	1.7301	4.2067e-05	0.11450	vapor
1117.3	2.5000	4.8661	0.20550	3740.7	4254.4	8.1704	1.9206	2.3973	799.34	1.7226	4.2128e-05	0.11473	vapor
1118.9	2.5000	4.8587	0.20582	3743.9	4258.4	8.1740	1.9217	2.3983	799.90	1.7151	4.2190e-05	0.11496	vapor
1120.6	2.5000	4.8514	0.20613	3747.1	4262.4	8.1775	1.9228	2.3994	800.46	1.7077	4.2251e-05	0.11520	vapor
1122.3	2.5000	4.8441	0.20644	3750.3	4266.4	8.1811	1.9239	2.4004	801.02	1.7003	4.2312e-05	0.11543	vapor
1123.9	2.5000	4.8368	0.20675	3753.5	4270.3	8.1846	1.9250	2.4014	801.57	1.6929	4.2374e-05	0.11566	vapor
1125.6	2.5000	4.8295	0.20706	3756.7	4274.3	8.1882	1.9261	2.4025	802.13	1.6856	4.2435e-05	0.11590	vapor
1127.2	2.5000	4.8223	0.20737	3759.9	4278.3	8.1917	1.9272	2.4035	802.69	1.6783	4.2496e-05	0.11613	vapor
1128.9	2.5000	4.8150	0.20768	3763.1	4282.3	8.1952	1.9283	2.4045	803.25	1.6711	4.2558e-05	0.11637	vapor
1130.6	2.5000	4.8078	0.20799	3766.3	4286.3	8.1988	1.9294	2.4055	803.80	1.6639	4.2619e-05	0.11660	vapor
1132.2	2.5000	4.8006	0.20831	3769.5	4290.3	8.2023	1.9305	2.4066	804.36	1.6567	4.2680e-05	0.11684	vapor
1133.9	2.5000	4.7935	0.20862	3772.7	4294.3	8.2058	1.9316	2.4076	804.91	1.6496	4.2741e-05	0.11707	vapor
1135.5	2.5000	4.7863	0.20893	3776.0	4298.3	8.2094	1.9327	2.4086	805.47	1.6425	4.2802e-05	0.11730	vapor
1137.2	2.5000	4.7792	0.20924	3779.2	4302.3	8.2129	1.9338	2.4096	806.02	1.6354	4.2863e-05	0.11754	vapor
1138.9	2.5000	4.7721	0.20955	3782.4	4306.3	8.2164	1.9349	2.4107	806.58	1.6284	4.2924e-05	0.11777	vapor
1140.5	2.5000	4.7650	0.20986	3785.6	4310.3	8.2199	1.9359	2.4117	807.13	1.6214	4.2985e-05	0.11801	vapor
1142.2	2.5000	4.7580	0.21017	3788.9	4314.3	8.2234	1.9370	2.4127	807.68	1.6145	4.3046e-05	0.11824	vapor
1143.8	2.5000	4.7510	0.21048	3792.1	4318.3	8.2269	1.9381	2.4138	808.23	1.6076	4.3107e-05	0.11848	vapor
1145.5	2.5000	4.7439	0.21080	3795.3	4322.3	8.2304	1.9392	2.4148	808.79	1.6007	4.3168e-05	0.11871	vapor
1147.2	2.5000	4.7370	0.21111	3798.6	4326.3	8.2339	1.9403	2.4158	809.34	1.5939	4.3229e-05	0.11895	vapor
1148.8	2.5000	4.7300	0.21142	3801.8	4330.3	8.2374	1.9414	2.4169	809.89	1.5871	4.3290e-05	0.11918	vapor
1150.5	2.5000	4.7230	0.21173	3805.0	4334.3	8.2409	1.9425	2.4179	810.44	1.5803	4.3351e-05	0.11942	vapor
1152.1	2.5000	4.7161	0.21204	3808.3	4338.4	8.2444	1.9436	2.4189	810.99	1.5736	4.3411e-05	0.11965	vapor
1153.8	2.5000	4.7092	0.21235	3811.5	4342.4	8.2479	1.9447	2.4199	811.54	1.5669	4.3472e-05	0.11989	vapor
1155.5	2.5000	4.7023	0.21266	3814.7	4346.4	8.2513	1.9458	2.4210	812.09	1.5603	4.3533e-05	0.12012	vapor
1157.1	2.5000	4.6954	0.21297	3818.0	4350.4	8.2548	1.9469	2.4220	812.63	1.5537	4.3593e-05	0.12036	vapor
1158.8	2.5000	4.6886	0.21328	3821.2	4354.4	8.2583	1.9480	2.4230	813.18	1.5471	4.3654e-05	0.12059	vapor
1160.4	2.5000	4.6818	0.21359	3824.5	4358.5	8.2618	1.9491	2.4241	813.73	1.5405	4.3715e-05	0.12083	vapor
1162.1	2.5000	4.6750	0.21390	3827.7	4362.5	8.2652	1.9502	2.4251	814.28	1.5340	4.3775e-05	0.12106	vapor
1163.8	2.5000	4.6682	0.21422	3831.0	4366.5	8.2687	1.9513	2.4261	814.82	1.5275	4.3836e-05	0.12130	vapor
1165.4	2.5000	4.6614	0.21453	3834.2	4370.5	8.2722	1.9523	2.4271	815.37	1.5211	4.3896e-05	0.12154	vapor
1167.1	2.5000	4.6547	0.21484	3837.5	4374.6	8.2756	1.9534	2.4282	815.92	1.5147	4.3957e-05	0.12177	vapor
1168.7	2.5000	4.6480	0.21515	3840.7	4378.6	8.2791	1.9545	2.4292	816.46	1.5083	4.4017e-05	0.12201	vapor
1170.4	2.5000	4.6413	0.21546	3844.0	4382.6	8.2825	1.9556	2.4302	817.01	1.5019	4.4077e-05	0.12224	vapor
1172.1	2.5000	4.6346	0.21577	3847.2	4386.7	8.2860	1.9567	2.4313	817.55	1.4956	4.4138e-05	0.12248	vapor
1173.7	2.5000	4.6279	0.21608	3850.5	4390.7	8.2894	1.9578	2.4323	818.09	1.4893	4.4198e-05	0.12271	vapor
1175.4	2.5000	4.6213	0.21639	3853.8	4394.7	8.2928	1.9589	2.4333	818.64	1.4831	4.4258e-05	0.12295	vapor
1177.0	2.5000	4.6146	0.21670	3857.0	4398.8	8.2963	1.9600	2.4343	819.18	1.4769	4.4319e-05	0.12319	vapor
1178.7	2.5000												

1208.6	2.5000	4.4923	0.22260	3919.4	4475.9	8.3609	1.9805	2.4538	829.41	1.3645	4.5457e-05	0.12769	vapor
1210.2	2.5000	4.4861	0.22291	3922.7	4479.9	8.3643	1.9816	2.4549	829.95	1.3589	4.5516e-05	0.12792	vapor
1211.9	2.5000	4.4798	0.22322	3926.0	4484.0	8.3676	1.9826	2.4559	830.48	1.3533	4.5576e-05	0.12816	vapor
1213.6	2.5000	4.4736	0.22353	3929.3	4488.1	8.3710	1.9837	2.4569	831.02	1.3478	4.5636e-05	0.12840	vapor
1215.2	2.5000	4.4674	0.22384	3932.6	4492.2	8.3744	1.9848	2.4579	831.55	1.3422	4.5695e-05	0.12864	vapor
1216.9	2.5000	4.4612	0.22415	3935.9	4496.3	8.3777	1.9859	2.4589	832.08	1.3367	4.5754e-05	0.12887	vapor
1218.5	2.5000	4.4551	0.22446	3939.2	4500.3	8.3811	1.9869	2.4600	832.61	1.3312	4.5814e-05	0.12911	vapor
1220.2	2.5000	4.4489	0.22477	3942.5	4504.4	8.3844	1.9880	2.4610	833.15	1.3258	4.5873e-05	0.12935	vapor
1221.9	2.5000	4.4428	0.22508	3945.8	4508.5	8.3878	1.9891	2.4620	833.68	1.3203	4.5933e-05	0.12959	vapor
1223.5	2.5000	4.4367	0.22539	3949.1	4512.6	8.3911	1.9901	2.4630	834.21	1.3149	4.5992e-05	0.12982	vapor
1225.2	2.5000	4.4306	0.22570	3952.4	4516.7	8.3944	1.9912	2.4640	834.74	1.3096	4.6051e-05	0.13006	vapor
1226.8	2.5000	4.4245	0.22601	3955.7	4520.8	8.3978	1.9923	2.4651	835.27	1.3042	4.6110e-05	0.13030	vapor
1228.5	2.5000	4.4184	0.22632	3959.1	4524.9	8.4011	1.9934	2.4661	835.80	1.2989	4.6170e-05	0.13054	vapor
1230.2	2.5000	4.4124	0.22663	3962.4	4529.0	8.4044	1.9944	2.4671	836.33	1.2936	4.6229e-05	0.13078	vapor
1231.8	2.5000	4.4064	0.22694	3965.7	4533.1	8.4078	1.9955	2.4681	836.86	1.2883	4.6288e-05	0.13101	vapor
1233.5	2.5000	4.4003	0.22725	3969.0	4537.2	8.4111	1.9966	2.4691	837.39	1.2831	4.6347e-05	0.13125	vapor
1235.1	2.5000	4.3943	0.22757	3972.3	4541.3	8.4144	1.9976	2.4702	837.91	1.2779	4.6406e-05	0.13149	vapor
1236.8	2.5000	4.3884	0.22788	3975.7	4545.4	8.4177	1.9987	2.4712	838.44	1.2727	4.6465e-05	0.13173	vapor
1238.5	2.5000	4.3824	0.22819	3979.0	4549.5	8.4211	1.9997	2.4722	838.97	1.2675	4.6524e-05	0.13197	vapor
1240.1	2.5000	4.3765	0.22850	3982.3	4553.6	8.4244	2.0008	2.4732	839.50	1.2624	4.6583e-05	0.13221	vapor
1241.8	2.5000	4.3705	0.22881	3985.7	4557.7	8.4277	2.0019	2.4742	840.02	1.2572	4.6642e-05	0.13245	vapor
1243.4	2.5000	4.3646	0.22912	3989.0	4561.8	8.4310	2.0029	2.4752	840.55	1.2521	4.6701e-05	0.13268	vapor
1245.1	2.5000	4.3587	0.22943	3992.3	4565.9	8.4343	2.0040	2.4762	841.08	1.2471	4.6760e-05	0.13292	vapor
1246.8	2.5000	4.3528	0.22974	3995.7	4570.0	8.4376	2.0050	2.4773	841.60	1.2420	4.6819e-05	0.13316	vapor
1248.4	2.5000	4.3470	0.23005	3999.0	4574.1	8.4409	2.0061	2.4783	842.13	1.2370	4.6878e-05	0.13340	vapor
1250.1	2.5000	4.3411	0.23036	4002.3	4578.2	8.4442	2.0072	2.4793	842.65	1.2320	4.6937e-05	0.13364	vapor
1251.7	2.5000	4.3353	0.23067	4005.7	4582.3	8.4475	2.0082	2.4803	843.17	1.2270	4.6995e-05	0.13388	vapor
1253.4	2.5000	4.3295	0.23098	4009.0	4586.5	8.4508	2.0093	2.4813	843.70	1.2221	4.7054e-05	0.13412	vapor
1255.1	2.5000	4.3237	0.23128	4012.4	4590.6	8.4540	2.0103	2.4823	844.22	1.2172	4.7113e-05	0.13436	vapor
1256.7	2.5000	4.3179	0.23159	4015.7	4594.7	8.4573	2.0114	2.4833	844.74	1.2123	4.7171e-05	0.13459	vapor
1258.4	2.5000	4.3121	0.23190	4019.1	4598.8	8.4606	2.0124	2.4843	845.27	1.2074	4.7230e-05	0.13483	vapor
1260.0	2.5000	4.3064	0.23221	4022.4	4603.0	8.4639	2.0135	2.4854	845.79	1.2025	4.7288e-05	0.13507	vapor
1261.7	2.5000	4.3006	0.23252	4025.8	4607.1	8.4671	2.0145	2.4864	846.31	1.1977	4.7347e-05	0.13531	vapor
1263.4	2.5000	4.2949	0.23283	4029.1	4611.2	8.4704	2.0156	2.4874	846.83	1.1929	4.7405e-05	0.13555	vapor
1265.0	2.5000	4.2892	0.23314	4032.5	4615.3	8.4737	2.0166	2.4884	847.35	1.1881	4.7464e-05	0.13579	vapor
1266.7	2.5000	4.2835	0.23345	4035.8	4619.5	8.4769	2.0177	2.4894	847.88	1.1833	4.7522e-05	0.13603	vapor
1268.3	2.5000	4.2778	0.23376	4039.2	4623.6	8.4802	2.0187	2.4904	848.40	1.1786	4.7581e-05	0.13627	vapor
1270.0	2.5000	4.2722	0.23407	4042.6	4627.7	8.4835	2.0198	2.4914	848.92	1.1739	4.7639e-05	0.13651	vapor

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